

1 **The effect of composition on chlorine solubility and**
2 **behaviour in silicate melts**

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10 REVISION2

Abstract

11

12 We have performed experiments at 1.5 GPa and 1400 °C on 25 different bulk compositions to
13 determine the effects of major element compositions on the Cl contents of silicate melts at
14 known fugacities of Cl₂ and O₂. The experimental method involved mixing a “sliding” Cl
15 buffer, a mixture of AgCl, AgI and Ag with the silicate bulk composition and performing the
16 experiment in a graphite capsule together with a source of CO₂ (AgCO₃). The graphite
17 capsules were sealed inside welded Pt tubes in order to maintain a CO₂-CO atmosphere with
18 oxygen fugacity fixed at the C-CO-CO₂ (CCO) buffer. During the experiment, the Cl buffer
19 segregates leaving a Cl-bearing melt, which quenches to a glass. We used the results to define
20 chloride capacity C_{Cl} for each melt at the pressure and temperature of the experiment:

$$C_{Cl} = \frac{Cl \text{ (wt\%)}}{\sqrt{f(Cl_2)}} \times \sqrt[4]{f(O_2)}$$

21 Chloride capacity was found to correlate positively with optical basicity and NBO/T and
22 negatively with ionic porosity and the Larsen Index. We combined our new data with the
23 results of Thomas and Wood (2021) to derive an equation describing the composition,
24 pressure and temperature dependence of the chloride capacity:

$$25 \log C_{Cl} = 1.601 + (4470X_{Ca} - 3430X_{Si} + 2592X_{Fe} - 4092X_K - 894P)/T$$

26 In this equation, X_{Ca}, X_{Si} and so on refer to the oxide mole fractions on a single cation basis,
27 P is in GPa and T in K. The equation reproduces 58 data points with an r² of 0.96 and a
28 standard error of 0.089. The addition of literature data on hydrous experiments indicates that
29 the effects of <4.3 weight% H₂O are small enough to be ignored. We also performed
30 experiments aimed at determining the conditions of NaCl saturation in melts. When
31 combined with literature data we obtained:

$$\log(Cl^-) = \log(a_{NaCl}) + 0.06 - (2431X_{Ca} + 3430X_{Si} - 2592X_{Fe} + 3484X_{Na} + 4092X_K - 2417)/T$$

Where (Cl⁻) is the Cl content of the melt in weight % a_{NaCl} is the activity of NaCl (liquid) and the other symbols are the same as before. The results indicate that basalt dissolves approximately 8 times more Cl than rhyolite at a given NaCl activity i.e., Cl is approximately 8 times more soluble in basalt than in rhyolite.

Key Words: basalt; rhyolite; Cl solubility in melts; Compositional effects on Cl solubility; Cl degassing; Chloride capacity; NaCl saturation in melts

INTRODUCTION

The volatile components whose behaviour is best understood in silicate melts are H₂O and CO₂ (Symonds et al. 1994; De Vivo et al. 2005). In the case of H₂O, the reasons are its high abundance, the major effects it has on viscosity, the melting and crystallisation temperatures of melts, and its importance in hydrothermal ore deposition associated with igneous activity. CO₂ came to be studied experimentally in the 1970's initially because of the observation that carbonatites were magmas with origins in the mantle. More recently concerns about volcanogenic CO₂ as a greenhouse gas has facilitated the establishment of a good database to describe CO₂ solubility in a wide range of melts over a wide range of physical conditions (Brooker et al. 2001; Stanley et al. 2011), allowing for the development of robust models, such as *VolatileCalc* (Newman and Lowenstern 2002) and *MagmaSat* (Ghiorso and Gualda 2015).

A third group of elements that are geologically and environmentally important and

55 whose behaviour in melts requires further elucidation are the halogens. Chlorine, the second
56 most abundant of the halogens (after F) in both the primitive and depleted mantle, and in the
57 bulk continental crust (Pyle and Mather 2009), is an important ligand in hydrothermal
58 processes and plays a major role in transporting economically important metals such as Au
59 and Cu in solution (Blundy et al. 2015). The segregation of Cl-rich brines from melts in the
60 later stages of igneous activity can lead to significant metal transport and has resulted in
61 major economic deposits at, for example, Broken Hill in New South Wales, Australia
62 (Millsted and Mavrogenes 2015) and in porphyry copper deposits (Nash 1976; Fuge et al.
63 1986). Moore and Nash (1974) found that halite rich fluid inclusions perfectly outlined the
64 Cu-rich ore zone at Bingham Canyon, Utah, USA and that fluid inclusions found in a PGE
65 deposit helped delineate the ore at the Stillwater Complex, Montana USA (Hanley et al.
66 2008). Lastly, the two most economically important iron oxide copper-gold (IOCG) deposits
67 in Chile, Mantoverde, and Candelaria-Punta del Cobre, both exhibit high-salinity fluid
68 inclusions (Marschik and Kendrick 2015).

69 Halogens released by volcanism act to transport trace metals in gaseous form into the
70 environment (Scholtysik and Canil 2021), which act as catalysts for the destruction of
71 stratospheric ozone (von Glasow et al. 2009) and in some cases can cause major local
72 environmental degradation. The 1783 eruption of Laki, for example, led to the release of ~8
73 million tonnes of F causing the deaths by fluorosis of a large fraction of Iceland's sheep and
74 cattle population and about 25% of the population in the ensuing famine.

75 During differentiation of igneous melts, the halogens behave as highly incompatible
76 elements (Edmonds et al. 2009; Pyle and Mather 2009) where they are concentrated in the
77 melts until lost in a gas or fluid phase or incorporated into a quenched glass and minor
78 crystalline phases such as apatite or sodalite (Sharp and Draper 2013). Thermodynamic
79 equilibrium speciation calculations and observations of modern volcanic edifices (Symonds

80 et al. 1992; Martin et al. 2006) indicate that the halogens are predominantly degassed in the
81 form of halogen-bearing acids (HF, HCl, HBr, and HI; Gerlach, (2004); Martin et al. (2006)).
82 Volcanic gases typically comprise > 90% H₂O plus CO₂, with < 10% SO₂ plus HCl and HF
83 and trace amounts of H₂S, H₂, CO, HBr, and HI (Pyle and Mather 2009; Martin et al. 2012).
84 Estimates of halogen fluxes vary greatly and current volcanic degassing from arc and non-arc
85 eruptions are estimated to vary from 0.3 Tg/Yr to 5.5 Tg/Yr for HCl, 0.15 Tg/Yr to 0.58
86 Tg/Yr for HF, 0.0001Tg/Yr to 0.016 Tg/Yr for HBr, and 0.00004 Tg/Yr to 0.0017Tg/Yr for
87 HI (Gerlach 2004; Aiuppa et al. 2009; Pyle and Mather 2009; Webster et al. 2018).

88 Given their environmental and geochemical importance, the properties and
89 distribution of halogens in natural and experimentally produced silicate melts and coexisting
90 fluid phases are the subject of broad ongoing interest. They are observed to have profound
91 effects on the phase equilibria and viscosities of melts (Zimova and Webb 2006; Filiberto
92 and Treiman 2009; Baasner et al. 2013) leading, for example, to Cl being twice as effective
93 on a molar basis at lowering the liquidus of basalt as H₂O (Filiberto and Treiman 2009).
94 Experimental determinations under controlled conditions show that Cl solubility tends to
95 increase with decreasing SiO₂ concentration in the melt (Iwasaki and Katsura, 1967; Carroll
96 and Webster, 1994; Webster et al. 1999; Signorelli and Carroll 2000; Webster and De Vivo
97 2002). Decreases in the SiO₂ concentration generally correlates with increasing
98 concentrations of network-modifying cations. Experiments employing saturation in hydro-
99 saline liquids (Webster et al. 2015) indicate that the Cl concentration increases at fixed
100 temperature and pressure with increasing CaO, MgO, and alkali contents of the silicate
101 melts. **OK** The compositional effects were parameterised as a Cl solubility
102 model (Webster et al. 2015), which provides an important baseline for future work. This
103 model has some uncertainty, however, because the coexisting hydrosaline liquids change in
104 composition, and hence the Cl₂ fugacity, as the silicate melt composition changes. A method

105 by which Cl fugacity can be varied independently of the silicate melt composition is
106 required to better constrain the compositional effects on Cl solubility. Thomas and Wood,
107 (2021) developed such a method based on the equilibrium:

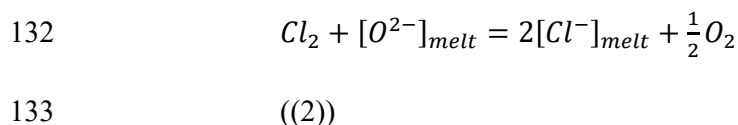


109 liquid liquid

110 Coexistence of liquid AgCl and liquid Ag metal at fixed pressure and temperature buffer the
111 fugacity of Cl₂. Since Ag is virtually insoluble in silicate melt, except under very oxidising
112 conditions (Thomas and Wood 2021), the composition of a coexisting silicate melt can be
113 varied almost at will at a known, (in principle), buffered, Cl fugacity. In practice, we found
114 that Cl fugacities were so high using the Ag/AgCl buffer that discrete Ca-Mg chloride
115 liquids segregated from haplobasaltic melts at the experimental conditions of 1.5
116 GPa/1400°C. In order to suppress the exsolution of chlorides, we therefore, diluted the AgCl
117 with AgI to form a mixed halide with a known ratio of Cl to I. This approach enables the Cl
118 fugacity to be calculated from a combination of the thermodynamic data for equilibrium (1),
119 the volumes of the liquid Ag and AgCl, and the ratio of Cl/(Cl+I) in the “sliding” Ag/AgCl-
120 AgI buffer. We have tested similar approaches with AgF, AgBr, and AgI and can report that
121 all three can be treated in a similar manner to AgCl in order to fix the fugacities of F, Br,
122 and I respectively. Given its abundance and importance in hydrothermal fluids and volcanic
123 gases, however, the remainder of this report will be dedicated to the behaviour of Cl in
124 silicate melts.

125 Thomas and Wood, (2021) used the Ag/AgCl buffer method described above to
126 investigate the nature of the initial dissolution of Cl in two silicate melts, an Icelandic basalt
127 and a haplobasalt of composition An₅₀Di₂₈Fe₂₂ (Table 1). We found that, at 1.5 GPa/1400
128 °C, dissolution of Cl follows Henry’s Law with the Cl concentration proportional to the

129 square root of Cl fugacity and the fourth root of oxygen fugacity up to concentrations of at
130 least 1.6 wt% Cl in the basalt and 2.6 wt% Cl in the haplobasalt. These observations imply
131 that $2Cl^-$ ions in the melt replace O^{2-} according to the reaction:



134 The Cl^- ions in the melt are dissociated from one another and it is straightforward to show
135 that, at equilibrium, the concentration of Cl^- in the melt is proportional to $f_{Cl_2}^{0.5}$ and inversely
136 proportional to $f_{O_2}^{0.25}$. At concentrations greater than 2.6 wt% Cl in the haplobasalt and ~1.6
137 wt% Cl in the natural basalt, the relationship between Cl concentration and $f_{Cl_2}^{0.5}$ deviates in a
138 direction consistent with the mutual avoidance of the Cl^- ions i.e., the concentration increases
139 less strongly with increasing $f_{Cl_2}^{0.5}$ than in the Henry's Law region (Fig. 1).

140 Our observation that a Ca-rich composition ($An_{50}Di_{28}Fo_{22}$) dissolves substantially
141 more Cl at fixed $f(Cl_2)$ than basalt (Thomas and Wood 2021) is qualitatively in agreement
142 with the model of Webster et al (2015), which incorporates a strong positive correlation
143 between CaO and MgO concentrations in the melt and the Cl content in the melt. These
144 correlations also appear to be reflected in the X-ray absorption (Evans et al. 2008; McKeown
145 et al. 2011) and Nuclear Magnetic Resonance spectra (Stebbins and Du 2002; Sandland et al.
146 2004) of Cl in quenched glasses. These authors concluded that Cl nearest-neighbours, and
147 hence the strongest influences on Cl solubility, are predominantly Ca and Mg (Evans et al.
148 2008; McKeown et al. 2011) or a combination of alkaline and alkali cations (Stebbins and Du
149 2002; Sandland et al. 2004).

150 From the preceding discussion and Figure 1, it is clear that there are strong
151 compositional dependences of Cl solubility in a silicate melt and that the CaO, MgO, and

152 Na₂O concentrations probably play major roles. Our aim here is to quantify these
153 compositional effects at known Cl fugacity in order to extend the application of our Cl
154 fugacity buffer and to build on the experimental approach of Webster et al. (2015). A major
155 advantage of the buffer method is that it is applicable to anhydrous melts, which enables us to
156 study compositional effects in the absence of H₂O and a coexisting hydrous fluid.

157

158 **EXPERIMENTAL METHODOLOGY**

159 **Starting compositions**

160 Since the principal aim of this study was to determine compositional effects on Cl
161 solubility we used a wide range of starting compositions comprising 7 natural samples, and
162 18 synthetic compositions. (Table 1). Synthetic starting compositions were prepared from
163 mixtures of analytical grade oxide powders, (with Fe added as Fe₂O₃), and carbonate powders
164 (Na₂CO₃, CaCO₃, and K₂CO₃). Powders were ground under ethanol for a minimum of 2.5
165 hours to ensure homogeneity. The mixtures were subsequently pressed into pellets,
166 decarbonated by incremental heating overnight from 400 to 800 °C, and the Fe reduced
167 overnight in a 1-atmosphere furnace at 1100 °C and at an $f(\text{O}_2)$ of IW+1 using a CO-CO₂ gas
168 mixture. The reduced mixes were used as starting materials for the experiments. A small
169 fraction of each was re-ground into powder and then melted at 1400 °C in air at 1 atm to
170 check the starting composition (Table 1).

171

172 **Controlling Cl and oxygen fugacity**

173 Chlorine fugacity was controlled by intimately mixing AgI and AgCl in a 75:25 ratio.
174 The presence of iodine reduces the Cl fugacity enough such that blebs of CaCl₂ and MgCl₂ do

175 not segregate from the silicate glass, therefore ensuring that the starting composition remains
176 constant. The Cl fugacity is then obtained from Thomas and Wood (2021):

$$\log f(\text{Cl}_2) = -\frac{11440}{T} + 2.961 + \frac{2150P}{T} - \frac{208P^2}{T} + 2\log\left(\frac{\text{Cl}}{\text{Cl+I}}\right)_{\text{halide}} - 2\log\left(\frac{\text{Ag}}{\text{Ag+Pt}}\right)_{\text{metal}}$$

177
178 (3)

179 In equation (3) the ratios (Cl/(Cl+I)) and (Ag/(Ag+Pt)) refer respectively to the mole
180 fractions of Cl in the mixed halide melt and Ag in the coexisting liquid metal. Mixing in both
181 liquids was assumed to obey Raoult's Law; an assumption, which can be readily shown to be
182 reasonable for AgCl-AgI liquids based on the temperature and position of the 1 atmosphere
183 eutectic (Levin et al. 1964), and to be reasonable for Ag-Pt liquids which are Ag-rich
184 (generally > 0.8 mole fraction; Table 2).

185 The starting silicate compositions were ground together with the AgI/AgCl mixture in
186 a ratio of 75:25 (and packed into 2.5mm outside diameter, 1 mm inside diameter graphite
187 capsules. The graphite capsules were placed, with a 1 mm graphite lid, inside 3mm outside
188 diameter Pt capsules with mixtures of graphite and Ag₂CO₃ above and below the graphite
189 capsule. The platinum capsule was welded shut. During the experiment, the Ag₂CO₃
190 decomposes to Ag liquid metal, and, by reaction with graphite, CO₂. The coexistence of C
191 and CO₂ buffers oxygen fugacity at CCO (Jakobsson and Oskarsson, 1994):

$$\log f(\text{O}_2)_{(\text{CCO})} = 4.325 - \left(\frac{21803}{T}\right) + 0.171\left(\frac{(P-1)}{T}\right) \quad (4)$$

192

193 At the conditions employed in this study (1400 °C and 1.5 GPa), the log $f(\text{O}_2)$ is fixed by this
194 assembly at -7.17 (Thomas and Wood 2021). The experiments employed a 32 mm long, 12.5
195 mm outside diameter, 8 mm inside diameter Ca fluoride cylinder as the principal pressure
196 medium. Inside this cylinder was an 8 mm O.D., 6 mm I.D. graphite cylinder which acts as
197 the furnace. The 3 mm outside diameter capsule was placed in the centre of the graphite

198 furnace with crushable MgO pieces above, below and around the capsule. All experiments
199 were then performed with an end-loaded ‘Boyd and England’-type ½ inch piston-cylinder
200 apparatus (Boyd and England, 1960) housed at the University of Oxford. The temperature
201 was measured and controlled using an alumina-sheathed C-type (W₉₅Re₅–W₇₄Re₂₆)
202 thermocouple, introduced through a hole in the upper MgO piece and separated from the
203 capsule by a 0.5 mm thick alumina disc. All experimental assembly pieces were heated to
204 minimise the presence of water as much as possible to ensure anhydrous conditions. This
205 included heating the MgO pieces at 1000 °C overnight.

206 Experiments were performed at a constant temperature and pressure of 1400 °C and
207 1.5 GPa, respectively (Table 2) using the ‘*hot piston-in*’ method and the pressure calibrations
208 of McDade et al. (2002). In order to test for approach to equilibrium, Thomas and Wood,
209 (2021) performed a time series of experiments from 5 min to 2 h at 1400 °C and 1.5 GPa
210 using a haplobasaltic composition with the oxygen fugacity fixed at the CCO buffer and the
211 Cl fugacity given by an initial AgI:AgCl ratio of 75:25 by weight. We found negligible
212 change in Cl concentration between 5 mins and 2 hours indicating a rapid approach to
213 equilibrium. We repeated the test in our new study using a more viscous dacitic composition
214 (Table 1), which might be expected to equilibrate more slowly than basalt. As before,
215 however, the concentration of Cl was, within uncertainty, unchanged in experiments from 5
216 min to 2 hours duration with a range of 0.46 – 0.50 wt% (Table 2). Subsequent experiments
217 were therefore performed for 1 h or more (Table 2).

218 All experiments resulted in a clear segregation of the silicate glass, metal halide and
219 metal (Figure 2). All experiments were quenched by cutting the power to the graphite furnace
220 (cooling at ≈120 °C/s). Once extracted, the recovered capsule was cleaned and weighed to
221 ensure no mass was lost or gained during the experiment.

222 Two additional experiments were performed with the aim of determining the Cl
223 content of melt at NaCl saturation. For these experiments, we used a natural phonolite (Table
224 1; LS-17985) as the silicate, intimately mixed with 20 wt% NaCl. One experiment was
225 buffered at the CCO oxygen buffer as described above and the other at the Re-ReO₂ buffer
226 using the assembly described by Thomas and Wood (2021). The experiments were held at
227 1100 °C and 1.0 GPa for 2 hours and quenched in the usual manner.

228

229 **Analytical techniques**

230 During the experiment, the buffer-silicate mixture segregates into a homogeneous
231 translucent glass, a metal chloride/iodide phase and an Ag-rich metal alloy (Figure 2). The
232 NaCl-buffered experiments segregated distinctive blobs of NaCl which could be analysed
233 easily with the electron microprobe. The capsules were mounted in epoxy, ground to expose a
234 cross section of the charge and polished with water-free diamond paste, using isopropanol as
235 a lubricant to prevent any Cl loss (Mungall and Brenan 2003).

236 Product silicate glasses and Cl fugacity buffers were analysed on the CAMECA SX-
237 Five-FE field emission electron microprobe at the University of Oxford's Department of
238 Earth Sciences. A 20 nA beam current, 15 kV accelerating voltage, and a defocused 10 µm
239 beam diameter was used for the glass analyses. To minimise the potential for element
240 migration during analysis, Cl, Na, K, and Si were analysed first. Standards used for silicate
241 glass analysis were natural albite (Si, Al, Na), andradite (Ca, Fe), synthetic thallium
242 bromiodide (Br,I) **{{AU: Please ask the authors to fully explain "Tl(Br.I)".DB}}** (I),
243 TiO₂ (Ti), Manganese (Mn), Sanidine (K), synthetic periclase (Mg), NaCl crystals (Cl), Ag,
244 and Pt. Counting times were a minimum of 30 s peak and 15 s background for all elements,
245 except for Cl, which was 80 s peak and 40 s background. The latter gave a detection limit of
246 ≤ 100 ppm for Cl. For Na and K we used 20s peak and 10s background counting times to

247 reduce the chance of element migration from the beam and these elements were analysed first
248 on 2 different spectrometers. Replicate analyses on the same spots of glass revealed that the
249 Cl counts were stable and consistent under these conditions. Over 20 points were taken on
250 each silicate portion of the charge, and 10 to 20 points were taken on the remaining buffer
251 and resultant metal phases. Results remained consistent with a low (< 0.2 wt%) standard
252 deviation (Table 2). Secondary standards including Durango apatite, which contains a known
253 Cl concentration of 0.41 wt% (Kusebauch et al. 2015) were used to ensure accurate Cl
254 analysis. We obtained an average of 0.412 wt% Cl with a standard deviation of 0.013% for
255 84 analyses.

256

257

RESULTS

258 All experiments, except those at NaCl saturation, were performed at 1400 °C and 1.5
259 GPa, using the CCO buffer ($f(O_2) = -7.17$ log units). All run conditions, the Cl concentrations
260 in the resultant glass phases, and the calculated Cl fugacities are given in Table 2. Complete
261 analyses of the silicate glass products are presented in supplementary Table S1. In order to
262 compare the results obtained at different Cl fugacities, and, considering that Cl solubility is
263 proportional to the Henry's Law relationship derived from reaction (2), we define the
264 *chloride capacity* (C_{Cl} ; Table 2) as:

$$265 \quad C_{Cl} = \frac{Cl \text{ (wt\%)}}{\sqrt{f(Cl_2)}} \times \sqrt[4]{f(O_2)}$$

266

((5))

267 We calculated the ferric-ferrous ratio of each experiment using the equation of Kress and
268 Carmichael (1991) and adjusted the FeO and Fe₂O₃ contents of our products accordingly.

269

270 **Henry's Law and melt composition**

271 Figure 3 shows the Cl contents of melts of a wide range of compositions equilibrated
272 at different fugacities of Cl with oxygen fugacity controlled at the CCO buffer and
273 temperature and pressure of 1400 °C and 1.5 GPa respectively. As can be seen, Cl dissolution
274 in all seven melts follows Henry's Law to concentrations of between, depending on major
275 element composition, at least 0.5 wt% (dacite) and 2.6 wt % ($\text{An}_{50}\text{Di}_{28}\text{Fo}_{22}$) Cl. The effect of
276 composition is dramatic with more than an order of magnitude difference between Cl
277 contents (under constant $f(\text{O}_2)$, $f(\text{Cl}_2)$ conditions) of a low SiO_2 , high CaO haplobasalt, which
278 is rich in Cl and a high SiO_2 , low CaO dacite, poor in Cl. Specific compositional effects will
279 be discussed further below.

280

281 **Correlation of empirical compositional parameters with chloride capacity**

282 There are a number of empirical parameters which have been proposed as being
283 simple ways of representing the complexities of silicate melt compositions by a single
284 parameter. These are all basically ways of representing the degree of polymerisation of the
285 melt by assigning different roles to “network-forming” (e.g., SiO_2) and “network-modifying”
286 or depolymerising (e.g., Na_2O) oxide components. Since Cl is observed to replace oxygen in
287 the silicate matrix, it is logical to assume that chloride capacity is a function of the way in
288 which oxygen is bonded in the silicate melt.

289

290 *Optical basicity:* Optical basicity is a parameter which empirically allocates an electron donor
291 power (Lewis basicity) to each individual oxide in a silicate melt matrix (Banin et al. 1997).
292 Optical basicity, denoted, Λ , was proposed as a useful index of melt properties by Duffy and
293 Ingram (1971) and adapted by Duffy and Ingram (1976) and Duffy (2004) as follows:

294
$$\Lambda = \frac{\sum X_i n_i \Lambda_i}{\sum X_i n_i}$$

295 ((6))

296 In equation (6) X_i is the mole fraction of oxide i , n_i is the number of oxygen atoms of the
297 oxide, and Λ_i is the optical basicity of oxide i . As expected, optical basicity decreases with
298 increasing SiO_2 and Al_2O_3 contents and increases with CaO, MgO, and alkali concentrations.
299 Therefore, as anticipated from Figure 3, there is a strong positive correlation of chloride
300 capacity with optical basicity (Fig 4a).

301

302 *NBO/T*: A second empirical way of representing the properties of the oxygen atoms in a
303 silicate matrix is through the ratio of non-bridging oxygens to tetrahedrally coordinated
304 cations, NBO/T. The chemical rationale is that oxygen atoms which bridge between
305 tetrahedral Si and Al have different properties from those which terminate silicate chains or
306 are present in isolated tetrahedra. We calculated NBO/T following the approach of Mills
307 (1993). This derives Y_{NB} and X_{T} as follows for $\text{Fe}^{3+}/(\text{Fe}^{2+}+\text{Fe}^{3+}) < 0.3$ (Mills 1993) from the
308 mole fractions x of the different oxides:

309
$$Y_{\text{NB}} = \sum 2[x\text{CaO} + x\text{MgO} + x\text{FeO} + x\text{MnO} + x\text{Na}_2\text{O} + x\text{K}_2\text{O}] + 6x\text{Fe}_2\text{O}_3 -$$

310 $2x\text{Al}_2\text{O}_3$ ((7))

311
$$X_{\text{T}} = \sum x\text{SiO}_2 + x\text{TiO}_2 + 2x\text{P}_2\text{O}_5 + 2x\text{Al}_2\text{O}_3$$

312 ((8))

313
$$\frac{\text{NBO}}{\text{T}} = \frac{Y_{\text{NB}}}{X_{\text{T}}}$$

314 ((9))

315 Since Y_{NB} increases with CaO, MgO and alkali contents, NBO/T correlates positively with
316 optical basicity and chloride capacity as shown in Figure 4b.

317

318 *Ionic porosity*: This parameter is a calculation of the percentage of the melt volume
319 unoccupied by cations and anions and defined as (Dowty, 1980):

$$320 \quad Z = 100(1 - V_{ca}/V_L)$$

321 \quad \quad \quad ((10))

322 In equation (10) V_{ca} is the total volume occupied by constituent atoms (cations + anions) in
323 one gram of melt, and V_L is the melt volume (cm^3/g) calculated using the oxide partial molar
324 volumes as given by Lange and Carmichael (1987). We calculated the ionic porosity of each
325 product glass using the calculator presented in Iacono-Marziano et al. (2010). Their model
326 uses the parameters of Carroll and Stolper, (1993) with volumes of individual cations and
327 anions calculated from effective ionic radii given by (Shannon and Prewitt, 1969; Shannon,
328 1976), assuming spherical geometry. All melt compositions were recalculated to 100% before
329 calculating ionic porosity. Since ionic porosity generally decreases with increasing Ca, Mg,
330 and alkalis and increases with SiO_2 , chloride capacity correlates negatively with ionic
331 porosity (Fig. 4c).

332

333 *Larsen Index*: The Larsen index is a measure of the extent of differentiation of a melt,
334 defined as follows (Larsen, 1938):

$$335 \quad LI = \left[\left(\frac{1}{3} \text{SiO}_2 + \text{K}_2\text{O} \right) - \left(\text{FeO} + \frac{9}{10} \text{Fe}_2\text{O}_3 + \text{MnO} \right) + \text{CaO} + \text{MgO} \right] \quad (11)$$

336 This index (Fig 4d) has been used extensively to correlate Cl solubility with chemical
337 composition (e.g. Webster et al. 2009; Webster et al. 2015; Webster et al. 2018; Webster et

338 al. 2019). Given the positive term in SiO₂ and negative term in CaO, chloride capacity
339 correlates, as expected, negatively with the Larsen Index as shown in Figure 4d.

340

341 *Oxide mole fractions:* It is clear from Figure 4 and the preceding discussion that all of the
342 empirical compositional parameters considered provide reasonable descriptions of the
343 compositional dependence of chloride capacity over the broad compositional range
344 investigated. We were seeking, however, to identify subtle variations in chloride capacity due
345 to different cations of similar, but not identical chemical behaviour. We therefore fitted the
346 logarithm of the chloride capacity using SPSS software to compositional terms for each of the
347 constituent oxides, with each oxide recalculated as the mole fraction on a single cation basis.
348 We used stepwise linear regression applying the F-test ($\alpha=0.05$) to determine which
349 compositional parameters are significant. In order to ensure that the compositional terms
350 approach zero at infinite temperature, the oxide mole fractions were divided by temperature.
351 Terms that were not significant at an F of 0.05 were excluded. This approach resulted in the
352 following equation:

$$353 \log C_{Cl} = 1.601 + (4470X_{Ca} - 3430X_{Si} + 2592X_{Fe} - 4092X_K - 894P)/T \quad (12)$$

$$354 R^2=0.96; \text{ standard error} = 0.089$$

355 Surprisingly, in view of previous results and inferences (Stebbins and Du 2002;
356 Sandland et al. 2004; Evans et al. 2008; McKeown et al. 2011), our data do not require terms
357 for Mg and Na contents. The influences of these cations have plausibly been subsumed into
358 the terms for Ca, Si, and K. In order to take account of pressure and temperature effects on
359 chloride capacity we regressed the data together with the data from Thomas and Wood,
360 (2021) in which the pressure and temperature effects on chloride capacity for the
361 An₅₀Di₂₈Fo₂₂ composition and the Icelandic basalt were independently established. As before

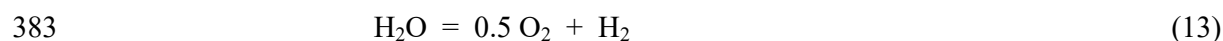
362 we found that the term in reciprocal temperature is insignificant, and that the P/T term is
363 required. The value of the latter in equation $\{\{\text{auth: ok?}\}\text{OK like this }\}$ (12) is within
364 uncertainty of the same terms previously obtained by regression and is close to the value
365 expected for the replacement of O^{2-} by 2Cl^- (Thomas and Wood 2021). A spreadsheet
366 enabling the calculation of Cl fugacities and chloride capacities as defined in equations (12)
367 and (15) is provided as the electronic supplement, '*ChlorCalc_v1*'.

368

369 DISCUSSION

370 The effects of H_2O on chloride capacity

371 There are a considerable number of studies of the partitioning of Cl and other
372 elements between silicate melts and aqueous fluids (Shinohara et al. 1989; Métrich and
373 Rutherford, 1992; Webster, 1992; Kravchuk and Keppler, 1994; Webster and Rebbert, 1998;
374 Bureau et al. 2000; Signorelli and Carroll 2000; Signorelli and Carroll 2002; Botcharnikov et
375 al. 2007; Chevychelov et al. 2008; Stelling et al. 2008; Alletti et al. 2009; Webster et al.
376 2009; Zajacz et al. 2012; Alletti et al. 2014; Beermann et al. 2015; Botcharnikov et al. 2015).
377 In general, however, because of the difficulties of fluid separation and analysis, authors
378 calculate the composition of the fluid by mass balance from the starting composition and the
379 measured melt composition. This approach works reasonably well for Cl, but concentrations
380 of charge-balancing cations in the fluid are difficult to estimate. This is important because for
381 experiments performed at fixed $f(\text{O}_2)$ or fixed $f(\text{H}_2)$, the Cl_2 fugacity is related to the HCl
382 fugacity via the equilibria:



385 If the concentrations of charge balancing cations, such as Na, Ca, and K are known, then any
386 Cl in excess of charge balance can be allocated, approximately, to HCl. If only Cl is known,
387 however, the fugacity of HCl must either be calculated by allocating all Cl to HCl or by
388 arbitrarily subtracting some fraction of the Cl as “bonded with other cations” in the fluid.

389 Bearing in mind these difficulties we attempted to incorporate the effects of H₂O on
390 chloride capacities using melt-aqueous fluid Cl partitioning data on a phonolite at 1000 °C
391 and 10-250 MPa (Alletti et al. 2014). In this case, the authors have calculated the Cl content
392 of the fluid as HCl. For the experiments of Alletti et al. (2014) we used the Modified Redlich
393 Kwong equation of state for H₂O-H₂-HCl fluids with parameters for H₂O, H₂ (Holloway,
394 1977), and HCl (Prausnitz et al. 1999). This enabled us to calculate the Cl₂ fugacity of each
395 experiment using the equilibrium constant for equilibria (13) and (14) from the NIST-JANAF
396 thermochemical tables (<https://janaf.nist.gov/>).

397 Adding the 23 data points from Alletti et al. (2014) to our 62 data points and
398 performing a stepwise linear regression with the same approach as before we obtained:

$$399 \log C_{Cl} = 0.571 + (4873X_{Ca} - 3803X_{Si} + 2724X_{Fe} + 1891 - 943P)/T \quad (15)$$

400 $R^2=0.94$; standard error = 0.117

401 The important points to note are as follows: 1) Although we added the H₂O contents (0.6-4.3 wt%) in mole
402 fractions (0.04-0.26) as a parameter to the regression, the term in H₂O was not significant at the $\alpha=0.05$ level. 2)
403 The X_{Ca} , X_{Si} , X_{Fe} , and P/T terms are very similar in equations (12) and (15) implying that they are quite robust.
404 3) The temperature range of the data has been extended by a further 200 °C, which has required the introduction
405 of a term in 1/T. **{{AU: The authors need to provide further discussion of this sentence. I see no difference**
406 **in the 1/T terms in Equations 12 and 15. D.B.}Don has misread the equations. (12) and (15) have almost**
407 **identical P/T terms, but (15) has the term 1891/T and no such term is present in (12).}** The latter was found
408 to be not significant in our earlier study, presumably because of the more restricted temperature range employed
409 in our higher-pressure experiments.

410 Although other data in the literature have the potential to provide additional
411 compositional constraints, we have found it difficult to treat all studies in a consistent way.
412 We therefore present equation (15) as an illustration of the extension of our approach to
413 lower temperatures and moderate H₂O contents (up to 4.3%) on the understanding that a

414 systematic addition of H₂O to experiments using our buffering approach is required to better
415 resolve the question of the effects of H₂O on chloride capacity.

416

417

IMPLICATIONS

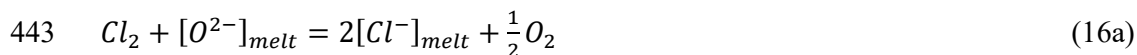
418 H₂O and HCl degassing

419 Thomas and Wood, (2021) observed that Cl should not degas significantly as HCl
420 during ascent of basalt until pressures are well below 10 MPa, and that most Cl would be
421 degassed below 2 MPa, equivalent to ~ 80 meters depth. In Figure 5 we illustrate the effect of
422 composition on these estimates made by assuming that the evolved gas is dominantly H₂O.
423 We considered 4 melts, basalt, andesite, dacite, and rhyolite (anhydrous compositions in
424 Table 1) and estimated their dry liquidus at 50 MPa using *alphaMELTS for Python*
425 (Antoshechkina and Ghiorso 2018). We then calculated the H₂O content of each melt at 50
426 MPa and a temperature just above the dry liquidus (1220, 1200, 1080 and 1030 °C for basalt,
427 andesite, dacite, and rhyolite respectively) using a spreadsheet from Moore et al. (1998). The
428 latter yields saturated H₂O contents of between 2.13 (andesite) and 2.34 (rhyolite) weight% at
429 50 MPa (Table 3).

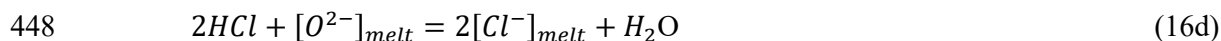
430 In order to calculate the degassing path of Cl from the melts of interest, we estimated
431 their chloride capacities from equation (15) at an oxygen fugacity corresponding to the
432 fayalite-magnetite-quartz (FMQ) buffer, assumed H₂O saturation at 50 MPa, and applied
433 starting concentrations of 2000 ppm (0.2 wt%) Cl in all 4 melts. We then calculated the
434 amounts of H₂O and the dominant chloride species, HCl (Shinohara et al. 1989), degassed in
435 H₂O-HCl fluids from 50 to 0.1 MPa in 0.5 MPa intervals. Although, as before, we adopted
436 the Modified Redlich Kwong (MRK) equation of state for the H₂O-H₂-HCl gas phase,
437 fugacity coefficients for H₂ and HCl in the water-rich gas are so close to 1.0 that they could

438 have been assumed to be perfect gases with little change in the result.

439 It should be noted that, although the chloride capacity depends on $f(O_2)$, the degassing
440 of HCl is actually independent of oxygen fugacity. This can be seen by combining the
441 dissolution reaction of Cl in the melt with those for the dissociation of H_2O and formation of
442 HCl:



446 If we subtract reaction (16b) from (16a) and add (16c) we eliminate oxygen and Cl fugacities
447 and obtain:



449 Thus, the results shown in Figure 5 are independent of the oxygen fugacity provided that Cl
450 is dominantly degassed as HCl, which is the case in low pressure, high temperature
451 environments.

452 As can be seen in Figure 5, and anticipated from equation (15), the effects of Ca, Fe,
453 and Si on chloride capacity result in basaltic melts having much higher Cl solubilities and
454 lower tendencies to degas HCl than silica-rich melts poor in Ca and Fe. We calculate that a
455 basaltic melt containing 2000 ppm (0.2 wt%) Cl at 50 MPa will degas only 0.03 wt% Cl
456 during the ascent to the surface. In contrast, andesitic, dacitic, and rhyolitic melts, initially
457 containing 0.2 wt% Cl, should degas 0.08, 0.12, and 0.17 wt % respectively during ascent.
458 Almost half of the degassing takes place at pressures below 3 MPa (110 meters depth),
459 conditions under which the gas pressure would be expected to fluctuate substantially due to
460 melt migration and convection. The calculations therefore show that HCl would degas mainly

461 in the very uppermost parts of a volcanic edifice or during an eruption. This conclusion is
462 consistent with the observations of Saito et al. (2005) at Miyakejima Volcano, Japan, who
463 found that Cl remains in the melt, even after shallow degassing, and thus only degasses at
464 very low pressures, well after H₂O and CO₂ (Spilliaert et al. 2006). More recently, Edmonds
465 et al. (2009) placed constraints on the depths of Cl degassing at Kilauea, and found that Cl
466 degasses at depths of 35 meters or less, at pressures below 1 MPa, and below pressures of
467 sulfur degassing. This conclusion coincides with the findings of (Lesne et al. 2011) who
468 performed experiments to simulate decompression-driven, closed-system degassing of
469 basaltic magma in equilibrium with an H-C-O-S-Cl fluid. They found that dissolved Cl
470 displayed minimal loss to the fluid over a wide pressure range, remaining in the melt from
471 400 MPa to 25 MPa. Finally, the enrichment of Cl in thermal springs is also believed to
472 reflect Cl degassing at very shallow conditions (Li et al. 2015).

473

474 **NaCl activities in Cl-containing silicate melts**

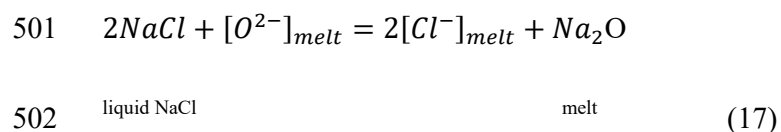
475 Brine separation from melts is an important process in the generation of many economically
476 important ore deposits (Cline and Bodnar 1994; Bruce et al. 1999; Bortnikov 2006; Gleeson
477 and Turner 2007; Wilkinson 2013; Blundy et al. 2015; Nshimiyimana et al. 2015; Essarraj et
478 al. 2016; Blundy et al. 2021). Understanding of the depths at which saturation occurs is
479 fundamental to the development of an understanding of the process in specific environments.

480 In order to provide a basis for understanding brine saturation, Webster and De Vivo,
481 (2002) and Webster et al. (2015) performed experiments in which silicate melts of a wide
482 range of compositions were saturated with chloride-rich liquids, the latter being dominated by
483 NaCl and KCl. In some cases, hydrous chlorides such as FeCl₂·4H₂O and CaCl₂·2H₂O were
484 added instead of, or in addition to, NaCl and KCl, as was oxalic acid, as a source of H₂O and

485 CO₂, as well as PtCl₄. Importantly, the experimental products were very close to chloride
486 saturation and Webster et al. (2015) used the results to model the solubility of chloride in
487 silicate melts.

488 In order to connect our chloride capacity measurements to the chloride saturation
489 experiments of Webster and De Vivo, (2002) and Webster et al. (2015), we performed two
490 experiments at 1100 °C and 1.0 GPa in which a phonolitic melt was saturated in NaCl at two
491 different oxygen fugacities. In these cases, the activity of NaCl is 1.0 at 1100°C/1 GPa while
492 the earlier experiments, performed at 1 bar to 0.7 GPa and 700 to 1250 °C, were saturated in
493 liquids with significantly lower, but unknown NaCl activities. The important consideration is,
494 however, that comparison of our data with the earlier results of Webster and De Vivo, (2002)
495 and Webster et al. (2015) should be based on NaCl activities as close to 1.0 as possible. We
496 therefore excluded all of the earlier experiments in which Cl was added as PtCl₄ and those in
497 which H₂O and/or Ca and Mg chlorides were added. This left 100 experiments of Webster
498 and De Vivo, (2002) and Webster et al. (2015) in which Cl was added as NaCl and KCl and
499 in which the NaCl activity was high.

500 The experimental data were considered in terms of the equilibrium:



503 We rearrange the equilibrium constant for equation ((17)) to yield:

$$504 \quad \log \left(\frac{a_{Cl^-}_{melt}}{a_{O^{2-}}_{melt}{}^{0.5}} \right) = \log(a_{NaCl}) - 0.5 \log(a_{Na_2O}) + 0.5 \log K \quad (18)$$

505 The term on the left-hand side is directly related to the chloride capacity through equilibrium
506 (2). It must therefore have the same compositional dependence on the chloride capacity as
507 that derived from equations (12) or (15). We therefore used equation (12) and calculated an

508 “effective” activity ratio $\left(\frac{a_{Cl^-}^{melt}}{a_{O^{2-}}^{melt}}\right)^{0.5}$ from the Cl concentration (Cl) in wt % and oxide mole
509 fractions on a single cation basis :

$$510 \log\left(\frac{a_{Cl^-}^{melt}}{a_{O^{2-}}^{melt}}\right)^{0.5} = \log(Cl^-) - (4470X_{Ca} - 3430X_{Si} + 2592X_{Fe} - 4092X_K)/T \quad (19)$$

511 In equation (19) Cl⁻ denotes the wt% concentration of Cl in the melt and the compositional
512 terms on the right-hand side remove the compositional dependence of $\left(\frac{a_{Cl^-}^{melt}}{a_{O^{2-}}^{melt}}\right)^{0.5}$ as
513 described by equation (12). This gave us 102 data points of known values of pressure,
514 temperature, and the left-hand side of equation (18). **{{AU: Please query the authors as to
515 whether they mean 18 or 19 at this point. D.B. We do mean (18)}}** Using the standard
516 state for NaCl as pure liquid NaCl at the pressure and temperature of interest, we assumed
517 that the activity of NaCl in our NaCl-saturated experiments was 1.0 and that the data of
518 Webster and De Vivo (2002) and Webster et al. (2015) referred to slightly lower activity
519 values of 0.8. We believe that the latter is a reasonable assumption since NaCl activity values
520 of about 0.5 fitted less well with our data for which the NaCl activity is known. We then
521 regressed $\log(a_{NaCl}) - \log\left(\frac{a_{Cl^-}^{melt}}{a_{O^{2-}}^{melt}}\right)^{0.5}$ against 1/T, P/T, and oxide mole fractions as before
522 in order to obtain the compositional dependence of NaCl saturation. The activity of Na₂O
523 (equation 18) is combined with the composition, temperature, and pressure terms. Using
524 stepwise linear regression and applying the F-test as before we obtained:

$$525 \log(a_{NaCl}) - \log\left(\frac{a_{Cl^-}^{melt}}{a_{O^{2-}}^{melt}}\right)^{0.5} = -0.06 + (6901X_{Ca} + 3484X_{Na} - 2417)/T \quad (20)$$

526 The standard error of the fit is 0.124 and $r^2 = 0.85$. We can now put (19) and (20) together to
527 obtain the Cl content of the melt at any NaCl activity as follows:

$$\begin{aligned} 528 \quad \log(Cl^-) &= \log(a_{NaCl}) + 0.06 - (2431X_{Ca} + 3430X_{Si} - 2592X_{Fe} + 3484X_{Na} + \\ 529 \quad &4092X_K - 2417)/T \end{aligned} \quad ((21))$$

530 It is interesting to note that the Cl content should not depend on oxygen fugacity $f(O_2)$ at
531 NaCl saturation as indicated by equation (17). We confirmed this supposition by performing
532 experiments at both the Re/ReO₂ (4 log $f(O_2)$ units above CCO) and the CCO buffers from
533 which Cl contents of 1.09 and 1.00 wt%, respectively were obtained (Table 2).

534 Figure 6 shows the calculated Cl contents of the same 4 melts as in Figure 5 plotted as
535 a function of NaCl activity. The form of equation (21) imposes a linear relationship between
536 NaCl activity and Cl content, but as can be seen, the major element composition has an
537 appreciable effect on NaCl solubility and saturation in natural silicate melts. Thus, for
538 example, we calculate that at 200 MPa and 900 °C, the basalt will contain 3.6% Cl (possibly
539 metastably) at NaCl saturation (activity = 1.0) while the rhyolite will reach NaCl saturation at
540 0.45 weight % Cl. The latter figure is similar to values measured in melt inclusions from
541 some felsic magmas (Webster et al, 2020) indicating that NaCl-rich brines are much more
542 likely to separate from felsic than from basic magmas. Equation (21), therefore, leads to a
543 means of using the compositions of melts to estimate the compositions of coexisting fluids,
544 specifically their NaCl contents at the conditions of fluid separation. In this we follow the
545 example of Webster et al. (2020) who used melt inclusion data from a large number of
546 localities to estimate whether or not the melts were in equilibrium with a hydrosaline liquid.

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556

557

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- 807

808

FIGURE CAPTIONS

809 **FIGURE 1.** A schematic showing the form of the relationship between the Cl content and the
810 Cl₂ fugacity established by Thomas and Wood (2021). The size of the Henry's Law region
811 depends on the major element composition.

812 **FIGURE 2.** Back-Scattered Electron (BSE) image of a typical experimental product, which
813 displays (i) separate and distinct phases of the silicate glass, metal chloride/iodide, and metal
814 and (ii) the CO₂ source as Ag₂CO₃.

815

816

817 **FIGURE 3.** This figure illustrates the minimum lengths of the Henry's Law, linear regions
818 for melts of different bulk composition at 1.5 GPa/1400°C. It also implies that SiO₂ and CaO
819 contents are likely important parameters in determining Cl solubility, as reflected in our fit
820 for equation (12).

821

822 **FIGURE 4.** Chloride capacity data at 1.5GPa/1400°C plotted against some of the more
823 relevant empirical parameters which aim to describe the degree of polymerisation and acid-
824 base behaviour of silicate melts. See text for definitions and discussion.

825

826 **FIGURE 5.** The expected losses of Cl as HCl from ascending magmas of different
827 composition. All 4 melts were assumed to contain 2000 ppm Cl initially and to begin losing
828 HCl at 50 MPa during isothermal ascent. In all 4 cases the fraction lost, as the surface is
829 approached, varies dramatically with composition where Rhyolite > Dacite > Andesite >
830 Basalt.

831

832 **FIGURE 6.** The calculated Cl contents of the same 4 compositions as in Figure 5 as a
833 function of the NaCl activity at 200 MPa and 900 °C. For a fixed NaCl activity the basalt is
834 calculated to contain ~8 times as much Cl as the rhyolite.

Table 1. Silicate melt compositions used for measuring chlorine solubility

Composition	SiO ₂	TiO ₂	Al ₂ O ₃	FeO _T	MnO
Icelandic basalt ^a	50.76	1.02	15.32	9.61	-
SM-Basalt ^b	40.76	-	10.52	16.25	-
MORB ^c	50.80	0.82	15.38	7.85	-
Low-Mg Basalt ^d	49.22	3.15	15.82	9.05	0.21
High-Mg Basalt ^e	42.51	4.10	9.54	13.16	0.18
CNMAS (Fo ₅ Di ₄₈ An ₄₇) ^f	48.06	-	16.49	-	-
CNMA-2 (En ₁₇ An ₄₃ Di ₄₀) ^g	49.61	-	15.36	-	-
CMAS (An ₅₀ Di ₂₈ Fo ₂₂) ^h	46.53	-	18.33	-	-
Lunar Basalt ⁱ	41.00	9.00	12.00	18.30	0.40
Martian basalt ^j	51.01	1.01	10.15	18.36	0.36
HED-Basalt-1 ^k	51.09	-	5.23	15.45	0.10
HED Basalt-2 ^k	52.39	0.02	6.67	15.41	0.08
Basanite ^l	45.14	2.47	11.33	12.22	0.19
Andesite ^m	62.85	0.62	18.30	4.01	-
High-Mg Andesite ⁿ	54.20	0.60	15.60	6.70	-
Dacite ^o	67.22	0.94	15.82	4.47	0.06
Obsidian ^p	74.35	-	12.87	1.51	0.07
Picrite ^q	49.06	2.01	9.41	11.30	0.17
Nephelinite ^r	43.78	2.42	15.32	10.44	0.31
Syn-Nephelinite ^s	39.95	2.76	13.50	11.79	0.28
Phonolite ^t	55.21	0.34	21.31	2.84	0.26
Syn-phonolite ^u	54.55	1.60	19.09	5.53	0.16
Granite ^v	74.74	-	14.92	-	-
Albite/Forsterite (Ab ₉₅ Fo ₅) ^w	69.92	-	18.95	-	-
Syn-Rhyolite-1 ^o	75.22	0.29	13.53	1.04	0.05
Rhyolite-2 ^x	73.66	0.22	13.45	1.25	0.03

FeO_T = FeO + Fe₂O₃

^aNatural Icelandic Basalt (Norris and Wood, 2017)

^bSynthetic Basalt (Sossi et al., 2019)

^cSynthetic Mid Ocean Ridge Basalt (MORB), by Kiseeva and Wood, (2013) based on Falloon et al.

^dNatural Low-Mg Basalt, El Hierro, Canary Islands, Tephrite, EGT17-01 (Taracsák et al., 2021)

- ^cNatural High-Mg Basalt, El Hierro, Canary Islands, Basanite, TNR14-01 (Taracsák et al., 2021)
- ^f1 bar eutectic composition (Osborn and Tait, 1952)
- ^g1 bar eutectic composition (Hytonen and Schairer, 1960)
- ^h1.5 GPa approximate eutectic composition, (Presnall et al., 1978)
- ⁱSynthetic Lunar Basalt model from Apollo 11
- ^jSynthetic Martian Basalt (Matzen et al., 2022)
- ^kSynthetic bulk silicate compositions of Vesta (Ashcroft and Wood, 2015)
- ^lSynthetic Basanite, modelled from the Nepheline basanite sample UT-70489 (Adam, 1990)
- ^mSynthetic Andesite (Carmichael et al., 1974)
- ⁿSynthetic High-Mg Andesite (Wood and Turner, 2009)
- ^oDacite and Rhyolite compositions based on STXB4y and STXG4y respectively (Muir et al., 2011)
- ^pNatural Lipari Obsidian LIP-17714 (Hunt and Hill, 1993)
- ^qNatural Picrite, Hawaii, HAW-16095 (Taracsák et al., 2021)
- ^rNatural Lacher See Nephelinite, LS-17980 (Taracsák et al., 2021)
- ^sSynthetic Nephelinite (Webb and Dingwell, 1990)
- ^tNatural Laacher See Phonolite, LS-17985 (Taracsák et al., 2021)
- ^uSynthetic Phonolite (Ridley, 1970)
- ^vAnhydrous granitic eutectic composition (Ebadi and Johannes, 1991)
- ^wSynthetic mixture of 95% Albite and 5% Forsterite
- ^xSynthetic Rhyolite made from the compositions of (Nockolds., 1954)
-

MgO	CaO	Na ₂ O	K ₂ O	P ₂ O ₅	Cr ₂ O ₃	NiO
9.19	12.26	2.01	-	-	-	-
15.10	16.69	-	-	-	-	-
10.44	12.62	1.37	-	-	-	-
4.20	9.38	4.77	1.99	1.32	-	-
13.46	11.34	2.79	1.05	0.69	-	-
12.30	21.75	0.90	-	-	-	-
14.27	19.25	1.29	-	-	-	-
17.82	17.33	-	-	-	-	-
8.00	10.00	0.60	-	-	-	-
11.94	6.72	-	-	-	-	0.45
22.60	4.60	0.58	-	-	0.57	0.10
15.99	6.33	0.02	-	-	0.17	0.13
13.59	9.82	2.16	0.23	-	-	-
3.49	6.89	3.37	1.04	-	-	-
9.40	9.60	2.60	1.30	-	-	-
1.45	3.40	2.12	4.24	0.27	-	-
0.05	0.74	3.93	5.11	-	-	-
16.99	8.08	1.74	0.37	0.22	-	-
4.25	11.71	5.39	3.79	1.22	-	-
7.86	12.94	4.54	3.32	1.55	-	-
0.12	1.82	8.15	8.56	0.05	-	-
1.76	4.07	9.06	3.64	0.12	-	-
-	-	6.61	3.72	-	-	-
2.85	-	7.30	-	-	-	-
0.22	0.77	2.18	6.60	0.08	-	-
0.32	1.13	2.99	5.35	0.07	-	-

id Green, (1987)

)

1)

4)



LOI	Total
	100.17
	99.32
	99.28
	99.11
	98.82
	99.50
	99.78
	100.01
	99.30
	100.00
	100.32
2.79	100.00
2.85	100.00
	100.57
	100.00
	99.99
	98.63
	99.35
	98.63
	98.49
	98.66
	99.58
	99.99
	99.02
	99.98
0.78	99.25



Table 2: Experimental conditions and compositions

Experiment ID	Silicate composition*	Time (hours)	Pressure (GPa)	Temperature (°C)
Ab/Fo-1	95% Albite - 5% Forsterite	1	1.5	1400
Ab/Fo-2	Ab/Fo + CaCO ₃	1	1.5	1400
Ab/Fo-3	Ab/Fo + CaCO ₃	1	1.5	1400
Ab/Fo-6	Ab/Fo + CaCO ₃	1	1.5	1400
AgI/CI-27†	Icelandic Basalt	1	1.5	1400
AgI/CI-005†	CMAS	1	1.5	1400
AgI/CI-024†	CMAS+ FeO	1	1.5	1400
AgI/CI-025†	CMAS+ FeO	1	1.5	1400
AgI/CI-026†	CMAS+ FeO	1	1.5	1400
CMAS+Na-1	CMAS + Na ₂ CO ₃	2	1.5	1400
CMAS+Na+2	CMAS + Na ₂ CO ₃	2	1.5	1400
Fo ₅ Di ₄₈ An ₄₇	CNMAS	2	1.5	1400
En ₁₇ An ₄₃ Di ₄₀	CNMAS-2	2	1.5	1400
Dacite-1	Dacite	2	1.5	1400
Dacite-2	Dacite	1	1.5	1400
TNR14-1	High Mg Basalt	1	1.5	1400
HA3-2	Basalt	2	1.5	1400
HA4-1	Basalt	1	1.5	1400
Rhyolite	Rhyolite	1	1.5	1400
LIP-17714	Lipari Obsidian	1	1.5	1400
AN-1	Andesite	4	1.5	1400
AN-2	Andesite	2	1.5	1400
SM-1	Basalt	2	1.5	1400
HiMgAnd	Andesite	1	1.5	1400
HAW-16095	Picrite	1	1.5	1400
EGT17-1	Low Mg Basalt	1	1.5	1400
KK3b-1	MORB	1	1.5	1400
KK3b-2	MORB	1	1.5	1400
Mars-1	Martian Basalt	1	1.5	1400
LS-17980	Nephelinite	1	1.5	1400
Basanite-1	Basanite	2	1.5	1400
Lunar-1	Lunar basalt	2	1.5	1400
KK-Rhy	Rhyolite	2	1.5	1400
Syn-Phono-1	Syn-Phonolite	2	1.5	1400
LS-17985-1	Phonolite	2	1.5	1400

LS-17985-2	Phonolite	2	1.5	1400
Granite-2	Granite	2	1.5	1400
Gran+Mg-1	Granite + MgO	2	1.5	1400
Gran+Mg-2	Granite + MgO	2	1.5	1400
Gran+Mg-3	Granite + MgO	2	1.5	1400
Phonolite-NaCl-1 [§]	80% LS-17985; 20% NaCl	0.5	1.0	1100
Phonolite-NaCl-2 [§]	80% LS-17985; 20% NaCl	2	1.0	1100
<i>Time series</i>				
Dacite-3	Dacite	0.75	1.5	1400
Dacite-4	Dacite	0.083	1.5	1400

Cl% error in () is 2 stdev

*Starting silicate melt compositions presented in Table 1

† Experiments originally presented in Thomas and Wood, (2021)

§ $f(\text{Cl}_2)$ and C_{Cl} calculated using *ChlorCalc_v1* (Spreadsheet available in the supplementa

C_{Cl} = Chloride capacity, OB = Optical Basicity, IP = Ionic Porosity, LI = Larsen Index (see

Measured Cl ^{glass} wt%	Buffer/Silic ate by mass	AgI/AgCl	Final Molar Cl/(Cl+I)	Molar Ag/(Ag+Pt)	<i>f</i> (O ₂) buffer	<i>log f</i> (O ₂)
0.56 (0.02)	75/25	75/25	0.325	0.879	CCO	-7.17
1.41 (0.06)	75/25	75/25	0.276	0.943	CCO	-7.17
2.75 (0.05)	75/25	75/25	0.183	0.812	CCO	-7.17
0.46 (0.01)	80/20	75/25	0.123	0.892	CCO	-7.17
1.6 (0.03)	50/50	75/25	0.209	0.778	CCO	-7.17
2.55 (0.04)	75/25	75/25	0.198	0.844	CCO	-7.17
2.54 (0.06)	75/25	75/25	0.198	0.887	CCO	-7.17
2.70 (0.19)	75/25	75/25	0.184	0.864	CCO	-7.17
3.49 (0.28)	75/25	75/25	0.120	0.903	CCO	-7.17
2.15 (0.06)	75/25	75/25	0.227	0.800	CCO	-7.17
2.32 (0.1)	75/25	75/25	0.214	0.836	CCO	-7.17
2.41 (0.14)	75/25	75/25	0.208	0.937	CCO	-7.17
2.60 (0.13)	75/25	75/25	0.194	0.793	CCO	-7.17
0.46 (0.08)	75/25	75/25	0.332	0.854	CCO	-7.17
0.17 (0.01)	75/25	90/10	0.142	0.776	CCO	-7.17
2.23 (0.12)	75/25	75/25	0.221	0.913	CCO	-7.17
1.62 (0.16)	75/25	75/25	0.265	0.882	CCO	-7.17
1.75 (0.2)	75/25	75/25	0.254	0.858	CCO	-7.17
0.27 (0.03)	75/25	75/25	0.340	0.812	CCO	-7.17
0.27 (0.03)	75/25	75/25	0.340	0.832	CCO	-7.17
0.72 (0.03)	25/75	75/25	0.227	0.785	CCO	-7.17
0.90 (0.05)	75/25	75/25	0.306	0.893	CCO	-7.17
3.05 (0.16)	75/25	75/25	0.158	0.938	CCO	-7.17
1.71 (0.03)	75/25	75/25	0.257	0.916	CCO	-7.17
1.90 (0.14)	75/25	75/25	0.244	0.947	CCO	-7.17
1.40 (0.02)	75/25	75/25	0.276	0.837	CCO	-7.17
1.13 (0.02)	25/75	75/25	0.130	0.707	CCO	-7.17
1.70 (0.04)	75/25	75/25	0.257	0.754	CCO	-7.17
2.02 (0.2)	75/25	75/25	0.236	0.961	CCO	-7.17
1.91 (0.03)	75/25	75/25	0.244	0.906	CCO	-7.17
2.06 (0.03)	75/25	75/25	0.234	0.897	CCO	-7.17
2.03 (0.09)	75/25	75/25	0.235	0.935	CCO	-7.17
0.15 (0.02)	75/25	75/25	0.347	0.948	CCO	-7.17
0.83 (0.02)	75/25	75/25	0.310	0.764	CCO	-7.17
0.68 (0.07)	75/25	75/25	0.319	0.955	CCO	-7.17

0.44 (0.03)	75/25	90/10	0.170	0.943	CCO	-7.17
0.31 (0.10)	75/25	75/25	0.339	0.916	CCO	-7.17
0.61 (0.10)	75/25	75/25	0.323	0.770	CCO	-7.17
0.67 (0.14)	75/25	75/25	0.320	0.918	CCO	-7.17
0.78 (0.10)	75/25	75/25	0.313	0.844	CCO	-7.17
1.09 (0.10)	-	-	-	-	RRO	-6.77
1.00 (0.12)	-	-	-	-	CCO	-10.31
0.47 (0.06)	75/25	75/25	0.330	0.856	CCO	-7.17
0.50 (0.17)	75/25	75/25	0.329	0.854	CCO	-7.17

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: text). RRO=Re/ReO2 buffer

$f(\text{Cl}_2)$	C_{cl}	OB	NBO/T	IP	LI
8.08E-04	0.32	0.53	0.00	72.56	20.66
5.05E-04	1.01	0.56	0.27	71.12	8.01
2.98E-04	2.57	0.58	0.57	69.81	-2.88
1.12E-04	0.70	0.58	0.38	70.54	5.54
4.24E-04	1.25	0.58	0.57	69.60	-5.10
3.24E-04	2.29	0.60	0.94	67.24	-18.22
2.94E-04	2.39	0.61	1.09	66.95	-23.01
2.68E-04	2.66	0.62	1.21	66.86	-25.94
1.04E-04	5.52	0.64	1.56	65.72	-34.06
4.76E-04	1.59	0.61	1.03	67.79	-13.33
3.89E-04	1.90	0.61	0.99	67.33	-17.34
2.92E-04	2.28	0.60	0.89	67.66	-16.97
3.52E-04	2.24	0.60	1.00	67.72	-16.44
8.90E-04	0.25	0.53	0.01	72.86	22.14
1.98E-04	0.20	0.53	0.00	73.03	23.44
3.47E-04	1.93	0.60	1.14	68.79	-18.68
5.32E-04	0.67	0.59	1.50	67.19	-23.23
5.18E-04	1.24	0.58	0.93	68.71	-9.84
1.04E-03	0.14	0.52	0.00	73.51	30.83
9.85E-04	0.14	0.52	0.00	73.49	29.18
4.92E-04	0.52	0.55	0.15	71.76	13.02
6.93E-04	0.55	0.55	0.15	71.72	11.17
1.67E-04	3.81	0.62	1.51	66.32	-28.16
4.65E-04	1.28	0.58	0.58	69.72	-4.45
3.93E-04	1.55	0.59	0.88	69.27	-12.20
6.43E-04	0.89	0.57	0.28	71.59	5.24
2.00E-04	1.29	0.59	0.72	69.45	-10.45
6.88E-04	1.05	0.58	0.57	69.45	-5.74
3.57E-04	1.73	0.60	1.14	68.09	-20.24
4.27E-04	1.49	0.60	0.62	69.64	-9.56
4.00E-04	1.66	0.59	0.93	68.96	-12.73
3.75E-04	1.69	0.60	0.78	70.90	-14.80
7.91E-04	0.09	0.52	0.00	73.28	27.25
9.72E-04	0.43	0.55	0.07	72.20	16.79
6.61E-04	0.43	0.56	0.00	72.06	21.84

1.92E-04	0.51	0.57	0.02	71.93	21.01
8.08E-04	0.18	0.52	0.00	73.32	28.08
1.04E-03	0.31	0.54	0.10	72.34	20.89
7.16E-04	0.40	0.54	0.15	72.09	19.03
8.09E-04	0.44	0.54	0.20	71.71	16.31
2.70E-03	0.42	0.57	0.00	72.67	21.28
4.46E-05	0.40	0.57	0.01	72.59	19.39
8.78E-04	0.26	-	-	-	-
8.77E-04	0.27	-	-	-	-

Table 3. Normalised silicate melt compositions at water saturation

Composition	Temperature (°C)	SiO ₂	TiO ₂	Al ₂ O ₃	FeO _T	MnO	MgO	CaO
Icelandic basalt	1220	49.57	1.00	14.96	9.38	-	8.97	11.97
Andesite	1200	61.16	0.61	17.81	3.91	-	3.40	6.70
Dacite	1080	65.72	0.92	15.47	4.37	0.06	1.42	3.32
Rhyolite	1030	73.48	0.28	13.21	1.02	0.05	0.21	0.75

*H₂O contents are calculated from Moore et al., (1998) at 50 Mpa, using anhydrous compositions (Table 3)

Na ₂ O	K ₂ O	P ₂ O ₅	H ₂ O*	Total
1.97	-	-	2.18	100.00
3.28	1.01	-	2.13	100.00
2.07	4.15	0.26	2.24	100.00
2.13	6.45	0.08	2.34	100.00

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Fig 1

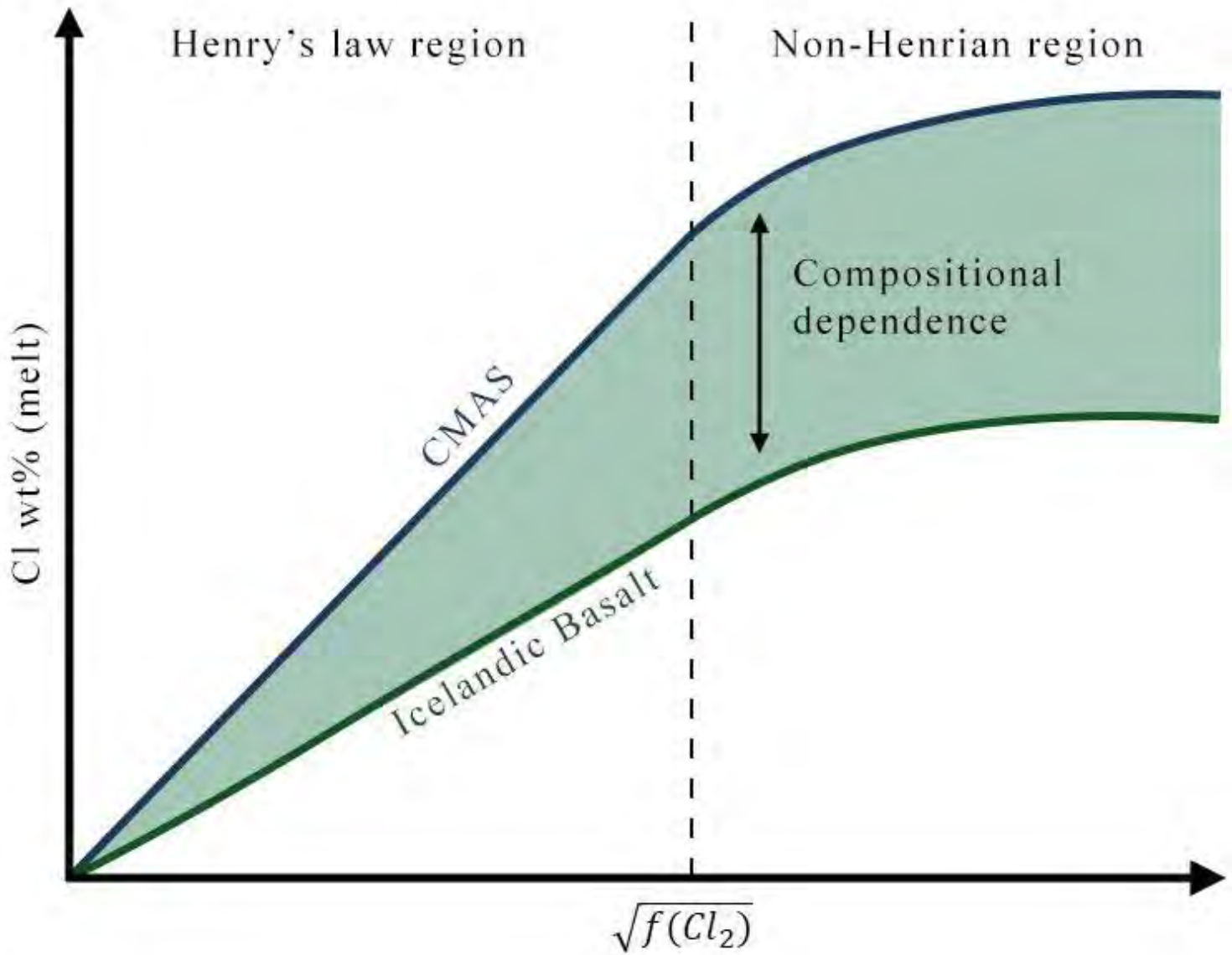


Fig 2

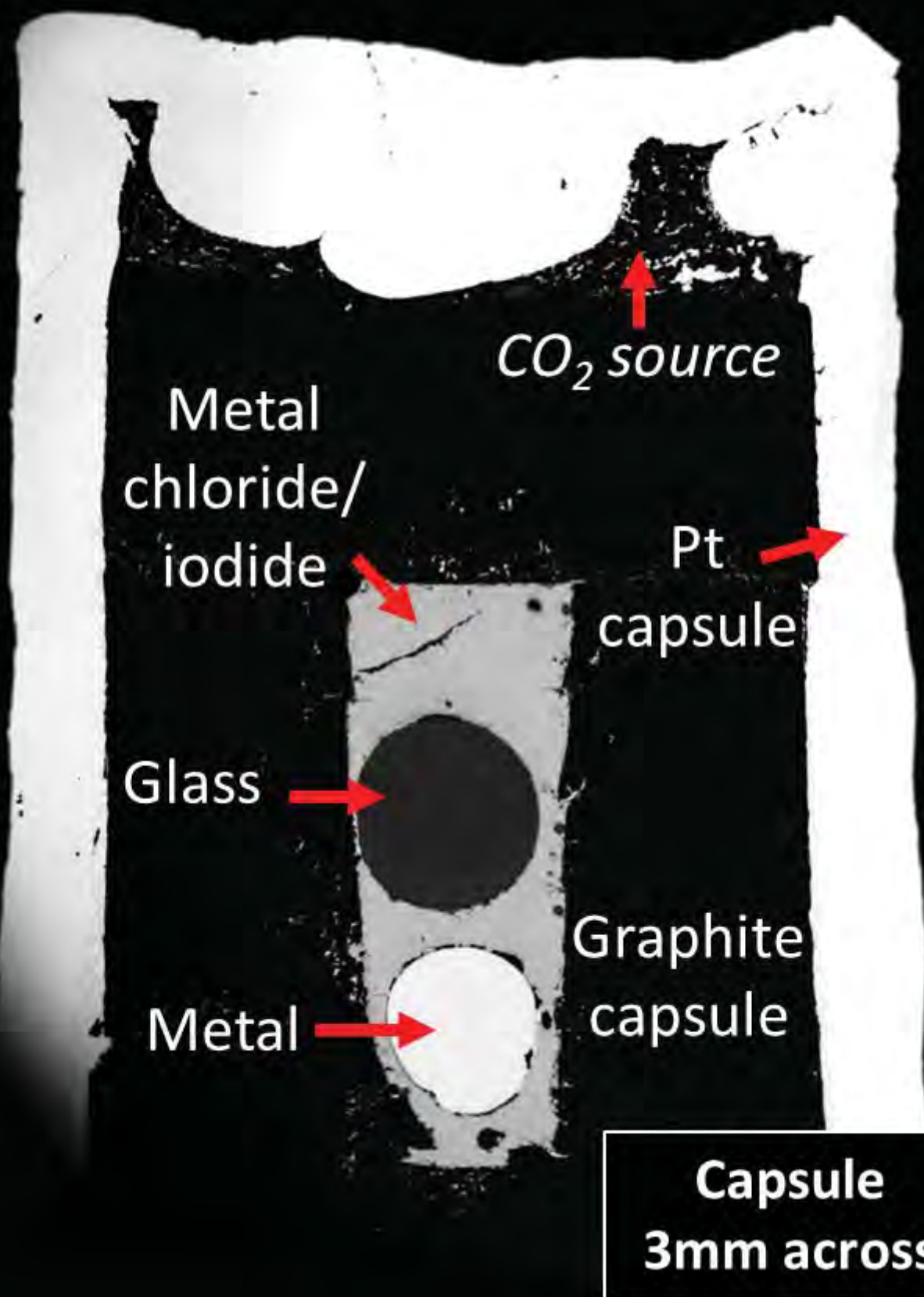


Fig 3

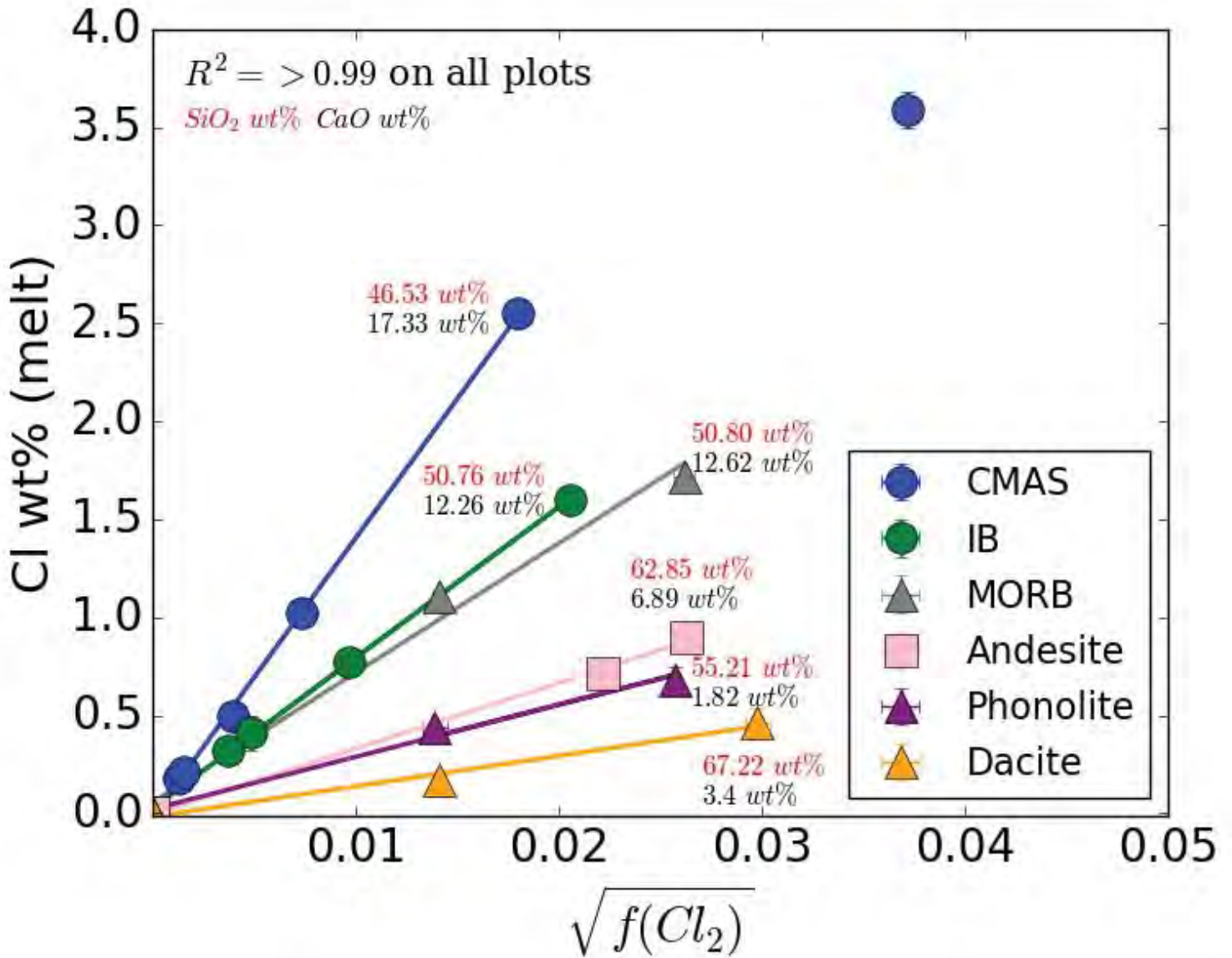


Fig 4

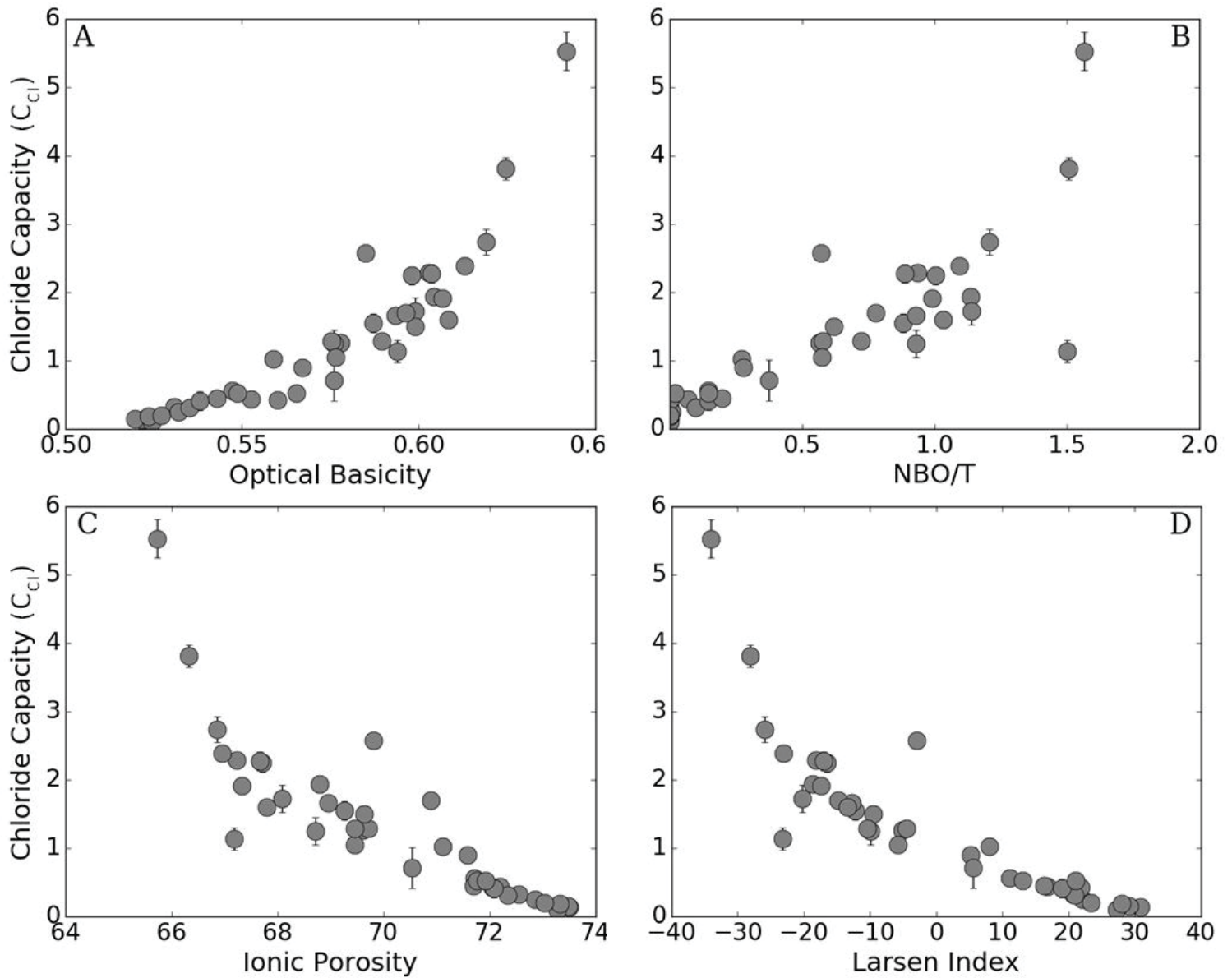


Fig 5

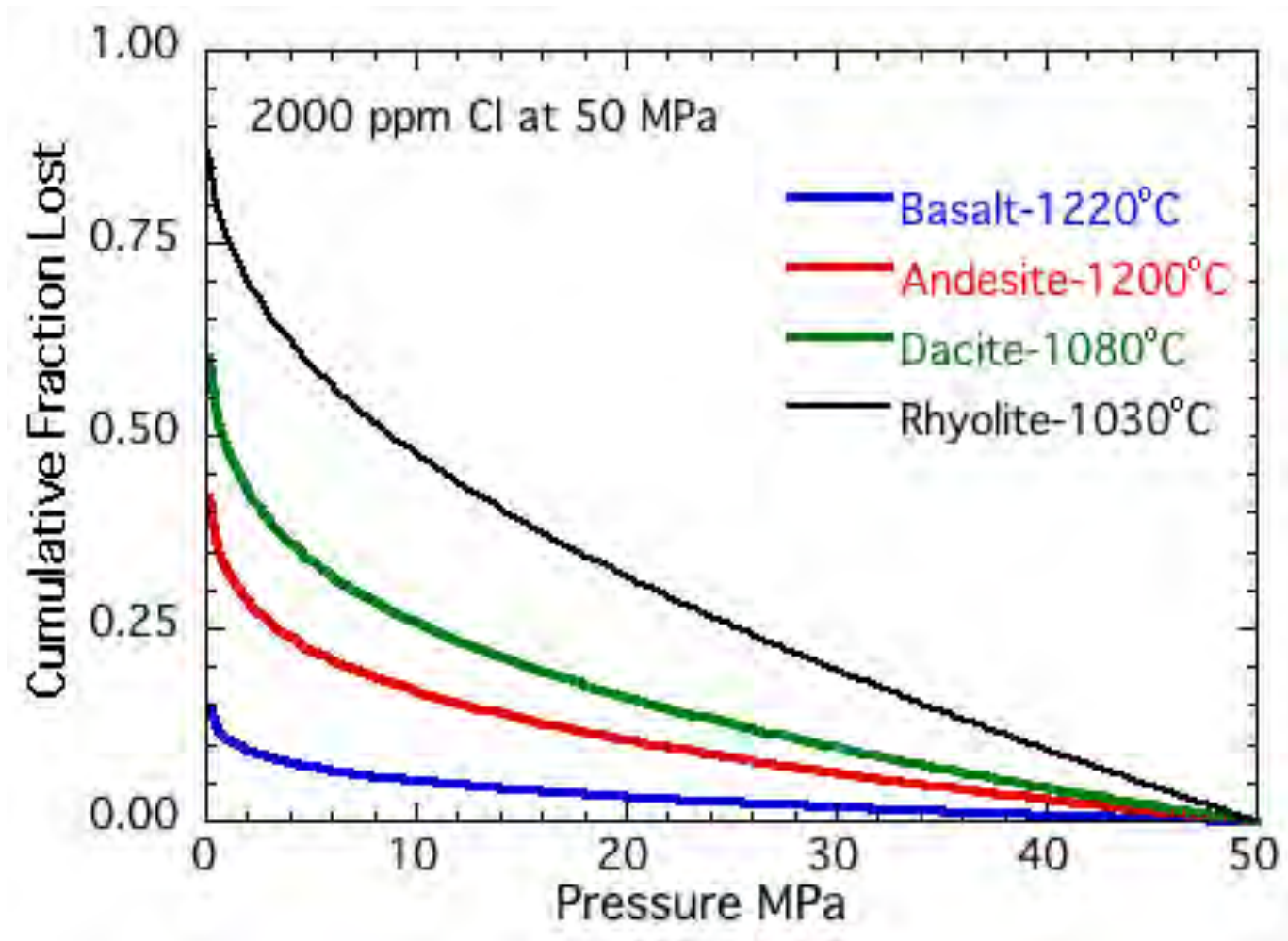


Fig 6

