

The CO₂–H₂O system: IV. Empirical, isothermal equations for representing vapor-liquid equilibria at 110–350 °C, $P \leq 150$ MPa

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ABSTRACT

Empirical formulae are presented for calculating vapor-liquid equilibria (VLE) in the CO₂-H₂O system at 10 temperatures between 110 and 350 °C. At each temperature, separate functions are used to represent the bubble- and dew-point boundary curves that: originate at the saturation vapor pressure of water ($P_{\text{sat}}^{\text{H}_2\text{O}}$) at $X_{\text{CO}_2} = 0$; diverge with increasing pressure up to $\sim P(X_{\text{CO}_2}^{\text{max}})$ where $\partial P/\partial X_{\text{CO}_2} = +\infty$ along the dew-point curve; then converge with increasing pressure above $P(X_{\text{CO}_2}^{\text{max}})$. At temperatures below 265 °C and pressures $> P(X_{\text{CO}_2}^{\text{max}})$, the compositions of coexisting liquid and vapor [$X_{\text{CO}_2}^{\text{L(V)}}$ and $X_{\text{CO}_2}^{\text{V(L)}}$] do not converge completely with increasing pressure due to the absence of critical behavior. Thus, relatively simple functions suffice to accurately represent VLE at those temperatures. In contrast, at $T > 265$ °C, $X_{\text{CO}_2}^{\text{L(V)}}$ and $X_{\text{CO}_2}^{\text{V(L)}}$ converge rapidly as P approaches P_c (the critical pressure in the CO₂-H₂O system at a given temperature between 265 and 374 °C and $P \leq 215$ MPa). For those temperatures, therefore, more complex VLE formulae are required to achieve close representation of phase relations. For dew-point equations, this includes adding an exponential “correction term” to ensure that $\partial P/\partial X_{\text{CO}_2} = 0$ at the critical points indicated by corresponding bubble-point functions.

Stable liquid-vapor coexistence in mixed-volatile systems requires $f_i^{\text{L}} = f_i^{\text{V}}$ (isofugacity conditions) for all “i” (volatile components) in the two fluid phases. Thus, the equations presented in this paper specify numerous P - T - X conditions where $f_{\text{H}_2\text{O}}^{\text{L}} = f_{\text{H}_2\text{O}}^{\text{V}}$ and $f_{\text{CO}_2}^{\text{L}} = f_{\text{CO}_2}^{\text{V}}$ in the CO₂-H₂O system. These results have important applications in the ongoing effort to develop a more rigorous thermodynamic model for CO₂-H₂O fluids at geologically relevant temperatures and pressures.