

1 Experimental Determination of Solubility Constants of Saponite at  
2 Elevated Temperatures in High Ionic Strength Solutions,  
3 Revision 1

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11

12 **ABSTRACT**

13 Saponite occurs in a wide range of environments from hydrothermal systems on  
14 the Earth to surface deposits on Mars. Of practical importance is that Mg-saponite forms  
15 when glasses for nuclear waste are altered in Mg-bearing aqueous solutions. In addition,  
16 saponite is favorably considered as candidate buffer materials for the disposal of high-  
17 level nuclear waste and spent nuclear fuel in harsh environments. However, the  
18 thermodynamic properties, especially for Mg-saponites, are not well known. Here the  
19 author synthesized Mg-saponite (with nitrate cancrinite) following a previously reported  
20 procedure and performed solubility experiments at 80 °C to quantify the thermodynamic  
21 stability of this tri-octahedral smectite in the presence of nitrate cancrinite. Then, in  
22 combination with the equilibrium constant at 80 °C for the dissolution reaction of nitrate  
23 cancrinite from the literature, the author determined the solubility constant of saponite at  
24 80 °C based on the solution chemistry for the equilibrium between saponite and nitrate  
25 cancrinite, approaching equilibrium from the direction of supersaturation, with an  
26 equilibrium constant of  $-69.24 \pm 2.08$  (2 $\sigma$ ) for dissolution of saponite at 80 °C.  
27 Furthermore, the author extrapolated the equilibrium constant at 80 °C to other  
28 temperatures (i.e., 50 °C, 60 °C, 70 °C, 90 °C and 100 °C) using the one-term  
29 isocoulombic method. These equilibrium constants are expected to find applications in  
30 numerous fields. For instance, according to the extrapolated solubility constant of  
31 saponite at 50 °C and 90 °C, the author calculated the saturation indexes with regard to  
32 saponite for the solution chemistry from glass corrosion experiments at 50 °C and 90 °C  
33 from the literature. The results are in close agreement with the experimental

34 observations. This example demonstrates that the equilibrium constants determined in  
35 this study can be used for reliable modeling of the solution chemistry of glass corrosion  
36 experiments.  
37

## 38 INTRODUCTION

39

40 Saponite, a tri-octahedral smectite, occurs in a wide range of environments. For  
41 instance, it occurs in igneous rocks as hydrothermal alteration products (e.g., Kohyama et  
42 al., 1973; April and Keller, 1992; Garvie and Metcalf, 1997), and in metamorphosed  
43 dolomitic limestone as hydrothermal products (e.g., Post, 1984). It also occurs as lake  
44 sediments and in volcanic rocks on seafloor (e.g., Desprairies et al., 1989; Cuevas et al.,  
45 2003; Kadir and Akbulut, 2003). Its occurrence in the Martian meteorites and its  
46 proposed occurrence in Mawrth Vallis region and Yellowknife Bay, Gale Crater on Mars  
47 (e.g., Bishop et al., 2013; Hicks et al., 2014; Bristow et al., 2015) generated enormous  
48 scientific interest. Most recently, saponite was also observed in an analog study of the  
49 hydrothermal alteration in the martian subsurface (e.g., Sueoka et al., 2019; Calvin et al.,  
50 2020).

51 Additionally, of practical importance and therefore particular interest is that  
52 saponite is relevant to the geological disposal of nuclear waste, as Mg-saponite has been  
53 observed as an alteration product when a borosilicate glass for nuclear waste is corroded  
54 (Thien et al., 2010) in Mg-containing solutions, as detailed below.

55 Mg-bearing groundwaters are common in the disposal concepts in various rock  
56 formations. For instance, salt formations have been recommended for nuclear waste  
57 isolation since the 1950's by the U.S. National Academy of Science (1957). Because of  
58 their excellent properties of high heat conduction, low permeability and a propensity to  
59 self-seal, rock salt is a viable candidate for a nuclear waste repository. Salt formations  
60 contain brines, which have relatively high concentrations of magnesium (Nishri et al.,

61 1988; Schussler et al., 2001; Xiong and Lord, 2008). For instance, the Q-brine at Asse,  
62 Germany, has a magnesium concentration of  $4.47 \text{ mol} \cdot \text{kg}^{-1}$  (Nishri et al., 1988; Schussler  
63 et al., 2001). When high level waste (HLW) glass is corroded in Mg-rich brines, Mg-  
64 bearing phyllosilicates form as part of the secondary phase assemblage (Strachan, 1983;  
65 Strachan et al., 1984; Grambow and Muller, 1989; Maeda et al., 2011). Although  
66 previously, and tentatively, identified as sepiolite (a member of the palygorskite family),  
67 more recent investigations have identified trioctahedral smectites, such as saponite with  
68 various stoichiometries, e.g.,  $(\frac{1}{2}\text{Ca}, \text{Na})_{0.66}\text{Mg}_6[(\text{Si}_{7.34}\text{Al}_{0.66})\text{O}_{20}](\text{OH})_4$  (e.g., Abdelouas et  
69 al., 1997; Thien et al., 2010; Zhang et al., 2012; Fleury et al., 2013; Debure et al., 2016;  
70 Aréna et al., 2017) as a reaction product. Note that in these more recent investigations,  
71 the concentration of Mg in solution is relatively low (milli-molal range), in accord with  
72 the dilute nature of pore water chemical compositions recovered from silicate-dominated  
73 prospective repositories (e.g., Gaucher et al., 2009). Other investigations have shown  
74 that when Mg-bearing glass, such as the British Magnox compositions, is altered in dilute  
75 aqueous solutions the released Mg also leads to formation of Mg-smectite phases (e.g.,  
76 Curti et al., 2006; Thien et al., 2012; Harrison, 2014). It is likely, therefore, that saponite  
77 could be a thermodynamically stable phase that precipitates when Mg-bearing solutions,  
78 both dilute and concentrated, contact silicate glass for a sufficient length of time.

79         When saponite forms, it may impact the near-field chemistry of a geological  
80 repository in various rock formations including salt formations by: (1) Controlling the  
81 chemical compositions, including hydrogen ion concentrations, of the contacting  
82 solutions, and (2) Forming a secondary mineral assemblage that will either enhance for  
83 certain periods (Lucksheiter and Nesovic, 1998; Curti et al., 2006; Fleury et al., 2013;

84 Aréna et al., 2016, 2017), or retard (Grambow and Strachan, 1984; Frugier et al., 2005) or  
85 both at different periods (Thien et al., 2012; Harrison, 2014), the dissolution rate of  
86 glasses, and impact the retention of hazardous (radioactive) constituents after release  
87 from the glass (e.g., Abdelouas et al., 1997).

88 In addition, because saponite has the swelling and sorption properties similar to  
89 those of montmorillonite, saponite has also been proposed as a candidate buffer material  
90 for HLW and spent nuclear fuel disposal in harsh environments (e.g., Yang et al., 2014).  
91 This is because tri-octahedral smectites such as saponite have higher thermal and  
92 chemical stabilities than di-octahedral smectites such as montmorillonite, and are less  
93 susceptible to alteration in harsh environments (e.g., Eberl et al., 1978; Güven, 1990).

94 Because the phyllosilicates that form on the glass surface are typically not well  
95 crystallized, and phase characterization efforts by X-ray diffraction are often technically  
96 challenging, some investigators have resorted to using solution modelling to infer the  
97 identity of candidate phases (c.f., Grambow and Müller, 1989). For this strategy to be  
98 viable, knowledge of the thermodynamic properties of eligible phases, such as saponite,  
99 is crucial. However, the thermodynamic properties of saponite, especially Mg-enriched  
100 saponite, are not well-defined, and few studies have attempted to obtain them via glass  
101 corrosion experiments (Aréna et al., 2017; Debure et al., 2016). For instance, in a recent  
102 study, Aréna et al. (2017) tried to calculate the solubility constant of saponite (they called  
103 it Mg-smectite) via geochemical modeling of their glass corrosion experiments.  
104 However, their experiments were not designed, nor were they ideal, for determining the  
105 solubility constants of saponite. Aluminum concentrations were very low in their  
106 experiments, hampering modelling efforts. Hence, several compensating hypotheses

107 were constructed to estimate aluminum concentrations, including: (1) that aluminium  
108 concentrations were equal to the quantification limit of the instrument (ICP-AES); (2)  
109 aluminum concentrations were equal to the quantification limit divided by 1000; and (3)  
110 aluminium was depleted stoichiometrically from saponite. These assumptions may not  
111 be warranted.

112 Without accurate knowledge of the thermodynamic properties of saponite, it is  
113 difficult to make reliable and accurate predictions for the evolution of chemical  
114 compositions of the solutions containing Mg interacting with glass. Accurate knowledge  
115 of its thermodynamic properties is thus the prerequisite for modeling glass corrosion in  
116 Mg-bearing solutions, both at high and low ionic strength.

117 The objective of this study is to determine experimentally the solubility constants  
118 of hydrous saponite at elevated temperatures under well constrained conditions. The  
119 author first synthesized saponite (from nitrate cancrinite) according to an established  
120 methodology (see Experimental Methods). Because hydrogen ion concentrations are a  
121 key parameter governing the dissolution of saponite, the author first measured pH and  
122 then applied correction factors obtained at elevated temperatures (Kirkes and Xiong,  
123 2018). With proper knowledge of the hydrogen ion concentrations and the  
124 concentrations of Al, Mg, Na and Si in solution, the author calculated the equilibrium  
125 quotients. Then, the appropriate activity coefficient model is applied to extrapolate  
126 equilibrium quotients at certain ionic strengths to infinite dilution. This model allows us  
127 to then assess the solubility of saponite in previously reported experiments. It is shown  
128 that an accurate log K value can be used to understand glass corrosion in Mg-bearing  
129 solutions under a variety of geochemical conditions.

130

## 131 **EXPERIMENTAL METHODS**

132 In this study, the chemicals used for synthesis of the starting material were ACS  
133 reagent grade chemicals. The synthesis followed the procedure of Shao and Pinnavai  
134 (2010) with some modifications. In the work of Shao and Pinnavai (2010), the sources  
135 for Al, Mg, Na and Si, were  $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ ,  $\text{Mg}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , and water glass solution  
136 (containing 27 wt.% Si and 14 wt.% NaOH), respectively. In this work, the source for Si  
137 is  $\text{Na}_2\text{SiO}_3 \cdot 9\text{H}_2\text{O}$ , and NaOH was used to control the  $\text{pH}_m$  conditions. Other reagents are  
138 the same as those in Shao and Pinnavai (2010). Deionized water (DI) with  $>18.3 \text{ M}\Omega \cdot \text{cm}$   
139 used in the experiments was purged with high purity Ar gas for a minimum of one hour  
140 to remove dissolved  $\text{CO}_2$ , following the procedure of Wood et al. (2002) and Xiong  
141 (2008).

142 A supersaturation experiment was conducted at  $80.0 \pm 0.5 \text{ }^\circ\text{C}$  as follows. First,  
143 the author synthesized a mixture of saponite and nitrate cancrinite at  $90 \text{ }^\circ\text{C}$  following the  
144 procedure of Shao and Pinnavai (2010). The author kept the synthesized solid mixture  
145 together with the mother solution in the same container in an oven at  $90 \text{ }^\circ\text{C}$  for 7 days.  
146 Then, the author transferred the container to another oven at  $80 \text{ }^\circ\text{C}$ . Because aluminum  
147 silicates such as zeolites exhibit prograde solubility (i.e., higher solubility at higher  
148 temperatures) (Xiong, 2013), it is considered that the experiment initially kept at  $90 \text{ }^\circ\text{C}$   
149 for some time, and then remained at  $80 \text{ }^\circ\text{C}$ , approaches the equilibrium from the direction  
150 of supersaturation.

151 Solution samples were periodically withdrawn from the experiments. Before each  
152 sampling, pH readings were taken for each experiment. In each sampling, about 3 mL of



153 solution was taken from each experiment, and the solution samples were filtered through  
154 a 0.2  $\mu\text{m}$  filter, and transferred into pre-weighed 10 mL Grade A volumetric flasks. After  
155 filtration, masses of each solution sample were determined with a balance that is precise  
156 to the fourth decimal place. Samples were then immediately acidified with 0.5 mL of the  
157 Optima® Grade concentrated  $\text{HNO}_3$  from Fisher Scientific, and diluted to 10 mL with DI  
158 water. Chemical analyses for sodium, magnesium, aluminum, and silica were performed  
159 using a PerkinElmer Optima 8300 Dual View (DV) ICP-AES.

160 The pH readings were measured with an Orion-Ross combination pH glass  
161 electrode, coupled with an Orion Research EA 940 pH meter that was calibrated with  
162 three pH buffers (pH 4, pH 7, and pH 13) at the experimental temperature of  $80 \pm 0.5^\circ\text{C}$ .  
163 The pH scale used in this work is the concentration scale (Mesmer and Holmes, 1992),  
164 denoted as  $\text{pH}_m$ , which is a negative logarithm of hydrogen ion concentration on a molal  
165 scale. The pH readings are converted to  $\text{pH}_m$ , according to the following equation (Xiong  
166 et al., 2010),

167

$$168 \quad \text{pH}_m = \text{pH}_{\text{ob}} + A_m = \text{pH}_{\text{ob}} + A_M - \log \Theta$$

169

170 where  $A_m$  and  $A_M$  are correction factors on a molal scale and a molar scale, respectively,  
171 and  $\Theta$  is a conversion factor from molality to molarity. In this study, the expression of  
172 correction factors as a function of ionic strength at  $80^\circ\text{C}$  determined for NaCl solutions  
173 from Kirkes and Xiong (2018) is used to calculate the correction factors for the ionic  
174 strengths of the experiment.

175 Solid phases were analyzed using a Bruker D8 Advance X-ray diffractometer  
176 with a Sol-X detector. XRD patterns were collected using  $\text{CuK}\alpha$  radiation at a scanning  
177 rate of  $0.667^\circ/\text{min}$  for a  $2\theta$  range of  $10\text{--}90^\circ$ .

178 Major elemental compositions ( $\text{Na}_2\text{O}$ ,  $\text{Al}_2\text{O}_3$ ,  $\text{MgO}$  and  $\text{SiO}_2$ ) of the saponite  
179 crystals were determined by electron microprobe analysis (EMPA) at Sandia National  
180 Laboratory, Albuquerque. Analyses were obtained using a JEOL JXA-8530F hyperprobe  
181 electron probe micro analyzer with a field emission electron gun. The beam conditions  
182 were  $<1\ \mu\text{m}$  spot size, 15 keV accelerating potential and a current of 20 nanoamps.  
183 Concentrations (wt.% oxide) were determined using Wavelength Dispersive  
184 Spectrometry (WDS) to count on separate X-ray peaks judiciously chosen for efficiency,  
185 performance and lack of interference. Background offsets were chosen at least 500 steps  
186 away from the peak centers. Concentrations were quantified by comparing counts from  
187 simple silicate standards whose chemical compositions are known. A table that lists the  
188 element, the lower limit of detection, or LLD (wt. %), the crystal diffractometer and the  
189 counting times is provided (Appendix A).

190 Concentrations of the major elements in saponite were determined by averaging  
191 27 points. Adsorbed water was determined by loss on ignition (LOI) by heating a sample  
192 to  $700\ ^\circ\text{C}$  for one hour using a Netzsch STA 409 thermal gravimetric analyzer (TGA).  
193 The chemical formula of the saponite was calculated on the basis of  $\text{O}_{20}(\text{OH})_4$  per  
194 formula unit.

195 SEM and EDS analyses were performed using a JEOL JSM-5900LV scanning  
196 electron microscope (SEM) imaging system coupled with a NORAN System 7 Spectral  
197 Analysis System for energy dispersive spectroscopy (EDS).

198

## 199 **RESULTS**

200 XRD pattern of the synthesized saponite is presented in Figure 1. As is shown,  
201 this pattern is in reasonable agreement with that for saponite 15Å (PDF 00-013-0086)  
202 (Figure 1). Notice that saponite 15Å is a pure end-member of magnesium saponite with a  
203 chemical formula of  $\text{Mg}_3(\text{Si}, \text{Al})_4\text{O}_{10}(\text{OH})_2 \cdot 4\text{H}_2\text{O}$ . The peak at  $2\theta \sim 60^\circ$ , characteristic of  
204 saponite, is present in the saponite synthesized in this work (Figure 1), which was also  
205 observed in saponite synthesized at 160 °C by other researchers (i.e., He et al., 2014).  
206 The d-spacings of the major peaks for the synthesized saponite compare well with those  
207 of saponite 15Å standard (see Appendix B). In the synthesized saponite, there are some  
208 concentrations of sodium, as indicated by EMPA (Table 1) and SEM-EDS analyses  
209 (Figure 2). As my synthesis method follows that of Shao and Pinnavaia (2010), in which  
210 it was known that there was nitrate cancrinite in addition to saponite, the two extra peaks  
211 at  $2\theta = 13.97^\circ$  and  $27.48^\circ$  in Figure 1 can be attributed to nitrate cancrinite (Hund, 1984;  
212 Liu et al., 2005).

213 Interestingly, the flower-like morphology of the synthetic saponite produced in  
214 this study (see Figure 2A, 2B, 2C), is very similar to that observed for saponite  
215 precipitated on the surface of vitrified intermediate level nuclear waste corroded in a  
216 calcium-rich, magnesium-bearing solution (see Figure 4b in Utton et al., 2013). The  
217 saponite in Utton et al. (2013) has a general formula of  
218  $\text{Ca}_{0.25}(\text{Mg}, \text{Fe})_3[(\text{Si}, \text{Al})_4\text{O}_{10}](\text{OH})_2 \cdot n(\text{H}_2\text{O})$ . The calcium in the saponite reported in Utton  
219 et al. (2013) comes from the high Ca solutions that reacted with glass. In the corrosion  
220 experiments of the nuclear waste glass in  $0.016 \text{ mol} \cdot \text{kg}^{-1} \text{ MgCl}_2$  at 50 °C performed by

221 Thien et al. (2010), the morphology of the corrosion product saponite (see Figure 1 in  
222 Thien et al., 2010) is also similar to that of the synthetic saponite in this study. In Thien  
223 et al. (2010), the stoichiometry of the saponite is  
224  $\text{Na}_{0.39}(\text{Mg}_{2.25}\text{Li}_{0.06}\text{Al}_{0.06}\text{Fe}_{0.06}\text{Mn}_{0.25})[(\text{Si}_{3.23}\text{Al}_{0.77})\text{O}_{20}](\text{OH})_4$ , where M is a cation as  $\text{Ni}^{2+}$  or  
225  $\text{Mn}^{2+}$ . This stoichiometry is similar to that of the saponite synthesized in this study (see  
226 below).

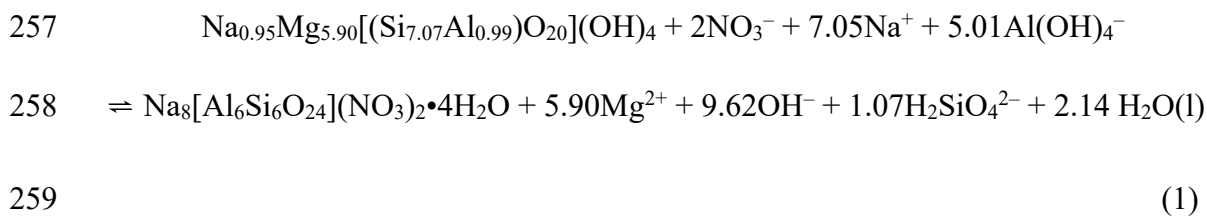
227 According to EPMA analysis, the stoichiometry of saponite synthesized in this  
228 work is  $\text{Na}_{0.95}(\text{Mg}_{5.90}\text{Al}_{0.06})[(\text{Si}_{7.07}\text{Al}_{0.93})\text{O}_{20}](\text{OH})_4$ . The structural formula is calculated  
229 by normalizing cation compositions to a theoretical structure containing  $\text{O}_{20}(\text{OH})_4$ . The  
230 total weight loss (loss on ignition, LOI) up to 700 °C is 19 wt%, similar to that for the  
231 natural saponite from California (Post, 1984), which has a total weight loss of 16.66 wt%  
232 (Table 1). The stoichiometry of the natural saponite from Ballarat, California, is  
233 calculated as  $(\text{Ca},\text{Na},\text{K})_{0.75}(\text{Mg}_{5.17}\text{Al}_{0.31}\text{Fe}^{\text{III}}_{0.13})[(\text{Si}_{7.55}\text{Al}_{0.45})\text{O}_{20}](\text{OH})_4$  (Table 1). The  
234 natural saponite from Milford, Utah, has a LOI of 17.30 wt% (Cahoon, 1954), and its  
235 stoichiometry is calculated as  $(\text{Ca},\text{Na},\text{K})_{0.42}(\text{Mg}_{5.72}\text{Al}_{0.19}\text{Fe}^{\text{III}}_{0.02})[(\text{Si}_{7.50}\text{Al}_{0.50})\text{O}_{20}](\text{OH})_4$   
236 (Table 1). In addition, the stoichiometry of the natural saponite from Allt Ribhein, Skye,  
237 is  $(\text{Ca},\text{Na},\text{K})_{1.02}(\text{Mg}_{5.84}, \text{Mn}_{0.01}, \text{Al}_{0.03}, \text{Fe}^{\text{III}}_{0.08})[(\text{Si}_{6.99}\text{Al}_{1.01})\text{O}_{20}](\text{OH})_4$  (MacKenzie,  
238 1957) (Table 1). Therefore, the stoichiometry of natural saponite varies to some degree.  
239 The stoichiometric coefficients for Mg are similar in saponite from these localities,  
240 suggesting they belong to Mg-saponite. Notice that the stoichiometry of the synthetic  
241 saponite is similar to that from Allt Ribhein, Skye, in terms of Si, Al, and Mg.

242 In this study, the solubility experiment at  $80 \pm 0.5$  °C was performed from the  
243 direction of supersaturation to approach equilibrium (see Experimental Methods section

244 for details). The experimental results for  $pH_m$ , sodium, total magnesium, total aluminum,  
245 total silica, nitrate and hydroxyl concentrations are presented in Table 2 and are displayed  
246 in Figure 3. It is clear from Figure 3 that steady state conditions were achieved for all  
247 solutes in terms of concentration with deviations generally  $\leq 25\%$  on a linear scale. For  
248 instance, the sodium concentrations remain between 1.38 and 1.44 mol•kg<sup>-1</sup>, a deviation  
249 of 4%. Note that Al and Si usually vary reciprocally for the dissolution of Al-silicates,  
250 and it is appropriate to assess their variations using the solubility product of both Al and  
251 Si (i.e.,  $m_{\Sigma Al} \times m_{\Sigma Si}$ ) (Xiong, 2016). As nitrate cancrinite and saponite are in equilibrium  
252 in our experiment, the equilibrium constant for the assemblage of nitrate cancrinite and  
253 saponite can be determined, based on the experimental results.

254 The equilibrium between saponite and nitrate cancrinite in alkaline solutions can  
255 be written as follows:

256



260 The equilibrium quotient for Reaction (1) is:

261

$$262 \quad Q_1 = \frac{(m_{\text{Mg}^{2+}})^{5.90} \times (m_{\text{H}_2\text{SiO}_4^{2-}})^{1.07} \times (m_{\text{OH}^-})^{9.62}}{(m_{\text{Na}^+})^{7.05} \times (m_{\text{NO}_3^-})^2 \times (m_{\text{Al}(\text{OH})_4^-})^{5.01}} \tag{2}$$

263

264 The equilibrium constant at infinite dilution is:

265

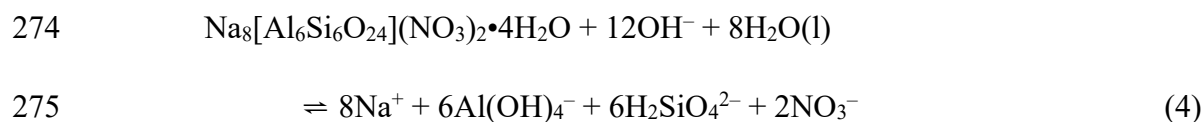
$$266 \quad K_1^0 = Q_1 \times \frac{(\gamma_{Mg^{2+}})^{5.90} \times (\gamma_{H_2SiO_4^{2-}})^{1.07} \times (\gamma_{OH^-})^{9.62} \times (a_{H_2O})^{2.14}}{(\gamma_{Na^+})^{7.05} \times (\gamma_{NO_3^-})^2 \times (\gamma_{Al(OH)_4^-})^{5.01}} \quad (3)$$

267

268 In the above equations,  $m_i$  denotes a concentration for the  $i$ -th species on a molal scale,  
 269 mol·g<sup>-1</sup>;  $\gamma_i$  an activity coefficient for the  $i$ -th species; and  $a_{H_2O}$  activity for water. The  
 270 equilibrium quotient for Reaction (1) at 80 °C is listed in Table 3.

271 Similarly, the dissolution reaction for nitrate cancrinite in alkaline solutions can  
 272 be expressed as:

273



276 The equilibrium quotient for Reaction (4) can be expressed as:

277

$$278 \quad Q_4 = \frac{(m_{Na^+})^8 \times (m_{NO_3^-})^2 \times (m_{Al(OH)_4^-})^6 \times (m_{H_2SiO_4^{2-}})^6}{(m_{OH^-})^{12}} \quad (5)$$

279

280 The corresponding equilibrium constant at infinite dilution is:

281

$$282 \quad K_4^0 = Q_4 \times \frac{(\gamma_{Na^+})^8 \times (\gamma_{NO_3^-})^2 \times (\gamma_{Al(OH)_4^-})^6 \times (\gamma_{H_2SiO_4^{2-}})^6}{(\gamma_{OH^-})^{12} \times (a_{H_2O})^8} \quad (6)$$

283

284 Bickmore et al. (2001) determined a value of  $\log_{10} K^0 = -36.2 \pm 0.6 (2\sigma)$  for

285 Reaction (4) at 89 °C. Lichtner and Felmy (2003) provided a value of  $\log_{10} K^0 = -39.03$

286 at 75 °C. The linear interpolation of these two values leads to a value of  $-37.99 \pm 0.70$   
287 ( $2\sigma$ ) for Reaction (4) at 80 °C (Table 3). This value is used to retrieve the solubility  
288 constant for saponite at 80 °C as detailed below.

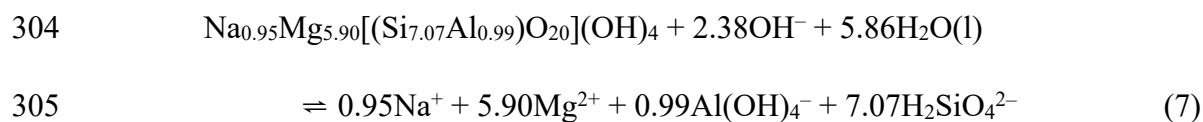
289 In our thermodynamic calculations for the activity coefficients for Equations (3)  
290 an (6), we use the computer code EQ3/6 Version 8.0a (Wolery et al., 2010; Xiong, 2011).  
291 In all calculations, the activity of all solid phases is assumed to be unity. The EQ3/6 code  
292 has been successfully used as a modeling platform in a number of previous studies at  
293 ambient temperature (e.g., Xu et al., 1999; Kong et al., 2013; Xiong, 2015, 2020) and at  
294 elevated temperatures up to 523.15 K (e.g., Xiong, 2013, 2014, 2016).

295 The database used for thermodynamic calculations is DATA0.YPF (Wolery and  
296 Jarek, 2003), which utilizes the Pitzer model for calculations of activity coefficients of  
297 aqueous species. The database was modified with the addition of the Pitzer parameters  
298 and equilibrium constants for Al and Si species from Xiong (2013 and 2014).

299 Based on the experimental data, we first calculated the equilibrium constant for  
300 Reaction (1) (Table 3). The equilibrium constant for Reaction (1) at infinite dilution and  
301 80 °C is  $-31.25 \pm 1.96$  ( $2\sigma$ ) in logarithmic units (Table 3).

302 The combination of Reactions (1) and (4) leads to,

303



306

307 The equilibrium quotient for Reaction (7) can be expressed as:

308

309 
$$Q_7 = \frac{(m_{Na^+})^{0.95} \times (m_{Mg^{2+}})^{5.90} \times (m_{Al(OH)_4^-})^{0.99} \times (m_{H_2SiO_4^{2-}})^{7.07}}{(m_{OH^-})^{2.38}} \quad (8)$$

310

311 The corresponding equilibrium constant at infinite dilution is:

312

313 
$$K_7^0 = Q_7 \times \frac{(\gamma_{Na^+})^{0.95} \times (\gamma_{Mg^{2+}})^{5.90} \times (\gamma_{Al(OH)_4^-})^{0.99} \times (\gamma_{H_2SiO_4^{2-}})^{7.07}}{(\gamma_{OH^-})^{2.38} \times (a_{H_2O})^{5.86}} \quad (9)$$

314

315 According to the equilibrium constants for Reactions (1) and (4), the equilibrium constant  
316 for dissolution of saponite at 80 °C in alkaline solutions (i.e., pH<sub>m</sub> ~12.58), represented  
317 by Reaction (7), is computed to be  $-69.24 \pm 2.08$  (2σ) in logarithmic units (Table 3). The  
318 quoted uncertainty includes the error propagations.

319

## 320 **DISCUSSIONS**

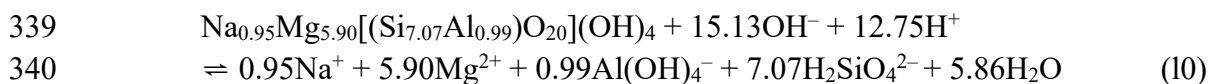
321 Debure et al. (2016) conducted three glass corrosion experiments with the  
322 International Simple Glass (GISG) at 90 °C. The first one involved pure water, the second  
323 experiment used  $8 \times 10^{-3} \text{ mol} \cdot \text{dm}^{-3}$  MgCl<sub>2</sub> as the Mg-source, and the third corrosion  
324 experiment was conducted in the presence of hydromagnesite. In their experiments with  
325 MgCl<sub>2</sub> and hydromagnesite, it was observed that Mg-phyllosilicates (saponite) were  
326 formed as white crusts on the glass powder surface, whereas no Mg-phyllosilicates were  
327 observed in the experiment with pure water. Because, for their corrosion experiment  
328 with hydromagnesite, they determined a complete set of chemical compositions for the  
329 solution, that experiment is an appropriate candidate to test the solubility constant of



330 saponite determined in this study. In the test, this author calculates the saturation index  
331 for saponite at 90 °C with the stoichiometry determined in this study for the experimental  
332 solution in Debure et al. (2016) at the same temperature.

333 In the calculations, the author first extrapolated the solubility constant of saponite  
334 determined at 80 °C to the experimental temperature of 90 °C in Debure et al. (2016). In  
335 the extrapolation, the author uses the one-term isocoulombic approach (Gu et al., 1994)  
336 for the following semi-isocoulombic reaction, utilizing ionization of water as a model  
337 substance to balance the charges for the reaction:

338



341

342 The transformation to the above semi-isocoulombic reaction is achieved by

343 combination of Reaction (7) with the following reaction,

344



346

347 In the one-term isocoulombic approach for extrapolation, the equilibrium  
348 constants for Reaction (10) at the temperatures of interest are first calculated. Then, the  
349 solubility constants for saponite for Reaction (7) at the respective temperatures are  
350 retrieved by adding the equilibrium constants for Reaction (11) to those for Reaction  
351 (10). The equilibrium constants for Reaction (11) at the temperatures of interest are  
352 taken from EQ3/6 database, DATA0.YPF. The extrapolated solubility constants for  
353 saponite at temperatures close to 80 °C obtained in this way are listed in Table 4.

354           The saturation index, for the experimental solution of Debure et al. (2016) (see  
355 their Table 3) at 90 °C is calculated (Table 5) with the solubility constant of saponite at  
356 90 °C. Note that the chemical composition of my synthesized saponite is similar to that  
357 reported by Debure et al. (2016) (“Phyllosilicate-Mg A”; see their Table 7). The  
358 calculated saturation index is 0.54, indicating that the solution is saturated or slightly  
359 supersaturated with saponite (Table 5). This is in good agreement with the experimental  
360 observations that Mg-phyllosilicate did form in their experiment. As mentioned above,  
361 the calculated saturation index is 0.54 (Table 5). Statistically speaking, the predictions  
362 could encompass the exact saturation when the uncertainty associated with the solubility  
363 constant of saponite at 90 °C ( $-67.6 \pm 2.5$ , Table 4) is taken into consideration.

364           Thien et al. (2012) conducted glass corrosion experiments in synthetic ground  
365 water (SGW) at 50 °C relevant to geological disposal of HLW. The SGW has the  
366 chemical compositions that represent the ground water in equilibrium with the Callovo-  
367 oxfordian argillite formation at Bure underground laboratory. The glasses they used were  
368 AVM 6 and AVM 10 glasses; both of them containing magnesium as one of the  
369 components. The AVM 6 glass was more enriched in SiO<sub>2</sub> than the AVM 10 glass. The  
370 Mg-phyllosilicate (saponite) was precipitated in their experiments involving the AVM 6  
371 glass.

372           Using the extrapolated solubility constant for saponite at 50 °C (Table 4), the  
373 author calculated the saturation index for the experimental compositions of Thien et al.  
374 (2012) involving the AVM 6 glass with the SGW at 50 °C. The calculated saturation  
375 index is 0.71 (Table 6), indicating that saponite has a thermodynamic driving force for its

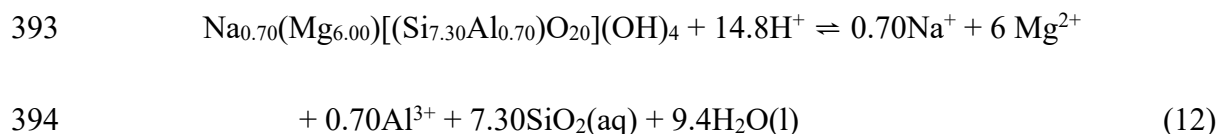
376 formation from the experimental solution. This is consistent with the experimental  
377 observations.

## 378 **IMPLICATIONS AND CONCLUDING REMARKS**

379 One important implication from this study is that when a nuclear waste glass is  
380 corroded in Mg-bearing solutions, Mg-saponite forms as a corrosion product, and the  
381 resulting solutions are close to be in equilibrium with Mg-saponite. Therefore, the  
382 solubility constants of Mg-saponite should be in the database as an essential part for  
383 prediction of the corrosion rates as a function of the solution chemistry in equilibrium  
384 with Mg-saponite.

385 Wilson *et al.* (2006) used the method proposed by Vieillard (2000) to estimate the  
386 Gibbs free energies of formation for smectites including Na-saponite with the  
387 stoichiometry of  $\text{Na}_{0.70}(\text{Mg}_{6.00})[(\text{Si}_{7.30}\text{Al}_{0.70})\text{O}_{20}](\text{OH})_4$ . Notice that Wilson *et al.* (2000)  
388 used  $\text{O}_{10}(\text{OH})_2$  per formula unit for Na-saponite. To be consistent with  $\text{O}_{20}(\text{OH})_4$  per  
389 formula unit used in this study, their values are converted to those referring to  $\text{O}_{10}(\text{OH})_2$   
390 per formula unit. They calculated the equilibrium constants for the dissolution of Na-  
391 saponite according to the following reaction,

392

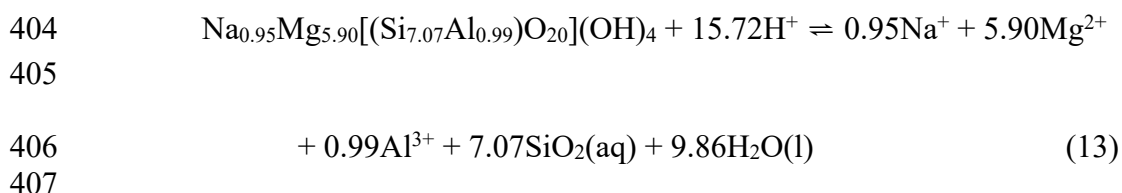


395

396 The  $\log_{10} K^0$  for Reaction (12) at 80 °C estimated by Wilson *et al.* (2006) is 50.95  
397 (uncertainty not provided, and the same is true with the following citations of the values  
398 from Wilson *et al.*, 2006). The stoichiometry of their Na-saponite is very close to that of

399 the saponite studied in this work, and therefore their estimated value can be compared  
400 with the value determined in this study. In order to do a direct comparison with the  
401 equilibrium constant at 80 °C determined in this study, Reaction (7) is transformed into  
402 the following form,

403

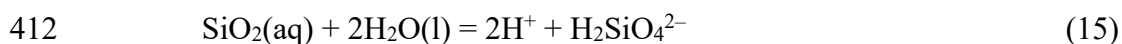


408 by combining Reaction (7) with the following reactions,

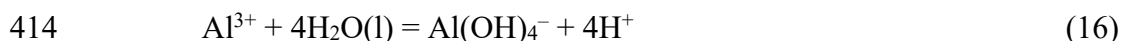
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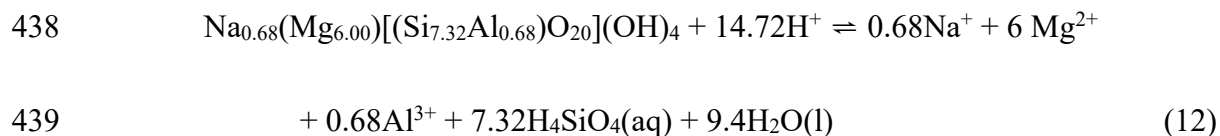
416 The equilibrium constants for Reactions (14) through (16) are from the EQ3/6 Data0.YPF  
417 database, Xiong (2013), and Xiong (2014), respectively. Accordingly, the  $\log_{10} K^0$  for  
418 Reaction (13) at 80 °C is  $70.30 \pm 2.08$ . The  $\log_{10} K^0$  estimated by Wilson et al. (2006)  
419 differs from the experimentally determined value by ~20 orders of magnitude.

420 The estimated  $\log_{10} K^0$  for Reaction (12) at 90 °C is 48.75 (Wilson et al. 2006), in  
421 comparison with the extrapolated  $\log_{10} K^0$  of  $70.8 \pm 2.5$ , based on the experimentally

422 determined value. When the estimated  $\log_{10} K^0$  is used to calculate the saturation index  
423  $(\log \frac{Q}{K})$  of saponite for the solution chemistry from Debure et al. (2016) at 90 °C, the  
424 saturation index is too high ( $\log \frac{Q}{K} > 12$ ) to be consistent with the experimental  
425 observations. Similarly, the estimated  $\log_{10} K^0$  for Reaction (12) at 50 °C is 58.35  
426 (Wilson et al. 2006), whereas the extrapolated  $\log_{10} K^0$  is  $70.4 \pm 2.5$ . When the  
427 estimated  $\log_{10} K^0$  is applied to the solution chemistry at 50 °C from Thien et al. (2012),  
428 the saturation index is too high ( $\log \frac{Q}{K} > 12$ ) to be consistent with the experimental  
429 observations. Consequently, in light of the experimental results presented in this work,  
430 the estimation method needs to be revised to reconcile with the experimentally  
431 determined values of this work and the experimental observations of Thien et al. (2012)  
432 and Debure et al. (2016).

433 In addition, there is a solid phase of saponite-Na in the ThermoChimie database  
434 (Giffaut et al., 2014; Blanc et al., 2015). The saponite-Na in the database has the  
435 following stoichiometry on the basis of  $O_{20}(OH)_4$  per formula unit:

436  $Na_{0.68}(Mg_{6.00})[(Si_{7.32}Al_{0.68})O_{20}](OH)_4$ . The solubility constant ( $\log_{10} K^0$ ) for dissolution  
437 of the saponite-Na at 25 °C according to the following reaction



440 is  $57.28 \pm 7.30$  based on the data set of 10a Version of September 26, 2018 (ANDRA,  
441 2021). Notice that the error estimates are calculated based on the error percentage

442 relative to the basis of  $O_{10}(OH)_2$  per formula unit in the original data set. The  
443 extrapolated value at 25 °C for Reaction (13) is  $72 \pm 5$ , based on the value listed in  
444 Table 4 in this study. When the quoted uncertainties and differences in stoichiometry are  
445 taken into consideration, the estimated value from the ThermoChimie can be considered  
446 to agree with the experimentally-based value at 25 °C. This is encouraging for the  
447 estimation method, and it can be recalibrated with the experimental data at 25 °C  
448 obtained in this study. In this way, the estimation method will be better to reconcile with  
449 the experimental data and experimental observations, especially at elevated temperatures,  
450 noted for the comparisons with the estimated values from Wilson *et al.* (2006), as the  
451 ThermoChimie database and Wilson *et al.* (2006) use the same or very similar estimation  
452 method.

453 In summary, the solubility constant of saponite with a stoichiometry of  
454  $Na_{0.95}(Mg_{5.90}Al_{0.06})[(Si_{7.07}Al_{0.93})O_{20}](OH)_4$  at 80 °C has been determined in this work.  
455 Then, the author extrapolated this value to other temperatures close to 80 °C (i.e., 50 °C,  
456 60 °C, 70 °C, 90 °C, and 100 °C) by employing the one-term isocoulombic approach. The  
457 author calculated the saturation indexes,  $\log \frac{Q}{K}$ , for the solution chemistry from the glass  
458 corrosion experiments in the presence of a Mg-source at 50 °C and 90 °C from different  
459 researchers. My calculated saturation indexes suggest that the solutions are  
460 saturated/slightly-supersaturated with saponite, which are in close agreement with the  
461 experimental observations at various temperatures. This suggests that the alteration  
462 products containing Mg formed when glasses are corroded in a solution in the presence of  
463 a Mg-source may control the chemical compositions, including hydrogen ion  
464 concentrations, of the solutions in contact with the glasses. As the compositions of

465 natural saponite vary to some degree, the results are best applied to the situations where  
466 the compositions of saponite are similar to those of synthetic saponite, such as the  
467 saponite from Allt Ribhein, Skye.

468

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683 Figure Captions

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686 Figure 1. XRD pattern of the solubility-controlling phases in the experiment performed  
687 in this work, compared with those of saponite 15A and NO<sub>3</sub>-cancrinite.

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690 Figure 2. SEM images and EDS analyses for the solid phases from the experiment  
691 performed in this study. A–C are SEM images with the respective EDS analyses: A.  
692 magnification at 6,500 times; B. magnification at 5,500 times; and C. magnification at  
693 3,700 times.

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696 Figure 3. A plot showing total molal concentrations of Al(III), Mg(II), Na(I), NO<sub>3</sub><sup>-</sup>, and  
697 Si(IV) as a function of experimental time in an experiment approaching equilibrium from  
698 the direction of supersaturation at 80 °C.

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Table 1. Chemical compositions of saponite synthesized in this work in comparison with those of natural saponite.

Oxide	Synthetic Saponite, This Work, wt%	Natural Saponite, Ballarat, California, wt% <sup>A</sup>	Natural Saponite, Milford, Utah, wt% <sup>B</sup>	Natural Saponite, Allt Ribhein, Fiskavaig Bay, Skye, wt% <sup>C</sup>
SiO <sub>2</sub>	46.80	51.26	50.01	43.62
TiO <sub>2</sub>	0.00	0.09	0.00	0.00
Al <sub>2</sub> O <sub>3</sub>	5.56	4.42	3.89	5.50
Fe <sub>2</sub> O <sub>3</sub>	0.00	1.14	0.21	0.66
FeO	0.00	---	0.00	---
MnO	0.00	0.03	0.00	0.06
MgO	26.22	23.54	25.61	24.32
CaO	0.00	1.25	1.31	2.85
Na <sub>2</sub> O	3.27	1.14	0.00	0.08
K <sub>2</sub> O	0.00	0.18	0.00	0.04
H <sub>2</sub> O (LOI)	19.26 <sup>D</sup>	16.66	17.30	22.90

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<sup>A</sup> Post (1984), (Ca,Na,K)<sub>0.75</sub>(Mg<sub>5.17</sub>Al<sub>0.31</sub>Fe<sup>III</sup><sub>0.13</sub>)[Si<sub>7.55</sub>Al<sub>0.45</sub>]O<sub>20</sub>(OH)<sub>4</sub>. The stoichiometry is calculated in this work on the basis of O<sub>20</sub>(OH)<sub>4</sub> per formula unit.

<sup>B</sup> Cahoon (1954), (Ca,Na,K)<sub>0.42</sub>(Mg<sub>5.72</sub>Al<sub>0.19</sub>Fe<sup>III</sup><sub>0.02</sub>)[Si<sub>7.50</sub>Al<sub>0.50</sub>]O<sub>20</sub>(OH)<sub>4</sub>. The stoichiometry is calculated in this work based on O<sub>20</sub>(OH)<sub>4</sub> per formula unit..

<sup>C</sup> Mackenzie (1957), (Na, K, Ca)<sub>1.02</sub>(Mg<sub>5.84</sub>, Mn<sub>0.01</sub>, Al<sub>0.03</sub>, Fe<sup>III</sup><sub>0.08</sub>)Si<sub>6.99</sub>Al<sub>1.01</sub>O<sub>20</sub>(OH)<sub>4</sub>. The stoichiometry was calculated by Mackenzie (1957). I obtained almost the same formula based on the compositions provided.

<sup>D</sup> Based on TGA analysis up to 700 °C.

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Table 2. Experimental data from the solubility experiment regarding the equilibrium between nitrate cancrinite and saponite produced in this study at  $80.0 \pm 0.5$  °C.

Experimental Number	Experimental time, days	<sup>A</sup> pH <sub>m</sub>	<sup>B</sup> m <sub>Na</sub>	<sup>B</sup> m <sub>ΣMg(II)</sub>	<sup>B</sup> m <sub>ΣAl(III)</sub>	<sup>B</sup> m <sub>ΣSi(IV)</sub>	<sup>C</sup> m <sub>NO<sub>3</sub><sup>-</sup></sub>	<sup>D</sup> m <sub>OH<sup>-</sup></sub>
SAP-80-1	64	12.58	1.38	1.24E-05	2.94E-04	1.66E-02	6.72E-01	0.674
	85	12.56	1.42	1.11E-05	2.78E-04	1.99E-02	7.01E-01	0.674
	92	12.61	1.44	1.50E-05	1.94E-04	3.51E-02	6.91E-01	0.674

729 <sup>A</sup> Measured pH readings at 64, 85, 92 days were 12.43, 12.40, and 12.45, respectively, at  
 730 the experimental temperature. The pH<sub>m</sub> values are calculated by applying the  
 731 correction factor at 80 °C from Kirkes and Xiong (2018) at the ionic strength of the  
 732 experiment.

733 <sup>B</sup> Analyzed with ICP-AES

734 <sup>C</sup> Calculated based on charge balance

735 <sup>D</sup> Based on the initial NaOH concentration.

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Table 3. Equilibrium constants of saponite at  $80 \pm 0.5$  °C determined in this work

Reactions	$\log_{10} Q^A$	$\log_{10} K^0$
$\text{Na}_{0.95}\text{Mg}_{5.90}[(\text{Si}_{7.07}\text{Al}_{0.99})\text{O}_{20}](\text{OH})_4 + 2\text{NO}_3^- + 7.05\text{Na}^+ + 5.01\text{Al}(\text{OH})_4^- \rightleftharpoons \text{Na}_8(\text{Al}_6\text{Si}_6\text{O}_{24})(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O} + 5.90\text{Mg}^{2+} + 9.62\text{OH}^- + 1.07\text{H}_2\text{SiO}_4^{2-} + 2.14\text{H}_2\text{O}(\text{l})$ (1)	$-23.52 \pm 1.96 (2\sigma)$	$-31.25 \pm 1.96 (2\sigma)$
$\text{Na}_8(\text{Al}_6\text{Si}_6\text{O}_{24})(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O} + 12\text{OH}^- + 8\text{H}_2\text{O}(\text{l}) \rightleftharpoons 8\text{Na}^+ + 6\text{Al}(\text{OH})_4^- + 6\text{H}_2\text{SiO}_4^{2-} + 2\text{NO}_3^-$ (4)		$-37.99 \pm 0.70 (2\sigma)^B$
$\text{Na}_{0.95}\text{Mg}_{5.90}[(\text{Si}_{7.07}\text{Al}_{0.99})\text{O}_{20}](\text{OH})_4 + 2.38\text{OH}^- + 5.86\text{H}_2\text{O}(\text{l}) \rightleftharpoons 0.95\text{Na}^+ + 5.90\text{Mg}^{2+} + 0.99\text{Al}(\text{OH})_4^- + 7.07\text{H}_2\text{SiO}_4^{2-}$ (7)		$-69.24 \pm 2.08 (2\sigma)^C$

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<sup>A</sup> At ionic strength of  $1.4 \text{ mol} \cdot \text{kg}^{-1}$

<sup>B</sup> Based on a linear interpolation of the values at  $89$  °C ( $-36.20$ ) from Bickmore et al. (2001) and at  $75$  °C ( $-39.03$ ) from Lichtner and Felmy (2003).

<sup>C</sup> A combination of the reaction in Row 2 with that in Row 3 leads to the reaction in Row 4 and its corresponding equilibrium constant.

Table 4. Extrapolated equilibrium constants of saponite with the stoichiometry determined in this work at other temperatures close to  $80$ °C

Reactions	T °C	$\log_{10} K^0$
$\text{Na}_{0.95}\text{Mg}_{5.90}[(\text{Si}_{7.07}\text{Al}_{0.99})\text{O}_{20}](\text{OH})_4 + 2.38\text{OH}^- + 5.86\text{H}_2\text{O}(\text{l}) \rightleftharpoons 0.95\text{Na}^+ + 5.90\text{Mg}^{2+} + 0.99\text{Al}(\text{OH})_4^- + 7.07\text{H}_2\text{SiO}_4^{2-}$	25	$-80 \pm 5^C$
	50	$-74.7 \pm 2.5^C$
	60	$-72.8 \pm 2.5^C$
	70	$-70.96 \pm 2.5^B$
	80	$-69.24 \pm 2.08 (2\sigma)^A$
	90	$-67.6 \pm 2.5^C$
	100	$-66.1 \pm 2.5^C$

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<sup>A</sup> Determined in this study.

<sup>B</sup> One-term isocoulombic extrapolation based on the experimental value at  $80$  °C.

<sup>C</sup> Linear extrapolation in the space of  $\log K$  vs.  $1/T$  where T is in absolute temperature in K, based on the values at  $70$  °C and  $80$  °C.



761 Table 5. Chemical compositions of the solution in which the international simple glass  
762 was corroded at 90 °C

Concentration	ΣSi	ΣB	ΣNa	ΣAl	ΣCa	ΣMg
mmolar <sup>A</sup>	1.49E+00	1.1561E+02	6.298E+01	6.00E-02	5.00E-02	5.00E-02
mmolal <sup>B</sup>	1.55E+00	1.20E+02	6.55E+01	6.24E-02	5.20E-02	5.20E-02
Saturation state with respect to saponite, Na <sub>0.95</sub> Mg <sub>5.90</sub> [(Si <sub>7.07</sub> Al <sub>0.99</sub> )O <sub>20</sub> ](OH) <sub>4</sub>						
log $\frac{Q}{K}$ <sup>C</sup>	0.5367					

763 <sup>A</sup> From Debure et al. (2016); concentration unit, 10<sup>-3</sup> mol•dm<sup>-3</sup>.

764 <sup>B</sup> This study, concentration unit, 10<sup>-3</sup> mol•kg<sup>-1</sup>. Converted from the results from Debure  
765 et al. (2016) by using a density of 0.15 mol•dm<sup>-3</sup> NaCl at 90 °C to approximate the  
766 density of the experimental solution in Debure et al. (2016). The density of 0.15  
767 mol•dm<sup>-3</sup> NaCl at 90 °C is from Söhnel and Novotný (1985).

768 <sup>C</sup> In log  $\frac{Q}{K}$ ,  $Q$  is ion activity product (IAP) with respect to saponite;  $K$  is the equilibrium  
769 constant defined by Reaction (7). In the calculation, pH was assumed to be constrained  
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Table 6. Chemical compositions of the solution in which the AVM 6 nuclear glass was corroded in synthetic groundwater (SGW) at 50 °C

Concentration	ΣSi	ΣB	ΣNa	ΣLi	ΣAl
mg/L <sup>A</sup>	19	786	2257	24	1.9
molar <sup>B</sup>	6.77E-04	7.27E-02	9.82E-02	3.46E-03	9.06E-05
molal <sup>C</sup>	6.86E-04	7.38E-02	9.96E-02	3.51E-03	9.19E-05
Concentration	ΣMg	ΣK	ΣCa	ΣCl	ΣSO <sub>4</sub>
mg/L <sup>A</sup>	16	45	30	1491	1397
molar <sup>B</sup>	6.58E-04	1.15E-03	7.49E-04	4.21E-02	1.45E-02
molal <sup>C</sup>	6.68E-04	1.17E-03	7.59E-04	4.27E-02	1.48E-02
Saturation state with respect to saponite, Na <sub>0.95</sub> Mg <sub>5.90</sub> [(Si <sub>7.07</sub> Al <sub>0.99</sub> )O <sub>20</sub> ](OH) <sub>4</sub>					
$\log \frac{Q}{K}$ <sup>D</sup>	0.7075				

779 <sup>A</sup> From Thien et al. (2012), their experimental compositions involving the AVM 6 glass  
780 with the SGW at 219 days and 50 °C; concentration unit, 10<sup>-3</sup> g•dm<sup>-3</sup>.

781 <sup>B</sup> This study, concentration unit, mol•dm<sup>-3</sup>; converted from the results of  
782 Thien et al. (2012). The calculated total ionic strength for the solution is 0.14 mol•  
783 dm<sup>-3</sup>.

784 <sup>C</sup> This study, concentration unit, mol•kg<sup>-1</sup>. Converted from the results on molar units by  
785 using a density of 0.14 mol•dm<sup>-3</sup> NaCl at 50 °C to approximate the density of the  
786 SGW in which AVM 6 nuclear glass was corroded at 50 °C. The density of 0.14  
787 mol•dm<sup>-3</sup> NaCl at 50 °C is from Söhnle and Novotný (1985).  
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789 <sup>D</sup> In  $\log \frac{Q}{K}$ ,  $Q$  is ion activity product (IAP) with respect to saponite;  $K$  is the equilibrium  
790 constant defined by Reaction (7).  
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793 Appendix A. The elements, their lowest limits of detection, or LLD (wt.%), the crystal  
794 diffractometer used and counting times for EPMA analyses  
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Element	1-σ LLD (wt.%)	Crystal	Counting time (s)
Si	0.040	TAP <sup>A</sup>	20 sec Peak, 5 sec Background
Al	0.027	TAP	20 sec Peak, 5 sec Background
Mg	0.055	TAP	20 sec Peak, 5 sec Background
Na	0.050	TAP	20 sec Peak, 5 sec Background

796 <sup>A</sup> TAP, Thallium Acid Phthalate.  
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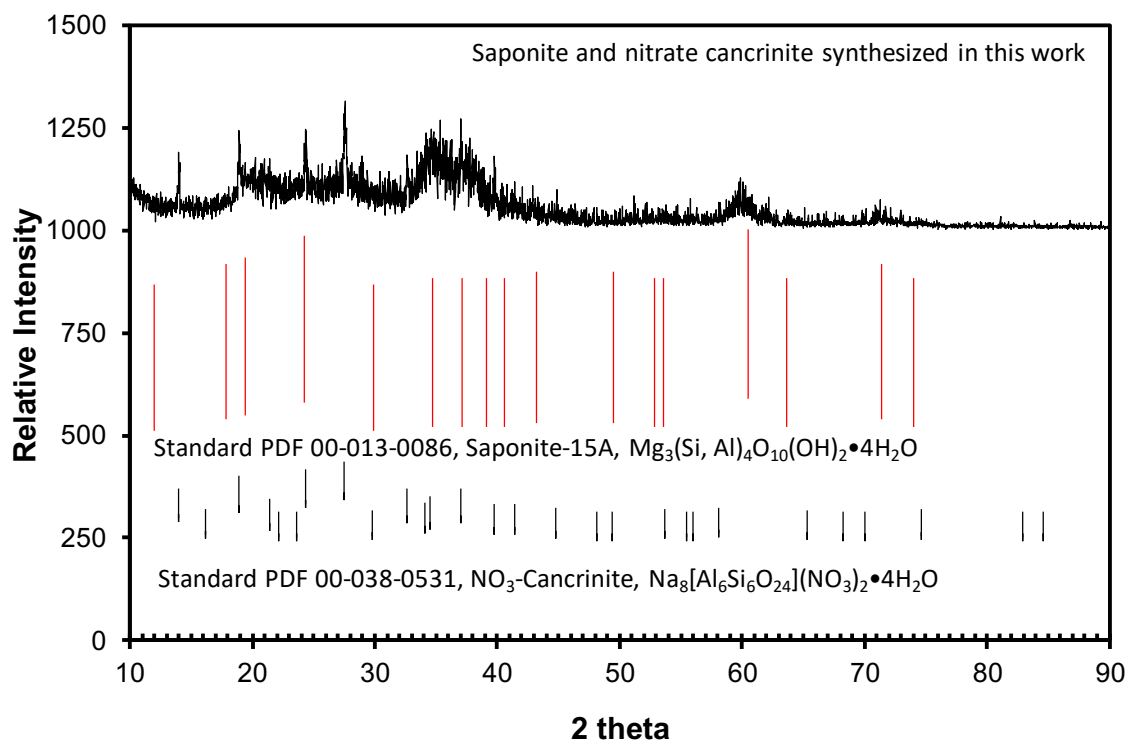
798 Appendix B. Comparison of major XRD peaks of saponite synthesized in this study with  
 799 those of the saponite 15 Å standard (PDF-00-013-0086)\*

Mg-saponite Standard, PDF-00-020-0964			Saponite, Synthesized in this study		
hkl	d-spacing, Å	Intensity	hkl	d-spacing, Å	Intensity**
(100)	4.57	50	(100)	4.572	166
(004)	3.67	60	(004)	3.666	214
(111)	2.58	20	(111)	2.577	242
(006)	2.42	20	(006)	2.421	217
(007)	2.09	30	(007)	2.089	82
(300)	1.53	90	(300)	1.534	111
(221)	1.32	40	(221)	1.322	76

800 \*The major peaks with intensity  $\geq 20$  in the standard are compared with those in  
 801 the synthetic saponite. The significant numbers presented for d-spacing of the  
 802 synthesized saponite are one more than those presented in the PDF database for  
 803 comparison. It is obvious that the synthesized saponite has the identical d-  
 804 spacings when its significant numbers are rounded as the same significant  
 805 numbers as the PDF database does.

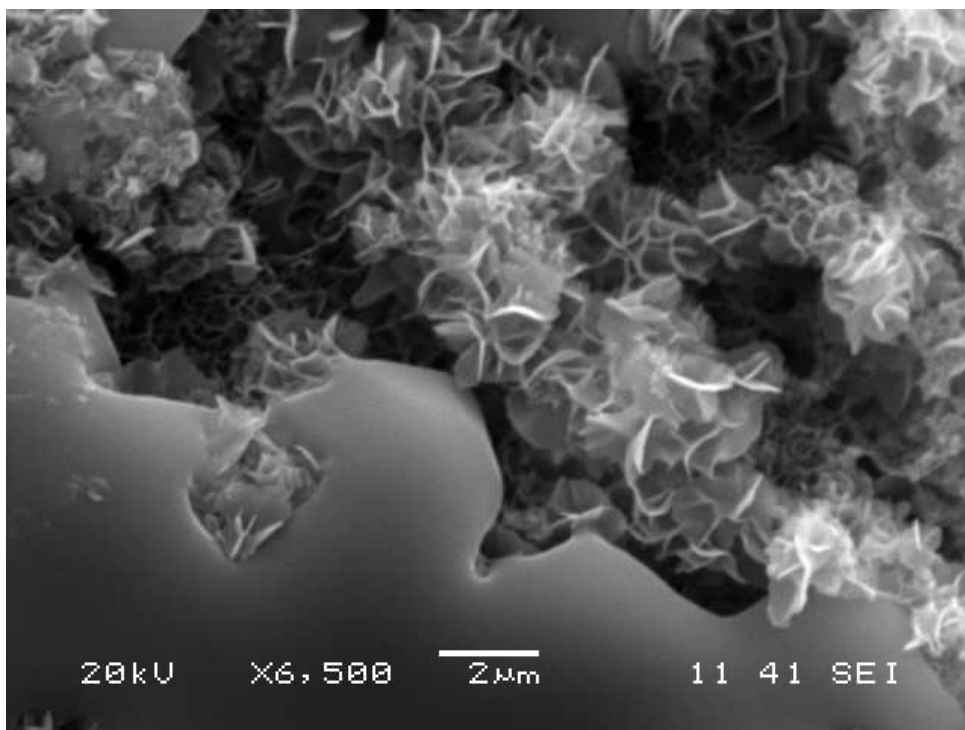
806 \*\* Experimental relative intensity

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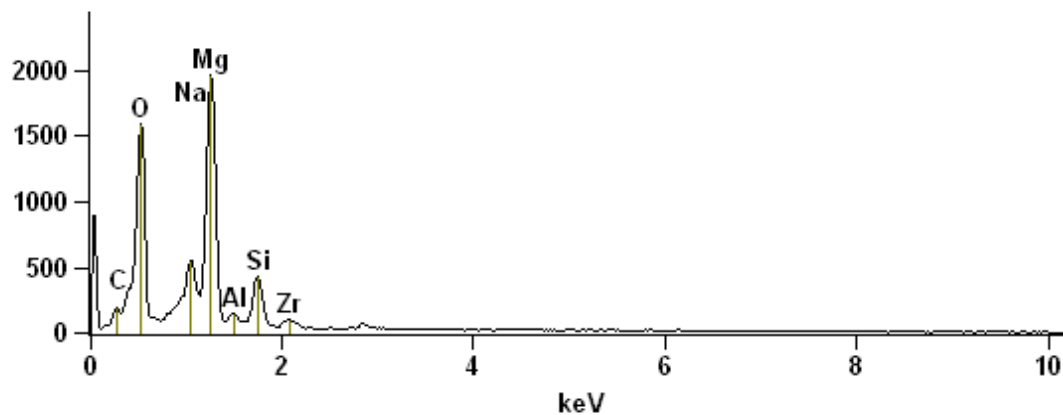
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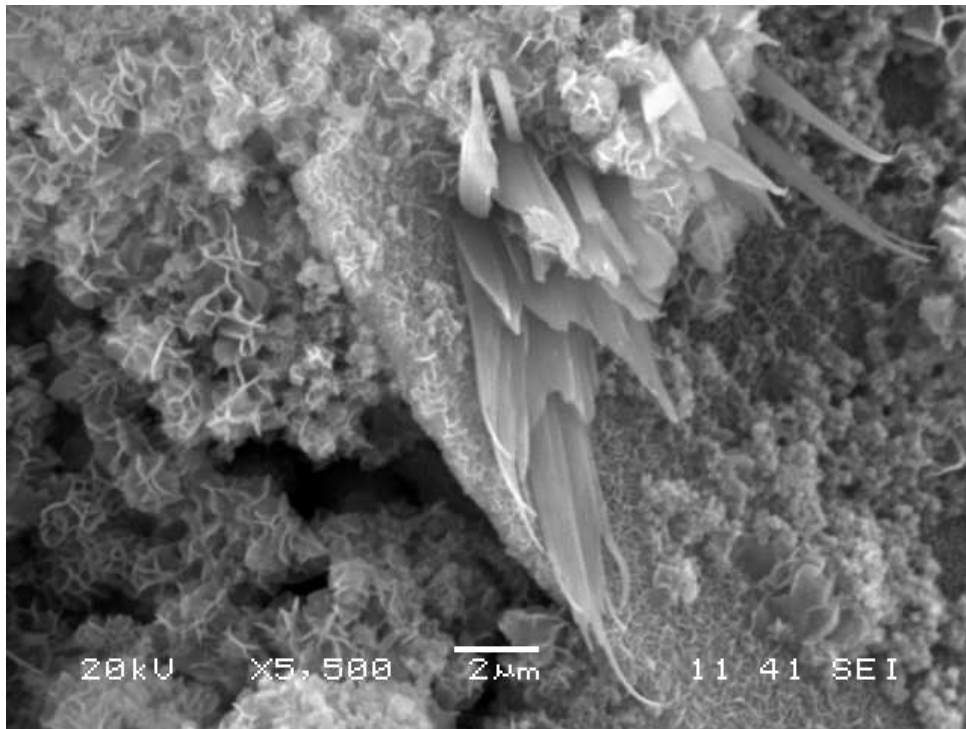
Full scale counts: 1956

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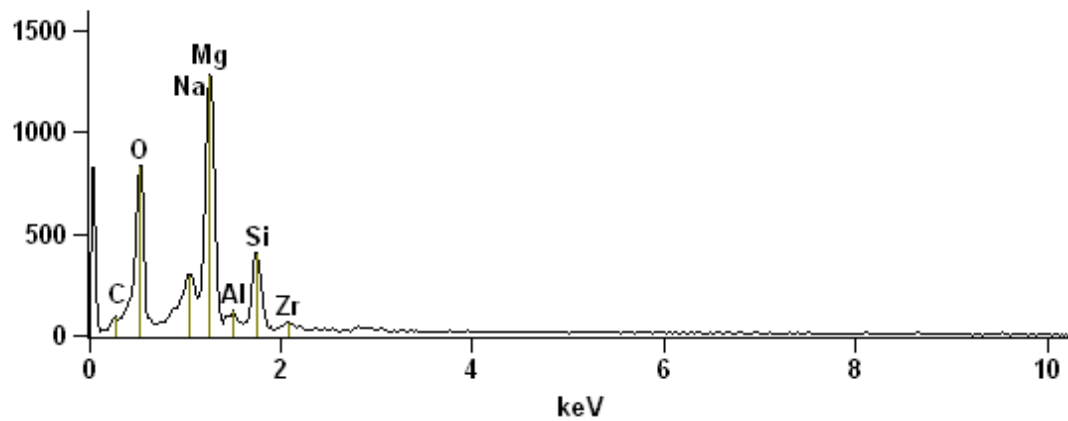
Figure 2A.



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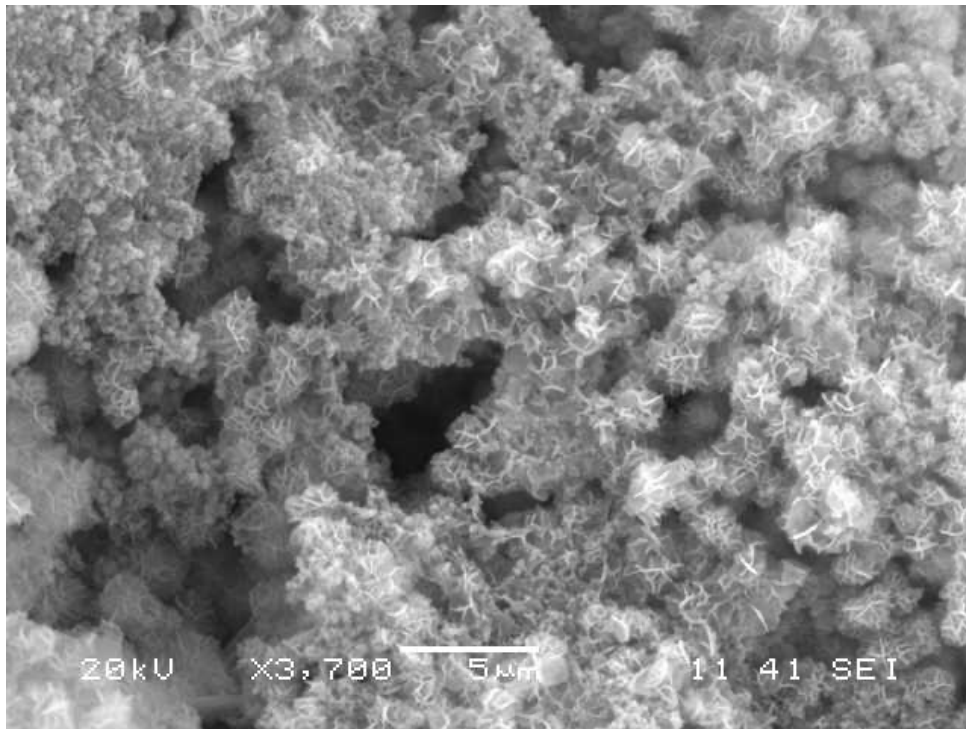
Full scale counts: 1279

Saponite 1(6)\_pt2



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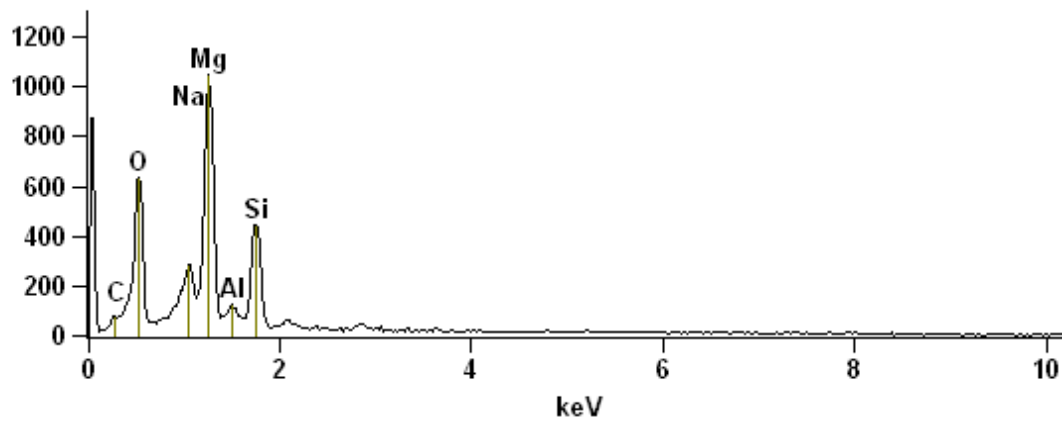
Figure 2B.



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Full scale counts: 1043

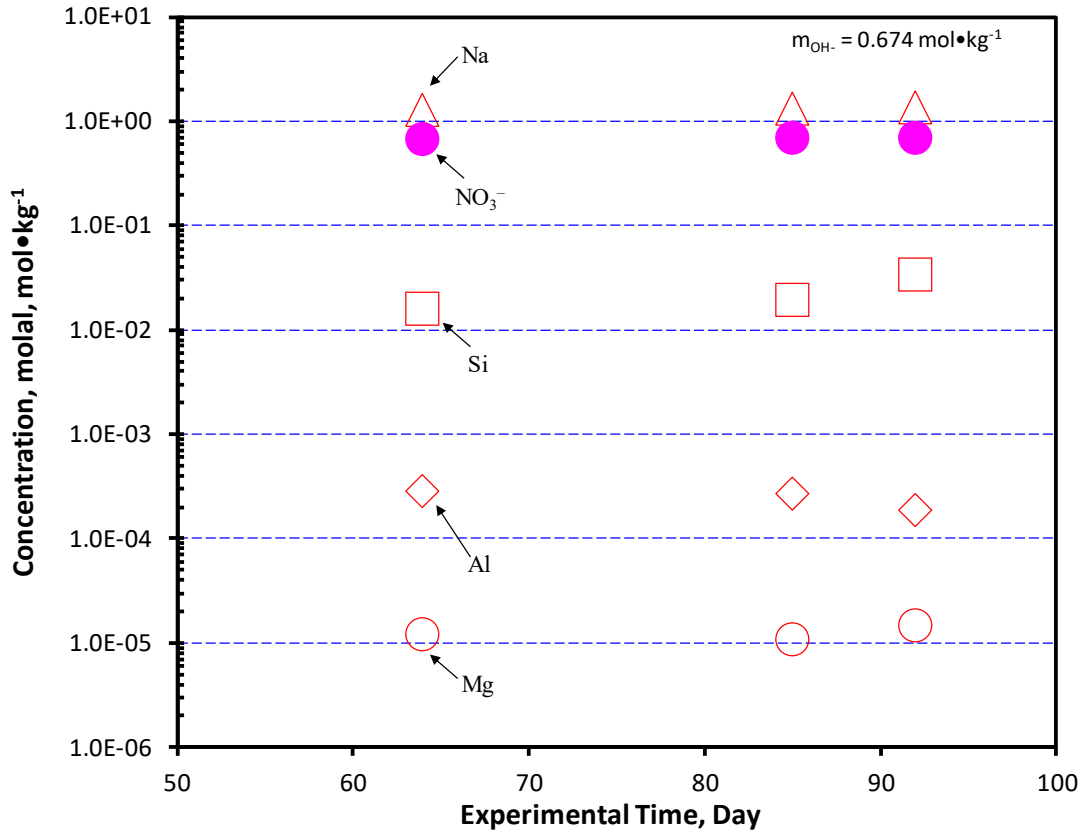
Saponite 1(5)\_pt2



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Figure 2C.

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Figure 3.