

1 **Revision 2**

2

3 **Title**

4 **Experimental constraints on bubble formation and growth during magma ascent: A**

5 **Review**

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15

16 **Abstract**

17 The number of studies investigating the vesiculation of natural samples and their implications to  
18 volcanic degassing and eruption mechanisms has been growing rapidly within the last decades.

19 In order to interpret the natural rock textures, the geoscience community has produced a range of  
20 experimental and theoretical datasets on bubble nucleation, growth and coalescence in magmatic  
21 systems. A robust experimental database is required to calibrate (theoretical and empirical)  
22 modeling approaches, which allow the calculation of magma ascent rates from erupted volcanic  
23 ejecta mainly by the determination of the bubble number density (BND). Although, the available

24 dataset is still limited, it already shows that variations in melt (and volatile/fluid) composition  
25 can have a significant effect. In this manuscript we (re-)evaluate the existing experimental  
26 dataset, while focusing mainly on the review and discussion of continuous decompression  
27 experiments.

28 One aim of this review article is to encourage scientists to fill the gaps in the existing  
29 experimental datasets and help to acknowledge, use and further develop the most promising  
30 experimental techniques. Therefore, we highlight different methods and discuss their advantages  
31 and possible limitations. We also discuss possible ways of how to better account for the  
32 influence of melt composition in models, which link BND to decompression rate.

33

#### 34 **Keywords**

35 bubble nucleation and growth, decompression experiment, magma ascent rates

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### 1. Introduction and Motivation

38 Large amounts of H<sub>2</sub>O, CO<sub>2</sub>, SO<sub>2</sub> and Cl are released by volcanic systems. However, the  
39 estimated annual volcanic emission of the “greenhouse gas” CO<sub>2</sub> to the atmosphere is ~0.1 to  
40 0.44 Gt and, thus, about a factor of 80 to 270 lower than the anthropogenic CO<sub>2</sub> in 2010  
41 (Friedlingstein et al, 2010). On the other hand, the global anthropogenic SO<sub>2</sub> emission ranges  
42 around 100 to 110 Mt within the last decade (Klimont et al., 2013), while a single eruption of a  
43 major volcano, such as the Mt. St. Helens eruption in 1480, the Tambora eruption in 1815 or the  
44 eruption of Krakatau in 1885, can increase the annual SO<sub>2</sub> emission by up to 70% (see  
45 Shinohara, 2008; and references therein). Although the man-made greenhouse gas emission is  
46 without a doubt exceeding the volcanic contribution, large eruptions such as the one of Mt.

47 Pinatubo (Philippines) in 1991 can release tremendous amounts of CO<sub>2</sub> (here: ~42 Mt CO<sub>2</sub>) and  
48 SO<sub>2</sub> (here: ~17-20 Mt SO<sub>2</sub>) over a short period (e.g., Bluth et al., 1992; Gerlach et al., 1996) and,  
49 thus, impact the global climate for months and even up to several years (e.g., Self et al., 1996).  
50 Notably, SO<sub>2</sub> is a much more efficient climate affecting gas than CO<sub>2</sub>. It is largely converted to  
51 sulfuric acid after being released to the atmosphere, where it condenses rapidly to form fine  
52 grained sulfate aerosols. The sulfate aerosol increases the reflection of radiation from the sun  
53 into space, causing the cooling of Earth's atmosphere and/or troposphere (McGee et al., 1997).  
54 Other possible major environmental impacts of S emission include: ozone depletion (via reaction  
55 with Cl; Self et al., 1996) and acid rain leading, amongst others, to significant crop failure  
56 (Sigurdsson, 1982). Although there is nothing (geo-)scientists can do about this natural  
57 contribution to climate change, the (physico-chemical) way on how the volatiles separate from a  
58 magma or lava is crucial for our understanding of eruption mechanisms and, thus, is helpful in  
59 forecasting volcanic eruptions and in possibly predicting the future impact of volcanic activities  
60 on the global climate.

61 Magma degassing, for instance during magma ascent (i.e., decompression-induced) or magma  
62 cooling (e.g., crystallization-induced second boiling), leads to the formation of bubbles, which  
63 can grow and/or coalesce over time and even separate the gas phase completely from the residual  
64 melt or magma (e.g., Sparks et al., 1994). The vesiculation of a magma, and here especially the  
65 size and number of bubbles, changes magma viscosity and, thus, significantly affects the eruptive  
66 style, i.e., "harmless" effusive vs. potentially "hazardous" explosive. The vesiculation of (natural  
67 and experimental) samples is typically described by the bubble number density (BND) and is a  
68 characteristic feature of some volcanic products (e.g., pumice, tephra) that can help to elucidate

69 the “ascent-history” of an erupted magma (e.g., Sparks et al., 1994; Toramaru, 1995; 2006;  
70 Hamada et al., 2010).

71 Once bubble nucleation is triggered and a certain vesiculation in a magma is reached, the bubbles  
72 may start to connect and form a bubble network along which large amounts of fluid can be  
73 transported upwards (Edmonds et al., 2010). This process may be limited to regimes with  
74 significant shear strain within the magma, e.g., along the conduit or in magma chambers with  
75 strong convections (e.g., Namiki and Manga, 2008; Namiki, 2012). It is worth noting that in  
76 systems with radii of  $>5$  mm for the largest bubbles, interaction between bubbles can induce  
77 significant bubble deformation (Manga and Stone, 1994), which may favor the formation of  
78 interconnected bubble networks. Even though an effective transport of fluids via bubble  
79 networks within a magma chamber may be questioned, the diffusive coarsening and bubble  
80 ascent from an underplating mafic magma to an overlaying felsic magma is probably an  
81 important process to transport volatiles and precious metals (e.g., Cu) from the mafic to the  
82 overlaying felsic magma and into fractures and intrusions where they can form porphyry-(Cu)-  
83 deposits (e.g., Hattori and Keith, 2001; Halter et al., 2005; Audétat and Simon, 2012). Although  
84 the majority of the fluids released by a magmatic system during an eruption may be transported  
85 to the surface along the conduit, these fluids may also play an important role in the formation of  
86 porphyry-(Cu)-deposits during periods of low volcanic activity (i.e., when bubbles have time to  
87 ascend). Thus, understanding bubble nucleation, growth and ascent in a magma at depth will also  
88 help elucidating timescales for the formation of porphyry deposits (and similar deposits).

89 In the last decades, several research groups worked on the experimental investigation of bubble  
90 nucleation processes in (silicate) melts. While the experimental and analytical techniques are  
91 continuously improving (see Section 2 and 3), we are getting more aware of the limitations of

92 certain techniques and a critical re-evaluation of the dataset is required. For instance, recently  
93 published experimental studies have revealed that the decompression style (continuous vs.  
94 stepwise) affects bubble formation to a significant extent (see Section 2 and Nowak et al., 2011;  
95 Marxer et al., 2015). This review focusses on decompression-induced bubble nucleation and  
96 aims at providing an overview of the existing experimental and analytical techniques as well as  
97 at the discussion and (re-)interpretation of previous results. Based on the compiled experimental  
98 literature data and three additional experiments performed for this study, we show that changes  
99 in major element composition and volatile contents can affect bubble nucleation considerably.  
100 However, the available dataset is still very limited and we highlight the existing gaps that should  
101 be filled in the near future, using the techniques described in this manuscript.

102

### 103 **1.1 Theoretical background of bubble formation**

104 When a volatile-supersaturated melt is cooled down or is depressurized, small clusters of gas  
105 molecules form and grow through volatile diffusion in the melt (e.g., Proussevitch et al., 1993;  
106 Proussevitch and Sahagian, 1996; 1998). Free energy and interfacial energy are linked to the  
107 formation of a separate gas phase and the creation of the bubble surface, respectively. The ratio  
108 between the two energies determines whether the critical (or minimum) bubble radius  $r_c$  ( $r_c = 2 \cdot$   
109  $\sigma / \Delta P_N$ ) can be overcome, leading to either homogeneous or heterogeneous bubble nucleation;  
110 see, e.g., reviews by Sparks (1978) and by Sparks et al. (1994). In heterogeneous bubble  
111 nucleation, wetted crystal surfaces, e.g., of Fe-Ti-oxides (Hurwitz and Navon, 1994), can act as  
112 bubble nucleation sites, lowering the required supersaturation pressure ( $\Delta P_N$ ; difference between  
113 gas pressure in the melt and ambient pressure) and, thus, decreasing the critical bubble radius  $r_c$   
114 (see Section 4.2). The melt-surface tension ( $\sigma$ ) is a function of the hydrous melt composition and

115 increases with higher silica content (Mangan and Sisson, 2005), negatively influencing the  
116 nucleation rate ( $J$ ). The strong dependence of the surface tension on melt composition was  
117 recently confirmed by experiments performed by Masotta et al. (2014) in an externally heated  
118 diamond anvil cell, using basaltic, andesitic and rhyodacitic melts. In contrast, the study of  
119 Gardner et al. (2013) on single-step decompression experiments supports the early work of  
120 Walker and Mullins (1981), indicating a rather minor effect of the melt composition on the  
121 surface tension of silicate melts and, thus, highlighting that further investigations are required.

122 However, following Hirth et al. (1970), the nucleation rate can be calculated using:

$$123 \quad J = J_0 e^{\left[-\frac{\Delta G}{kT}\right]} \quad (1),$$

124 where  $J_0$  is related to the statistical distribution of gas molecules in the melt,  $\Delta G$  is the free  
125 energy of formation of a critical nucleus,  $k$  is the Boltzmann constant and  $T$  is the temperature.

126 The nucleation pressure ( $P_N$ ) characterizes the onset of nucleation in a melt at a specific  
127 supersaturation pressure  $\Delta P_N$ . Typically, the supersaturation pressure is lower in the event of  
128 heterogeneous bubble nucleation than in the case of homogenous vesicle nucleation, owing to  
129 reduced energy barriers (e.g., Hurwitz and Navon, 1994; Gardner and Denis, 2004; Iacono  
130 Marziano et al., 2007; Larsen, 2008).

131 The growth of existing gas bubbles requires lower energies and can occur either by i) volatile  
132 diffusion from the melt into adjacent preexisting bubbles or through ii) mechanical expansion  
133 due to decreasing ambient pressure (e.g., Proussevitch et al., 1993; Sparks et al., 1994; Huber et  
134 al., 2014). Bubble growth is kinetically preferred over bubble nucleation at lower degrees of  
135 supersaturation, when the necessary nucleation pressure has not been reached yet. The growth  
136 rate ( $G_R$ ) is given by the increase of the bubble radius over a unit of time.

137 In natural magmatic systems crystals are certainly already present at magma storage conditions  
138 and, thus, heterogeneous nucleation is often expected (e.g., Mangan et al., 2004a). However,  
139 homogenous nucleation can also occur in low-crystalline magmas where high supersaturation of  
140 the interstitial bulk melt is reached before the volatiles can diffuse over the entire distance to  
141 bubbles that grow on sparsely distributed crystals. Moreover, only some specific crystals  
142 (probably oxides) may lead to heterogeneous bubble nucleation (see Section 4.2 and 4.4 for  
143 details and Hurwitz and Navon, 1994). Hence, magma composition and the prevailing pressure  
144 (P) – temperature (T) - oxygen fugacity ( $fO_2$ ) conditions at depth significantly influence whether  
145 bubbles nucleate homogeneously or heterogeneously.

146 The rock vesicularity, the bubble size distribution (BSD) and the bubble number density (BND)  
147 have become the most important parameters in understanding and tracing volatile exsolution  
148 processes and their related magma ascent velocities. BSD refers to the number of bubbles per  
149 unit volume within a series of defined size intervals (typically shown in a histogram plot of  
150 population density vs. size; Marsh, 1988), whereas BND stands for the total number of bubbles  
151 per unit volume and can be described as (e.g., Toramaru, 1995; Gardner et al., 1999):

$$152 \quad BND = \frac{\phi_m}{\sum \left( \frac{n_i}{N_T} V_i \right)} \quad (2),$$

153 where  $\phi_m$  is the vesicle volume fraction,  $N_T$  is the total number of bubbles,  $n_i$  is the bubble  
154 number and  $V_i$  is the bubble volume at a diameter  $i$ .

155 BNDs have been found to be strongly dependent on the decompression rate ( $r = \Delta P/\Delta t$ ),  
156 particularly at fast ascent rates (e.g., Toramaru, 1995; 2006), showing a positive correlation  
157 between BND and ascent velocities. Higher BND values are an indicator for a large number of  
158 bubbles and, thus, are a record of dominating bubble nucleation over bubble growth (e.g.,  
159 Mourtada-Bonnefoi and Laporte, 2004; Nowak et al., 2011). Furthermore, the volatile exsolution

160 and nucleation of gas bubbles is strongly dependent on the diffusivity of the volatile species in  
161 the melt. Thus, a possible delay in bubble nucleation can occur between a fast and a slow  
162 diffusing volatile component, affecting BND; see, e.g., difference in diffusion rates between H<sub>2</sub>O  
163 and CO<sub>2</sub> in silicate melts studied by Baker et al. (2005). On the other hand, a sudden change to  
164 faster decompression rate can also lead to a second nucleation event in magmas with preexisting  
165 bubbles as experimentally investigated and modeled by Toramaru (2014) and others (e.g.,  
166 Masotta et al., 2014). Here, secondary nucleation events result in complex, multi-peak BSD  
167 patterns (Toramaru, 2014) as observed in many studies on natural samples (Sparks and Brazier,  
168 1982; Klug and Cashman, 1994; Klug et al., 2002; Formenti and Druitt, 2003; Polacci et al.,  
169 2003; 2008; Lautze and Houghton, 2007; Giachetti et al., 2010; Shea et al., 2010; Parcheta et al.,  
170 2013).

171 Additionally, the “bubble signature” of a rock can also be altered or overprinted by coalescence  
172 during an annealing period producing complex size distribution that might lead to the  
173 misinterpretation of multiple nucleation events (e.g., Masotta et al., 2014), or simply by volatile  
174 loss and separation upon degassing. Moreover, during and after degassing of a melt (within a  
175 magma), smaller bubbles are often removed by diffusive coarsening (Ostwald ripening) of the  
176 larger bubbles (Lautze et al., 2011). This process favors growth of larger bubbles, and once they  
177 reached a size of  $\geq 1$  mm they can ascent multiple kilometers within the magma reservoir.  
178 However, this bubble ascent takes hundreds to thousands of years as shown by Lautze et al.  
179 (2011) based on experimental results and, thus, cannot sufficiently explain the short delay  
180 observed at volcanic systems between seismic activity and volcanic gas release as well as the  
181 very fast release of gases prior or during eruptions (e.g., Hautmann et al., 2014). Here, the  
182 formation of tensile hydraulic fractures is probably the most plausible mechanism, which allows

183 rapid separation of a fluid from a magma and the transport of this fluid phase to the surface  
184 (Scandone et al., 2007; Hautmann et al., 2014).

185

186

## 2. Experimental techniques

### 2.1 Experimental devices

187  
188 Most commonly, experimental studies on decompression-induced bubble formation focus on  
189 volcanic conduit regimes at relatively low pressures ( $\leq 500$  MPa), representing relatively shallow  
190 depths ( $\leq 20$  km). Such experiments are typically conducted in internally heated pressure vessels  
191 (IHPVs) or in cold-seal (externally heated) pressure vessels (CSPVs). Detailed description of  
192 their setup and mode of operation can be found in diverse publications (for IHPV: e.g.,  
193 Holloway, 1971 and the review of Lofgren, 1987; for CSPV: e.g., Tuttle, 1949 and the review of  
194 Ulmer et al., 1987). The maximum pressure usually reaches up to 300 to 500 MPa, typically  
195 using argon (Ar) gas as the pressure medium. In some cases, CSPVs can have hydrothermal  
196 setups, using water for pressurization (H<sub>2</sub>O-CSPV). TZM pressure vessels are a special type of  
197 cold-seal apparatuses that use a Mo-Ti-Zr-alloy for higher experimental run temperature ( $\sim 1200$   
198 °C at 200 MPa), instead of the Waspaloy alloy and Rene 41 alloy in a standard CSPV (max. 850  
199 °C at 300 MPa); see, e.g., Williams (1966) and Luth and Tuttle (1963). IHPV furnaces run  
200 conveniently at temperatures up to 1250 °C and pressures up to 500 MPa, while special high-  
201 temperature furnaces can reach 1450 °C and a pressure up to 900 MPa can be achieved in some  
202 IHPVs. The oxygen fugacity of experimental systems can be adjusted, for example, with i) the  
203 double-capsule technique by adding an outer capsule filled with a solid oxygen buffer (in H<sub>2</sub>O-  
204 and Ar-IHPV or Ar-CSPV), or ii) via Ar-H<sub>2</sub> gas mixtures using a Shaw-membrane to monitor the  
205 H<sub>2</sub>-partial pressure in IHPVs (e.g., Berndt et al., 2002), or iii) by using different alloys for the

206 vessel (in H<sub>2</sub>O-CSPV). Sensor capsules are often used to determine the oxygen fugacity for a  
207 specific vessel/pressure-medium setup, especially if H<sub>2</sub> sensors are not available (e.g., Taylor et  
208 al., 1992). Quench rates are dependent on the applied technique (and the sample size). Simply  
209 switching off the power to the furnace in IHPVs or removing the hot autoclave from the external  
210 CSPV-furnace and cooling it off with compressed air results in quench rates of about 150-200  
211 °C/min (e.g., Behrens and Zhang, 2009). Whereas the rapid-quench sample holders of IHPVs  
212 enable the capsule(s) to drop immediately into the colder part of the assembly (e.g., Holloway et  
213 al., 1992; Berndt et al., 2002), cooling the sample with  $\geq 150$  °C/sec. Similar quench rates can be  
214 achieved in vertical rapid-heat, rapid-quench (TZM) CSPV, which use a magnet to transfer the  
215 sample(s) between the hot and the cold zone (e.g., Gaillard et al., 2003).

216 Additionally, experimental techniques have been developed to observe bubble formation *in situ*,  
217 recording the nucleation and growth rates via digital video cameras and time-lapse photography.  
218 Most *in situ* observations setups are limited to atmospheric pressures, e.g., using a special  
219 furnace-setup at a X-ray beamline (Bai et al., 2008; 2011) or a heating stage on an optical  
220 microscope (e.g., Bagdassarov et al., 2000; Navon et al., 1998) or a moissanite cell apparatus  
221 (see, e.g., Schiavi et al. (2010) for detailed description). Efforts have been made to modify an  
222 internally heated vessel, adding a transparent sapphire window for *in situ* observation at high-  
223 temperatures and high-pressures (TIHPV; Gondé et al, 2006; 2011). This vessel design requires a  
224 high degree of maintenance and, thus, has unfortunately been abandoned (*Laporte and Gondé,*  
225 *personal correspondence*).

226 Decompression experiments in externally heated diamond anvil cells also allow *in situ*  
227 observation of bubble formation through, e.g., moissanite windows (Masotta et al., 2014). Here,  
228 the decompression rate is adjusted by (controlled) cooling of the sample chamber. Results of

229 such experiments are not directly comparable to isothermal decompression experiments owing to  
230 the strong influence of temperature on melt parameters such as viscosity and volatile diffusivity,  
231 which affected bubble formation, growth and coalescence.

232 For completion of the experimental device list, we want to mention decompression experiments  
233 performed in piston-cylinder apparatuses (PCA), simulating volatile degassing at greater depths  
234 corresponding to the lower mantle regime (e.g., Hardiagon et al., 2013). PCAs use steel pistons  
235 to compress a solid pressure medium surrounding the sample, reaching pressures up to several  
236 GPa. Cells are commonly made of, e.g., NaCl, BN, MgO and/or pyrex (e.g., Johannes et al.,  
237 1971). Gas pressure vessels (i.e., IHPV and CSPV) allow relatively large sample volumes and  
238 provide enough space for the capsule volume to expand owing to the formation of a fluid phase  
239 in the melt, while the gas pressure is measured directly by pressure transducers and gauges.  
240 Whereas in PCA experiments the sample pressure inside the apparatus has to be calibrated to the  
241 external oil pressure applied onto the steel pistons. Also there are concerns that at high  
242 decompression rates the oil pressure release is faster than the reaction (relaxation) time of the  
243 solid media around the capsule (*Hardiagon, personal correspondence*), leading to deviation of  
244 the pressure shown at the pressure transducer in relation to the true pressure on the sample (e.g.,  
245 Boyd and England, 1960). Thus, additional calibrations are necessary, which can be quite  
246 challenging and time-consuming, and a constant decompression rate may not be possible.

247 In the following, we will focus on “shallow depth” decompression experiments, simulating the  
248 magma ascent from magma chamber depth (equivalent to 300-500 MPa) to near-surface  
249 pressures.

250

251

## 252 **2.2 Capsule material and experimental design**

253 The majority of the bubble nucleation experiments were conducted in gas or hydrothermal  
254 pressure vessels using Ar±H<sub>2</sub> gas mixtures or H<sub>2</sub>O as a pressure medium. For these experiments,  
255 capsules suitable for magmatic pressures and temperatures are required (cf. Gondé et al., 2011;  
256 Fiege et al., 2014a). Here, Au is often the preferred material (e.g., Mangan et al., 2004a; 2004b),  
257 whereas other noble metal containers such as Pt and AuPd are also used (e.g., Gondé et al., 2011;  
258 Preuss et al., 2014), having the advantage to allow higher temperatures. However, the run  
259 durations are limited for Fe- and/or S-bearing compositions because the latter capsule materials  
260 form alloys with the Fe and S in the melt, which can lead to capsule failure (e.g., Barr and Grove,  
261 2010; Zajacz et al., 2012; 2013; Fiege et al., 2015). A notable advantage of Au and Pt over AuPd  
262 (or even AgPd) alloy is certainly the high flexibility and elasticity of Au and Pt at high  
263 temperatures, which allows a better response to changes in pressure and, thus, also decreases  
264 chances of capsule failure (*pers. experience of the authors*).

265 Preliminary results of Preuss et al. (2014) indicate that using glass powder in the experimental  
266 setup instead of glass cylinders can lead to a "preferred" bubble nucleation on former grain  
267 boundaries and more likely, on N<sub>2</sub>-rich bubbles, which can form early during decompression  
268 owing to the low solubility (Carroll and Webster, 1994). Moreover, first results of Marxer et al.  
269 (2013) show that the capsule design can have a significant effect, at least on the shape of the  
270 bubbles. The fluid (and melt) density increases significantly during quenching, leading to a  
271 shrinkage (isometric contraction or deformation/flattening) or even a collapse of bubbles  
272 (Marxer et al., 2013; 2015). The bubbles stop to shrink at a fictive temperature that is possibly  
273 close to the glass transition temperature (T<sub>g</sub>; Marxer et al., 2015). In experiments terminated  
274 using a rapid-quench technique the samples are typically cooled below the glass transition

275 temperature within a few seconds (e.g. Berndt et al., 2002). It should be emphasized that this  
276 quench related effect might be enhanced by the capsule design and material, since flat crimped  
277 run products of experiments performed in Au or Pt capsules typically do not show evidence of  
278 significant bubble deformation owing to quench related contraction (e.g., Hamada et al, 2010;  
279 Fiege et al., 2014a; 2015).

280 The undesired interaction of Fe and S of melt with the noble metal capsules, leading to Fe and S  
281 loss of the melt, can be avoided by using inner containers made out of, e.g., quartz (Fleet et al.,  
282 1991) or olivine (Beermann et al., 2011), which are suitable for high-temperature experiments at  
283 constant pressures. In these experimental setups a piston or lid is used to separate the melt inside  
284 the crystal container from an outer noble metal container. However, once pressurized these  
285 setups respond slowly and unpredictably to a pressure decrease in the vessel; i.e., continuous,  
286 controlled decompression is not possible (similar problem as for piston cylinder experiments).  
287 To our knowledge, successful decompression experiments using quartz, olivine or similar  
288 capsule materials do not exist.

289 Furthermore, as mentioned above, Masotta et al. (2014) performed experiments using a Bassett-  
290 type externally-heated diamond anvil cell, which allows *in situ* observation of bubble formation  
291 through moissanite windows. In these experiments, fluid-saturation and, thus, bubble formation  
292 is induced via rapid-cooling. The results provide valuable information, for example, about the  
293 required supersaturation pressure ( $\Delta P_N$ ) in different melt compositions (< 60 MPa in basalt and  
294 andesite; ~200 MPa in rhyodacite) and bubble growth rates. The experimental setup also allows  
295 the evaluation of the dominating degassing process (e.g., bubble growth vs. nucleation) at  
296 different stages of volatile exsolution. However, the sole effect of decompression rate ( $\approx$  magma  
297 ascent rate) cannot be tested by this experimental approach, since simultaneous cooling probably

298 affects significantly the bubble formation, growth and/or coalescence. For instance,  
299 heterogeneous bubble nucleation occurs simultaneously with crystal nucleation in the  
300 experiments of Masotta et al. (2014), which may have influenced supersaturation pressure  $\Delta P_N$   
301 and, hence, the degassing processes.

302

### 303 **2.3 Starting composition**

304 The majority of the published experimental studies were performed using evolved rhyolitic melt  
305 compositions at fluid-saturated conditions prior to decompression. Here, glass (drilled) cylinders  
306 or pieces of synthetic or natural glasses are typically hydrated in a first step (cf., Mourtada-  
307 Bonnefoi and Laporte, 2002). More recently the experimental community started to focus on less  
308 evolved systems (Mangan et al., 2004b; Cichy et al., 2011; Pichavant et al., 2013; Fiege et al.,  
309 2014a; Masotta et al., 2014). Here, Gondé et al. (2011) observed that water-undersaturated  
310 rhyodacitic melts may produce up to 3 log units higher BND than water-saturated ones at similar  
311 decompression rates, which seems to be consistent with experimental results of Fiege et al.  
312 (2014a) and Preuss et al. (2014). Considering that ( $\pm$ CO<sub>2</sub>-free) natural systems are often not  
313 fluid-saturated prior to decompression, these observations are very important but certainly  
314 require further systematic experimental investigations.

315

### 316 **2.4 Decompression style**

317 Experimental studies on different pressure release techniques have emphasized the importance of  
318 the decompression paths on (homogeneous) bubble nucleation in melts (e.g., Nowak et al., 2011;  
319 Marxer et al., 2015). The three major styles used in literature are i) *single-step*, ii) *multi-step* and  
320 iii) *continuous decompression*; see Fig. 1. The single-step method simulates a scenario where the

321 entire magma ascent (from greater depths at the initial pressure  $P_i$  up to shallower depths at the  
322 final pressure  $P_f$ ) is accomplished instantaneously within the first seconds of the experiments.  
323 Here, the subsequent annealing time ( $t_A$ ) at final pressure determines the overall, integrated  
324 decompression rate ( $r_{int} = \Delta P/\Delta t$ ; in this case corresponds to  $[P_i - P_f]/t_A$ ). The multi-step method  
325 consists of a number of regular instantaneous pressure drops of fewer MPa followed by short-  
326 term annealing times at intermediate pressures until final experimental pressures have been  
327 reached and the experiment is quenched. In both cases the pressure release is typically conducted  
328 by manually opening needle valves to release the pressure medium (e.g., Ar gas or water) from  
329 the IHPV or CSPV. Whereas in a continuous decompression path no severe pressure drops occur  
330 but rather a controlled release of pressure at an uninterrupted manner. The sample is cooled  
331 immediately when the final pressure is reached (i.e.,  $t_A = 0$  h). Continuous pressure release has  
332 been mainly performed manually by opening a bleeding valve and monitoring the pressure on a  
333 strip chart recorder (e.g., Hamada et al., 2010), or can be done at very low decompression rates  
334 by issuing a piezoelectric-driven valve while visually controlling the values read from the  
335 pressure transducer with the number of ascending gas bubbles released into a water-filled glass  
336 column at the end of the pressure line (Nowak et al., 2011). Another possible way to perform  
337 experiments at constant decompression rates includes connecting two (or more) gas pressure  
338 vessels (IHPV or CSPV) and adjusting the decompression rate via controlled cooling of the  
339 connected vessel(s) while running the sample in the other vessel at constant temperature.  
340 However, with this technique, the range of decompression rates (fast rates are not possible) and  
341 the total decompression  $\Delta P$  is rather limited (see, e.g., Waters, 2013); i.e., the pressure may only  
342 be decreased by a factor of  $\sim 2$  via cooling of a connected “empty” vessel.

343 The study of Nowak et al. (2011) shows that homogeneous bubble nucleation is the dominant  
344 bubble forming process during a single-step pressure release (large number of relatively small  
345 bubble sizes, leading to a large BND), while bubble growth is dominating in continuously  
346 released water-saturated rhyodacitic melts (low bubble number density resulting from only few  
347 larger sized bubbles). A multi-step decompression technique can be seen as the intermediate case  
348 between the formerly discussed methods, where the predominance of either bubble nucleation or  
349 growth is mainly controlled by the number of reoccurring decompression-annealing steps, i.e., by  
350 the step size of the individual pressure drops.

351 In the results and discussion sections of this review article we will mainly focus on  
352 decompression experiments using continuous, constant decompression rates or multi-step  
353 approaches with very small steps (< 1 MPa), because of the better applicability to natural  
354 systems and the better reproducibility (see Section 4.6 and Marxer et al., 2015).

355

356

### 3. Analytical techniques

357 Chemical analyses of experimental run products are consulted in order to determine whether the  
358 volatile exsolution during decompression occurred in equilibrium or not. Especially very fast  
359 decompressed samples may end up having significantly higher contents of dissolved volatiles  
360 (e.g., H<sub>2</sub>O, CO<sub>2</sub>) in their residual melts in comparison to isobaric solubility experiments at final  
361 pressures. Mass balance calculations based on electron microprobe analysis (EMPA) datasets as  
362 well as Raman or Fourier transform infrared (FTIR) spectroscopy and Karl-Fischer titration are  
363 the most common techniques for water and carbon dioxide determination in the melt. Only few  
364 studies have made the effort to analyze the volatile content trapped inside the bubbles in order to  
365 calculate overpressures (e.g., CO<sub>2</sub>-bubbles in mid-ocean ridge basalts; Burnard, 1999).

366 A very powerful tool for understanding bubble formation processes, their time-scales and  
367 relationship to eruption dynamics is the image and texture analysis of two- and three-  
368 dimensional vesicle features such as size, number and shape as well as nucleation and growth  
369 rates. Here, structural features such as interpenetration shapes, dimples or flattened inter-bubble  
370 melt films indicate a contribution of bubble coalescence (Castro et al., 2012). Textural analyses  
371 can be subdivided into two- and three-dimensional methods, which will be described separately  
372 in the following two sections.

373

### 374 **3.1 2D methods**

375 Two-dimensional (2D) digital images can be obtained by various techniques, e.g., optical or  
376 scanning electron microscopy, and are usually taken at various magnifications and locations to  
377 reduce truncation effects (= underestimation of the largest and/or the smallest bubbles; see  
378 Armienti, 2008). With the help of image processing programs (e.g., *ImageJ*;  
379 <http://imagej.nih.gov/ij/>) parameters such as area, width, length, and circularity of individual  
380 bubbles as well as the overall total area, average size and area fraction of vesicles throughout the  
381 images can be determined. The detection limit of single objects of interest is dictated by the  
382 magnification and resolution of the digital picture.

383 The next step is typically the stereological conversion of the two-dimensional results into three-  
384 dimensional (3D) information. The simplest approach is to assume perfectly shaped bubble  
385 spheres or, typically more appropriate, ellipsoidal shapes for vesicles of irregular (non-spherical)  
386 geometry, applying their general volume formulas and inserting these values into equations to  
387 determine population densities ( $n$ ) used in bubble size distribution (BSD) plots, or to calculate  
388 bubble number densities (BND); see also Noguchi et al. (2008); Cichy et al. (2011).

389 The calculation of 3D bubble or particle distributions based on 2D information is complex and  
390 several approaches were published within the last decades (e.g., Higgins, 1994; Peterson, 1996;  
391 Sahagian and Proussevitch, 1998). Computer programs have been created, which allow a (semi-  
392 automatic stereological conversion of 2D into 3D data. Whereas the FOAMS software is limited  
393 to the assumption of spherical bubbles (Shea et al., 2010;  
394 <http://www2.hawaii.edu/~tshea/foams/foamsintro.html>), the CSDcorrection software by Higgins  
395 (2000, 2002, 2006, 2007; <http://www.uqac.ca/mhiggins/csdcorrections.html>) allows also the  
396 input of aspect ratio and circularity data of objects, reducing the stereological error and providing  
397 non-spherical bubble volumes presented in size distribution plots. Additionally, new ImageJ  
398 plugins have been made available that allow the easy data transfer into the CSDcorrection  
399 program. Higgins's software provides, for instance, the classic size distribution diagrams and  
400 corresponding tables; including the bubble number per size intervals, which give the BND when  
401 summed up.

402

### 403 **3.2 3D methods**

404 Within the last couple of years, non-destructive, high-resolution computer tomography (CT) or  
405 X-ray  $\mu$ -tomography became popular among researchers studying natural and experimental rock  
406 textures. The main advantage of 3D-imaging is the resolution of possible bubble networks (e.g.,  
407 owing to coalescence) and orientations that are otherwise not or not clearly visible in 2D-images.  
408 These tomographic scan datasets consist of 2D slice images, which can be individually processed  
409 as two-dimensional images as described in the previous section, or the entire set of images can  
410 be implemented into 3D computer programs. There is a number of commercially licensed 3D-  
411 software available, but also a couple of freeware, which are customized to the mineralogical

412 scope of texture analysis, e.g., BLOB3D (Ketcham, 2005; <ftp://ftp.ctlab.geo.utexas.edu/Blob3D/>)  
413 and YaDiV (Friese et al., 2013; <http://www.welfenlab.de/yadiv.html>). These programs allow the  
414 calculation of bubbles numbers and individual (true) bubble volumes via 3D-segmentation and  
415 separation of density-related grey values. Additionally, the segmented volumes of interest are  
416 visualized in 3D, which may unravel preferred orientation or flow structures that would have not  
417 been resolved with 2D-images only (see Fig. 2).

418

## 419 **4. Results and Discussion of the experimental database**

### 420 **4.1 Supplementary decompression experiments**

421 Recent studies indicate a significant effect of the melt composition on bubble formation and  
422 evolution during decompression (cf. Masotta et al., 2014; Fiege et al., 2014a). To further  
423 investigate the potential effect of (minor) volatile species such as S and Cl on the bubble number  
424 density during magma ascent, we performed three additional continuous decompression  
425 experiments for this review article, following the experimental and analytical strategy described  
426 by Fiege et al. (2014a); a more detailed description of the experiments is provided in Fiege et al.  
427 (2014b). We used the same anhydrous dacitic andesite as a starting material (see notes below  
428 Table A.1; appendix A).

429 In brief, the experimental procedure comprises three steps: 1) Synthesis of an anhydrous  
430 andesitic glass (1 atm; 1600 °C; 2 × 2 h); 2) Hydration (~6.2 wt% H<sub>2</sub>O) of the glass in an  
431 internally heated pressure vessel (IHPV) at 1030 °C, 500 MPa for 12 h. Minor amounts of sulfur  
432 (~80 ppm) were added to the system using gypsum (Ca[SO<sub>4</sub>] 2H<sub>2</sub>O); 3) Continuous  
433 decompression experiments in an IHPV at 1030 °C. The initial pressure of the decompression  
434 experiments was 400 MPa. The pressure was released continuously at a constant decompression

435 rate of 0.1 MPa/s and the samples were quenched (rapid-quench technique) at final pressures of  
436 150, 100 and 70 MPa. The synthesis and the decompression experiments were performed at  
437  $\log(fO_2) = FMQ+3.6$  (fayalite-magnetite-quartz buffer).

438 We collected five back scattered electron (BSE) images at different magnifications and locations  
439 on each run product (selected images are shown in Fig. A.1; appendix A) and analyzed the  
440 images following the procedure described by Fiege et al. (2014a). All relevant details for the  
441 experiments as well as the BND values obtained for each run product are given in Table A.1 (see  
442 appendix A). The analytical results of these additional run products are compared to literature  
443 data and discussed in the following sections.

444

#### 445 **4.2 Homogeneous vs. heterogeneous bubble nucleation**

446 Bubble nucleation in melts and magmas can be homogeneous or heterogeneous. Homogeneous  
447 bubble nucleation requires relatively high supersaturation pressures ( $\Delta P_N = P_N - P_{SAT}$ ;  $P_N$ :  
448 nucleation pressure;  $P_{SAT}$ : volatile-saturation pressure) and typically occurs in systems without  
449 phases that can serve as preferential nucleation sites (Hurwitz and Navon, 1994). Mangan et al.  
450 (2004a) showed, based on numerical modeling using available experimental data that  
451 heterogeneous bubble nucleation is triggered in water-saturated rhyolite at supersaturation  
452 pressures  $\Delta P_N < 5\text{-}20$  MPa, while a supersaturation pressure of  $> 120\text{-}150$  MPa is required for  
453 homogeneous nucleation.

454 The interaction between crystals and heterogeneously forming (bubble-) nuclei is illustrated in  
455 Fig. 3. It is emphasized that the sketched Fe-(Ti)-oxides in Fig. 3, serving as preferred nucleation  
456 sites, are to be seen as examples. Even though, to our knowledge, only Fe-(Ti)-oxides have been  
457 proven to trigger heterogeneous nucleation (e.g., Hurwitz and Navon, 1994; Cluzel et al., 2008),

458 other oxides such as hematites (e.g., Gardner and Denis, 2004; Gardner, 2007) and magnetites  
459 (Edmonds et al., 2014; Knipping et al., 2015), but also (noble) metals (e.g., Mangan and Sisson,  
460 2000) or even sulfides (Mungall et al., 2015) may have a similar effect. For instance,  
461 experimental data from Matveev and Ballhaus (2002) indicate that the presence of chromites  
462 probably favors heterogeneous bubble nucleation, while silicates such as plagioclase may have a  
463 minor or even no effect (e.g., Cichy et al., 2011). According to Hurwitz and Navon (1994) a flat  
464 interface between bubble and melt is formed when the wetting angle ( $\Psi$ ) reaches  $135^\circ$  ( $\Psi = 180^\circ$   
465  $- \theta$ ;  $\theta$  is the contact angle; the correct determination of wetting and contact angles can be found in  
466 Gualda and Ghiorso; 2007). Here, the wetting angle can be used to calculate the wetting factor  
467 ( $\Phi$ ), which is required to calculate supersaturation pressures for heterogeneous bubble nucleation  
468 (see equations shown in Fig. 3); i.e.,  $\Phi = 1$  for homogeneous nucleation ( $\Psi = 0^\circ$ ). Hurwitz and  
469 Navon (1994) showed that the supersaturation pressures can decrease down to  $\sim 1$  MPa in  
470 hydrous rhyolites, which contain Fe-Ti-oxide microlites and this was recently confirmed by *in*  
471 *situ* observation of Masotta et al. (2014) using a diamond-anvil apparatus.

472 It is worth noting that heterogeneous bubble nucleation usually also occurs in experiments  
473 ultimately designed to investigate homogeneous nucleation processes. Here, numerous but small  
474 bubbles often form within a tiny layer (= fringe) of  $\leq 10 \mu\text{m}$  at the melt-capsule interface. These  
475 bubbles are often referred to as “fringe” bubbles (cf. Mangan and Sisson, 2000) and have to be  
476 excluded for the determination of BND, BSD, etc.

477 For homogeneous bubble nucleation a negative correlation between the supersaturation pressure  
478 and the initial  $\text{H}_2\text{O}$  content in the melt was observed by Mourtada-Bonnefoi and Laporte (2002),  
479 while the supersaturation pressure was found to increase with increasing  $\text{CO}_2$  concentration. This  
480 is directly related to changes in volatile-saturation pressure, i.e., to the influence of pressure on

481 H<sub>2</sub>O and CO<sub>2</sub> solubility in the silicate melts (e.g., Burnham, 1975; Holtz et al., 1992; Moore et  
482 al., 1995; Jakobsson, 1997; Shishkina et al., 2010; Lesne et al., 2011a, 2011b, 2011c).

483 In the following sections we will present and evaluate experimental results for homogeneous and  
484 heterogeneous bubble nucleation, respectively. As mentioned previously, we will mainly focus  
485 on experimental studies using continuous or almost continuous (e.g., multi-step decompression  
486 with small step sizes) decompression rates for the experiments. The set of available data  
487 (homogeneous and heterogeneous) is listed in Table 1 (all known bubble nucleation studies using  
488 continuous decompression technique are considered; selected studies using single- or multi-step  
489 technique are listed, too).

490

#### 491 **4.3 Available data for homogeneous bubble nucleation**

492 Understanding bubble number density related to homogeneous bubble nucleation in silicate  
493 melts during continuous decompression has been the objective of ten experimental studies  
494 published in the last ~15 years. While the majority of these studies focuses on evolved rhyolitic  
495 compositions (six studies), experimental data on decompression-induced homogeneous bubble  
496 nucleation in less evolved systems are very limited (see Fig. 4). Two relevant studies were  
497 published using intermediate melt compositions (rhyodacite: Gondé et al., 2011; andesite: Fiege  
498 et al., 2014a) and two using mafic melt composition (phonolite: Marxer et al., 2015; basalt:  
499 Pichavant et al., 2013). Additionally, Masotta et al. (2014) use rhyolitic, andesitic and basaltic  
500 compositions; however, the bubble nucleation in the studied systems is related to cooling and,  
501 thus, not directly comparable; i.e., the cooling-induced crystallization can change the degassing  
502 mechanism from homogeneous to heterogeneous.

503 Fig. 4a shows a compilation of the available experimental data, while Fig. 4b represents an  
504 enlarged view of 4a, focusing on BND values obtained at 800 °C for initially volatile-saturated  
505 rhyolite melts, containing variable amounts of CO<sub>2</sub> (0 to ~800 ppm). Notably, experimental  
506 results for decompression rates  $\leq 0.02$  MPa/s are very limited. The model of Toramaru (2006;  
507 see Section 5.1) is used to predict a trend for rhyolitic compositions at 800 °C. Although some  
508 datasets scatter significantly and (possible) effects of volatile contents and (anhydrous) melt  
509 composition have to be considered for a qualitative interpretation, the results indicate that for  
510 rhyolitic compositions the influence of temperature on BND may be rather small in the range of  
511 700 to 1000 °C, which is consistent with observations made by Gondé et al. (2011) for  
512 rhyodacite.

513 On the other hand, melt composition seems to play a more significant role (e.g., Bai et al., 2008;  
514 Gondé et al., 2011; Fiege et al., 2014a; Masotta et al., 2014). Here, the compositional effect can  
515 be subdivided into effects related to significant changes in major element composition (e.g., from  
516 rhyolite to basalt) and effects related to changes in volatiles/fluid composition (e.g., variations in  
517 relative concentrations of H<sub>2</sub>O, CO<sub>2</sub>, S and Cl). For instance, for a given decompression rate, the  
518 bubble number density seems to increase by about two log unit from (evolved) rhyolitic to  
519 (primitive) basaltic melt compositions (see Fig. 4). Moreover, a positive correlation is observed  
520 between BND and CO<sub>2</sub> content. Here, the addition of ~800 ppm CO<sub>2</sub> may lead to an increase of  
521 BND by more than one log units (see Fig. 4b). However, the relevant data scatter quite a bit and  
522 experiments at 1 atm. show that  $\geq 880$  ppm CO<sub>2</sub> are required to affect bubble nucleation to a  
523 significant extent (Bai et al., 2008).

524 Gardner (2012) performed homogeneous bubble nucleation experiments using a water-saturated  
525 phonolitic melt. The author applied an experimental technique, which includes a fast

526 decompression step ( $\sim 4$  MPa/s at 1150 °C or  $\sim 12$  MPa/s at 875 °C) followed by 10 to 37 s of  
527 annealing. Therefore, the results are probably not directly comparable to continuous  
528 decompression experiments, which are followed by immediate rapid-quench (cf., Nowak et al.,  
529 2011). However, while the highly variable BND values that Gardner (2012) obtained for 875 °C  
530 [ $\log(\text{BND} \cdot \text{mm}^3) = 1.4$  or  $4.6$ ] are somewhat hard to interpret, the BND values determined for  
531 1150 °C (average  $\log(\text{BND} \cdot \text{mm}^3) = 2.0 \pm 0.6$ ) are obviously very low for an integrated  
532 decompression rate of  $\sim 4$  MPa/s when compared to the compiled data shown in Fig. 4. This  
533 indicates that the effect of melt composition on BND is possibly inversed if a melt is fluid-  
534 saturated (instead of fluid-undersaturated) prior to decompression conditions [*please note*: the  
535 only relevant experimental results on non-rhyolitic compositions are based on experiments using  
536 water-undersaturated starting glasses (Gondé et al., 2011; Pichavant et al., 2013; Fiege et al.,  
537 2014a)]. Although, a more reasonable explanation for the low BND values found by Gardner  
538 (2012) at 1150 °C in phonolitic systems is that the decrease in BND with annealing after  
539 decompression is much more significant in less evolved, mafic (phonolitic) systems at 1150 °C  
540 than in intermediate (andesitic) systems at 1030 °C (see Fig. 6 and Section 4.4), owing to higher  
541 diffusivity and lower melt viscosities. The compositional effects on homogeneous bubble  
542 nucleation are further discussed in Section 5.1.

543

#### 544 **4.4 Available data for heterogeneous bubble nucleation**

545 There are five experimental studies on heterogeneous bubble nucleation using (almost)  
546 continuous and constant decompression rates in their experimental setup (Mangan and Sisson  
547 2000; Mangan et al, 2004a; 2004b; Cluzel et al., 2008; Cichy et al., 2011). Notably, to date, the  
548 effect of the decompression technique (continuous, multi-, single-step) has only been studied for

549 homogeneous bubble nucleation (Nowak et al., 2011; Marxer et al., 2015). Thus, although the  
550 main focus of this paper is to review results of continuous decompression experiments, Fig. 5  
551 includes also results from three of the most comprehensive studies using single- (Gardner and  
552 Denis, 2004; Gardner, 2007) or multi-step (Cichy et al., 2011) approaches in order to evaluate  
553 the possible effect of changing decompression style on heterogeneous bubble nucleation. The  
554 results from single- (or multi-) step experiments (Fig. 5a) clearly show that temperature and  
555 decompression rate have small to negligible influence on BND. In contrast, in crystal-poor  
556 rhyolitic systems at 800 to 900 °C, a strong positive correlation between BND and  
557 decompression rate can be observed if a continuous decompression technique is applied, while  
558 the effect of temperature may also be negligible [Fig. 5b; compare data from Mangan and Sisson  
559 (2000) to results from Cluzel et al. (2008)]. This behavior is very similar to what can be observed  
560 for homogeneous bubble nucleation (see Section 4.3; Fig. 4), as already noted by Mangan and  
561 Sisson (2000), and indicates that degassing of rhyolitic magmas is rather controlled by  
562 homogeneous than heterogeneous nucleation if the crystal content is below a certain threshold  
563 ( $\ll 1$  vol% or  $\leq 10^4$  crystals/cm<sup>3</sup>). On the other hand, a significant temperature-dependence can  
564 be observed for the bubble formation in Fe-(Ti)-oxides-bearing runs (see Fig. 5b). Here, a strong  
565 positive correlation between BND and decompression rate at 950 °C is indicated by the data of  
566 Mangan et al. (2004a), while at lower temperatures (~850 °C) this effect is again rather small  
567 (Mangan et al., 2004b). At 850 °C a change in bulk composition from rhyolitic to rhyodacitic  
568 and, thus, a further increase in total crystal content, may also have a minor effect. Notably, the  
569 run products of Cichy et al. (2011) contain only very small amounts of Fe-(Ti)-oxides (< 0.1  
570 vol%), while the total crystal fraction ranges between ~1 and ~9 vol%, indicating that minerals  
571 such as amphibole, clinopyroxene, orthopyroxene and/or plagioclase, which are present in

572 varying abundances in the experiments of Cichy et al. (2011), may change the degassing  
573 mechanism from dominantly homogeneous to dominantly heterogeneous bubble nucleation.  
574 Furthermore, the results for rhyolitic to rhyodacitic Fe-(Ti)-oxides-bearing systems at 850 °C are  
575 almost indistinguishable from those using multi- or single-step technique, indicating that such  
576 systems can be studied using multi- or single-step approaches without risking “artificial”  
577 (unnatural) effect.

578

#### 579 **4.5 The effect of annealing after decompression**

580 There are several studies using a single-step decompression approach followed by various times  
581 of annealing. However, to our knowledge, only the study of Fiege et al. (2014a) applies the  
582 continuous decompression technique to investigate the influence of subsequent annealing on  
583 (homogeneous) bubble nucleation and evolution in andesitic melts at 1030 °C. The results show  
584 that BND decreases by  $\geq 1$  log unit during the first  $\sim 5$  h of annealing (Fig. 6a). Based on the total  
585 duration of the experiment after initiation of the decompression and the total decrease in  
586 pressure, we have calculated the integrated decompression rate ( $r_{\text{int}}$ ) for the experiments shown  
587 in Fig. 6a. In Fig. 6b we compare the results shown in Fig. 6a but using the integrated  
588 decompression rate, to the continuous decompression experiments by Fiege et al. (2014a)  
589 without annealing but at various decompression rates. Fig. 6b reveals that significant difference  
590 may be observed for experiments annealed for 1 to 5 h after fast decompression, while  
591 experiments annealed for  $\geq 72$  h seem to produce similar BND values at a given (integrated)  
592 decompression rate. These observations have two main implications:

593 i) A simple approach using a relatively fast decompression rate ( $\sim 0.1$  MPa/s) in a first stage  
594 followed by long term annealing ( $\geq 72$  h) at final pressure in a second stage should produce

595 similar BND than an experiment based a continuous decompression approach with a rate  
596 identical to the integrated decompression rate used for the two-stages setup. This observation is  
597 of high importance for the design of future experiments since an almost constant and fast  
598 decompression rates of  $\geq 0.1$  MPa/s can be easily adjusted by simply bleeding gas out of a CSPV  
599 or IHPV via a manual valve; i.e., a special low-flow rate decompression valve is not necessarily  
600 required.

601 ii) Average magma ascent rates are often estimated based on a distinct seismic activity prior to  
602 eruption, the time of eruption and geophysical data constraining the approximate depth of the  
603 magma source (e.g., Shimizu et al., 1997; Cashman, 2004; Scandone et al., 2007; Castro and  
604 Dingwell, 2009; Sparks et al., 2012; Jousset et al., 2013). Here, magmas ascend with a velocity  
605 of  $> 10$  km/h during Plinian eruptions, while the ascent rate for Volcanian eruptions is probably  
606  $< 0.1$  km/h. The high kinetic energy of magmas traveling upwards at  $> 10$  km/h may easily allow  
607 it to overcome most obstacles along the conduit; i.e., the magma ascends almost continuously to  
608 the surface. On the other hand, magmas, which are characterized by significantly lower kinetic  
609 energy during eruption (i.e., much lower ascent rates), may easily stop ascending or slow down  
610 considerably for a certain amount of time before continuing to ascend to the surface. Here, the  
611 results presented in Fig. 6a indicate that such an intermittent ascent does not affect the final  
612 vesiculation of the volcanic ejecta if the average (integrated) ascent rates are  $\leq 0.001$  MPa/s ( $\pm$   
613 Volcanian eruptions: Cashman, 2004).

614

#### 615 **4.6 The effect of decompression path on bubble forming processes**

616 In general, bubble number densities produced by single-step and multi-step (depending on step  
617 size) runs can be orders of magnitude higher than BND of continuous style decompression

618 experiments at a given (integrated) decompression rate (Nowak et al., 2011; Marxer et al., 2015).  
619 This has to be considered for the interpretation of BND values of natural samples based on  
620 experimental results. We think that in volcanic systems two decompression/ascent scenarios are  
621 most likely:

622 i) A magma starts to ascend along the conduit and moves all the way towards the surface without  
623 major interruptions, which would result in a continuous decompression at a quite constant  
624 decompression rate. These eruptions are most appropriately simulated by continuous  
625 decompression experiments.

626 ii) A magma starts to ascend but the upwelling is interrupted at a certain place (or places) along  
627 the conduit; i.e., the kinetic energy of the magma, related to buoyancy, does not allow it to  
628 overcome an obstacle. Here, after decompression, which can induce degassing (depending on  
629 volatile contents and total pressure decrease  $\Delta P$ ), the magma may remain for a certain time (=   
630 annealing time) at certain pressure-temperature conditions before it (may or may not) continues  
631 to ascend to the surface. Similar degassing processes can be induced if a magma volume from a  
632 deeper reservoir ascends and intrudes into a shallower reservoir, assuming that the change in  
633 pressure is sufficient to reach volatile-saturation. The vesiculation within such magmas at  
634 relatively shallow depth is most appropriately simulated by continuous decompression  
635 experiments, which are annealed for certain times after decompression at final pressure-  
636 temperature conditions.

637 While scenario i) is more likely in Subplinian to Plinian eruptions where the momentum of an  
638 ascending magma is high enough to overcome possible obstacles, a rather slowly ascending  
639 magma might get stuck on its way to the surface. Here, fluid-melt disequilibrium conditions  
640 related to fast (Plinian style) decompression can lead to overpressurization within the upwelling

641 melt/magma and, thus, may result in more explosive volcanic eruptions (e.g., Mangan and  
642 Sisson, 2000). In agreement with recent results of Marxer et al. (2015), we strongly recommend  
643 to use only continuous or almost continuous (step size < 1 MPa) decompression techniques,  
644 which also improves the reproducibility of the experiments (Marxer et al., 2015).

645

## 646 **5. Implications for natural systems**

### 647 **5.1. Compositional effects and decompression-rate-meter(s)**

648 Toramaru (2006) developed a model, which allows one to predict the bubble number density for  
649 a given decompression rate and, thus, is a valuable tool to estimate decompression rates ( $\approx$   
650 magma ascent rates) based on the vesiculation of natural samples (e.g., pumices). Here, the  
651 following equation based on numerical simulations of Toramaru (1995, 2006) and provided by  
652 Hamada et al. (2010) can be used to predict BND:

$$653 \text{ BND} \approx 34 \cdot C_{\text{SAT}} \cdot \left( \frac{16 \cdot \pi \cdot \sigma_{\text{LB}}^3}{3 \cdot k \cdot T \cdot P_{\text{SAT}}^2} \right)^{-2} \cdot \left( \frac{\Omega_{\text{L}} \cdot P_{\text{SAT}}}{k \cdot T} \right)^{-\frac{1}{4}} \cdot \left( \frac{P_{\text{SAT}}^2 \cdot k \cdot T \cdot C_{\text{SAT}} \cdot D_{\text{H}_2\text{O}}}{4 \cdot \sigma_{\text{LB}}^2 \cdot r} \right)^{\frac{3}{2}} \quad (3),$$

654 where  $C_{\text{SAT}}$  is the H<sub>2</sub>O content at saturation pressure expressed as the number of H<sub>2</sub>O-molecules  
655 per unit volume of liquid,  $\sigma$  is the surface tension of the bubble-liquid interface in N/m,  $k$  is the  
656 Boltzmann constant ( $1.38 \times 10^{-23}$  J/K),  $T$  is the temperature in K,  $P_{\text{SAT}}$  is the H<sub>2</sub>O-saturation  
657 pressure in Pa,  $\Omega_{\text{L}}$  is the molecular volume of H<sub>2</sub>O in the liquid (typically fixed to  $3 \times 10^{-29}$  m<sup>3</sup>;  
658 Toramaru 1989; Hamada et al. 2010),  $D_{\text{H}_2\text{O}}$  is the H<sub>2</sub>O diffusivity in the melt in m<sup>2</sup>/s, and  $r$  is the  
659 decompression rate in Pa/s. The surface tension of the bubble-liquid interface  $\sigma$  can be estimated  
660 using the following equation 4 (e.g., Hirth et al. 1970; Blander and Katz 1975; Hurwitz and  
661 Navon 1994; Mangan and Sisson 2005; Gardner and Ketcham 2011):

$$662 \quad J = \frac{2 \cdot n_0^2 \cdot \Omega_L \cdot D_{\text{H}_2\text{O}} \cdot [\sigma_{\text{LB}} / (k \cdot T)]^{1/2}}{a_0} \cdot \exp \left[ \frac{-16 \cdot \pi \cdot \sigma_{\text{LB}}^3}{3 \cdot k \cdot T \cdot \Delta P^2} \right] \quad (4),$$

663 where  $J$  is the nucleation rate, which is calculated by dividing the BND by the time allowed for  
664 nucleation ( $t_N$ ; see, e.g., Gardner and Ketcham 2011).

665 While this model reproduces experimental data of H<sub>2</sub>O-saturated rhyolitic melts relatively well,  
666 it fails to reproduce H<sub>2</sub>O-undersaturated melts and/or less evolved melt compositions (Gondé et  
667 al., 2011; Fiege et al., 2014a). The H<sub>2</sub>O-undersaturated andesitic melts are characterized by 1-2  
668 log units higher BND values at a given decompression rate when compared to H<sub>2</sub>O-saturated  
669 rhyolitic melts. Moreover, the model of Toramaru (2006) does not consider the possible effect of  
670 variation in volatile composition on bubble nucleation. It has been noted that CO<sub>2</sub> affects bubble  
671 nucleation to a significant extent if the system contains  $\geq 880$  ppm CO<sub>2</sub> (cf. Bai et al., 2008) and  
672 that the diffusivity of carbon dioxide in the melt can limit CO<sub>2</sub> exsolution and, thus, restrict  
673 bubble growth (see Pichavant et al., 2013). The available experimental dataset indicates that even  
674 small amounts of CO<sub>2</sub> ( $< 800$  ppm) might change BND considerably (Fig. 4b); however, more  
675 experiments are needed to allow modeling the effect of CO<sub>2</sub>. Furthermore, although Fiege et al.  
676 (2014a) observed no dependence of BND on changing bulk S (from  $\sim 150$  to  $\sim 1000$  ppm) and Cl  
677 (0 to 1000 ppm), it cannot be ruled out that these volatiles can have a significant influence,  
678 considering that the S and Cl contents were not varied systematically and that the possible effects  
679 of S and Cl may be overprinted by smaller variations in the initial H<sub>2</sub>O content (see Table 2 in  
680 Fiege et al., 2014a). Here, a comparison of the results of this study obtained for CO<sub>2</sub>-Cl-free, S-  
681 poor dacitic andesite (average BND =  $10^{5.4}$  mm<sup>3</sup>) with the BND values determined by Fiege et  
682 al. (2014a) for CO<sub>2</sub>-free, S-Cl-bearing dacitic andesite (BND =  $10^{4.6}$  mm<sup>3</sup>) at the same  
683 decompression rate (0.1 MPa/s), indicates a decrease of BND with the addition of Cl and/or S for

684 a given decompression rate. Hence, we suggest that the H<sub>2</sub>O diffusivity term in equation 3 and 4  
685 should be replaced by:

$$686 \quad D_{\text{vol+alk}} = F_{\text{H}_2\text{O}} D_{\text{H}_2\text{O}} + F_{\text{CO}_2} D_{\text{CO}_2} + F_{\text{S}} D_{\text{S}} + F_{\text{Cl}} D_{\text{Cl}} + F_{\text{Na}} D_{\text{Na}} \quad (5),$$

687 where F is the fraction of H<sub>2</sub>O, CO<sub>2</sub>, S, Cl and Na in the fluid, and D is the diffusivity of the  
688 respective molecule or element in the melt. Sodium should be considered since it is typically the  
689 charge-balancing cation for Cl within the fluid phase (e.g., Bodnar et al., 1985). A similar  
690 approach should be used for the molecular volume of H<sub>2</sub>O in the liquid  $\Omega_L$ . Here, a bulk value  
691 should be estimated for  $\Omega_L$  based on the fluid composition. However, more experimental data are  
692 needed to calibrate the effect of varying volatile compositions on BND and to adjust equation 3,  
693 4 and 5 accordingly.

694 While the proposed approach should help to improve applicability of equation 3 and 4 to more  
695 complex melts containing different volatile species it does not account for the influence of water  
696 activity  $a(\text{H}_2\text{O})$  on BND at a given decompression rate as observed by Gondé et al. (2011) and  
697 Fiege et al. (2014a). Assuming that the ~800 ppm CO<sub>2</sub> in the experiments of Pichavant et al.  
698 (2013) and the minor amounts of S and Cl in some of the experiments of Fiege et al. (2014a)  
699 have a minor effect on BND, we can use these results in combination with the H<sub>2</sub>O-  
700 undersaturated experiments of Martel and Bureau (2001) and Gondé et al. (2011) to evaluate the  
701 effect of the water activity on bubble nucleation in CO<sub>2</sub>-poor systems. Fig. 7 shows the relevant  
702 data. It is emphasized that Gondé et al. (2011) detected a water loss during their experiments,  
703 which depends on samples size and run duration. They showed that for shorter run duration of  
704 ~1000 s this effect is rather small. Thus, only runs 44, 45 and 51 are shown in Fig. 7 (run  
705 duration < 1400s; see Table 3 in Gondé et al., 2011).

706 It seems to be well-accepted that – for a given melt composition and given pressure-temperature  
707 conditions – the correlation between BND and decompression rate on a double logarithmic scale  
708 can be described by linear trends with a constant slope (e.g., Toramaru, 2006; Gondé et al., 2011;  
709 Fiege et al., 2014a). Hence, we propose that the following equation can be used to describe the  
710 relationship between the decompression rate  $r$  and BND in a simple way:

$$711 \log(\text{BND}) = A \cdot \log(r) + B \quad (6),$$

712 where  $A$  and  $B$  are empirical parameters. Here,  $A$  is the slope of the linear trend(s), which  
713 according to Fiege et al. (2014a) is well predicted by the Toramaru (2006) model and  $A$  is  
714 estimated to be  $\sim 1.5$ , being in agreement with several previous studies (see trends in Fig. 4a).  $B$   
715 is the Y-axis intercept, which can be easily calculated based on the known values for  
716 decompression rate and BND for each experimental data-point.

717 Since the experimental dataset is growing but still very limited (e.g., systematic investigations of  
718 the influence of major element composition, volatile contents and temperature on  
719 decompression-induced bubble formation are missing), we suggest that a model approach for the  
720 estimation of  $B$  in equation 6 should be kept relatively simple using only one well-constrained  
721 parameter, which varies with temperature and melt composition.

722 A melt property parameter, which is influenced by bulk composition and temperature, and which  
723 is directly affecting bubble formation is the melt viscosity ( $\eta$ ). The viscosity of the most relevant  
724 silicate melts is experimentally very well constrained and different (numerical) model  
725 approaches exist, which allow us to accurately calculate the viscosity for various melt  
726 compositions and conditions. We emphasize that the diffusivities of volatiles such as  $\text{H}_2\text{O}$ ,  $\text{Cl}$ ,  
727  $\text{CO}_2$  and  $\text{S}$  can typically be well-described by the Eyring equations, which relates chemical  
728 diffusivities to melt viscosities (e.g., Behrens and Stelling, 2010; Zhang and Ni, 2010) and also

729 that the surface tension of a melt/liquid is closely related to its viscosity (e.g., Gardner and  
730 Ketcham, 2011). We use the viscosity models of Hui and Zhang (2007) and of Giordano et al.  
731 (2008), which are two of the most comprehensive and accepted models published in the last  
732 couple of years. Notably, these models do not account for the effect of CO<sub>2</sub>, S and Cl on  
733 viscosity; however, these and other volatiles (Br, I) appear to be less important in terms of  
734 directly influencing melt viscosity when compared to, e.g., H<sub>2</sub>O (e.g., Dingwell and Hess, 1998;  
735 Bourgue and Richet, 2001; Zimova and Webb, 2006; 2007; Giordano et al, 2008). The melt  
736 viscosities were estimated for compositions prior to decompression and the average values for  
737 the melt viscosities, calculated based on the two applied viscosity models, are provided in the  
738 legend of Fig. 7. In Fig. 7b we plot the Y-axis intercept estimated for each relevant data-point or  
739 -set assuming a slope of 1.5 (= A in equation 6; see above) against the predicted melt viscosity  
740 (*please note*: average B values are presented in Fig. 7b for the results of Fiege et al. (2014a) and  
741 Pichavant et al. (2014) as well as for results of Martel and Bureau (2001) at 750 °C). In a first  
742 approach we fitted a logarithmic regression to describe the dependence between B and melt  
743 viscosity  $\eta$  (equation 7):

$$744 \quad B = -4.567 (\pm 0.539) \cdot \log(\eta) + 7.876 (\pm 0.299) \quad (R^2 = 0.935) \quad (7).$$

745 In combination with equation 6 the decompression rate  $r$  can be predicted based on bubble  
746 number densities measured in natural samples, which were produced by the eruption of an  
747 initially water-undersaturated magma. Although, considering that CO<sub>2</sub>, S, and Cl may have a  
748 significant effect on BND at a given decompression rate, equation 8 is proposed for CO<sub>2</sub>-, S-,  
749 and Cl-free systems. Here, the results of Pichavant et al. (2013; CO<sub>2</sub>-bearing) and Fiege et al.  
750 (2014a; S- and Cl-bearing) are excluded for the calculation of equation 8, while the results of this  
751 study are still considered, since the starting glass contains only minor amounts of S (~80 ppm).

752  $B = -5.097 (\pm 1.193) \cdot \log(\eta) + 8.197 (\pm 0.756) \quad (R^2 = 0.859) \quad (8).$

753 We emphasize that the proposed parameterizations are based on a limited dataset and strongly  
754 encourage the community to calibrate the relationship between melt viscosity, decompression  
755 rate and bubble number density based on additional experimental studies.

756

757 **5.2. Linking experimental results to natural samples: Perspective for future experiments**

758 Studying bubble nucleation, both experimentally and theoretically, is an undeniable prerequisite  
759 to understand and interpret the vesiculation in volcanic ejecta such as pumices or tephra. In this  
760 manuscript we have reviewed the available experimental dataset and techniques, while focusing  
761 on bubble textures produced by (almost) continuous decompression experiments. Even though  
762 the evaluation of the existing data shows that there is a dependence of the bubble number  
763 densities on the decompression path and more importantly on the decompression rate, we see the  
764 urgent necessity to widen the experimental database to more mafic melt compositions as well as  
765 to lower decompression rates ( $\ll 0.1$  MPa/s). We suggest performing future decompression  
766 experiments mostly by (almost) continuous pressure release as this seems to reflect a more  
767 natural approach of simulating magma ascent on the laboratory scale. However, the compilation  
768 of experimental data shows that low ascent rates ( $\approx$  low decompression rates) can be simulated  
769 by using relatively fast and continuous decompression steps ( $\sim 0.1$  MPa/s) followed by a long  
770 term annealing period (more than  $\sim 70$  h). In any case, experimentalists should balance out  
771 advantages and disadvantages of different capsule material and designs, and carefully separate  
772 homogeneous from heterogeneous bubble nucleation in their run products. It is highly  
773 recommended to apply new, high precision technologies in terms of image analysis as 3D-

774 tomographic scans can provide true bubble volumes, shapes and networks, and in respect of *in*  
775 *situ* observations techniques at simultaneous high-temperatures and high-pressures.

776 Progress has been made in the last decades on understanding the difference between  
777 homogeneous und heterogeneous bubble nucleation. Various studies, mainly on rhyolitic  
778 systems, show that the presence of Fe-(Ti)-oxides can lead to heterogeneous bubble nucleation  
779 upon decompression (e.g., Hurwitz and Navon, 1994). However, while crystals are inevitably  
780 present in magmas, the crystal fraction (Mangan et al., 2004a) and the crystal types seem to  
781 dictate the dominant nucleation mechanism; i.e., heterogeneous vs. homogeneous (see the  
782 compilation of experimental result in Fig. 5b). In systems with low amounts of Fe-(Ti)-oxides,  
783 distances between heterogeneously nucleating bubbles may be too large to transport the volatiles  
784 to the bubbles before the total decompression  $\Delta P$  reaches values, which allows homogeneous  
785 nucleation. Moreover, owing to the lack of experimental data on possibly heterogeneous bubble  
786 nucleation in crystal-bearing but Fe-(Ti)-oxides free systems, it is still not possible to state  
787 whether homogenous or heterogeneous bubble nucleation is prevailing in magmatic systems.  
788 However, if oxides (and possible sulfides) are the only phases that significantly affect the  
789 nucleation mechanism, parameters such as oxygen fugacity (and sulfur fugacity) may be critical  
790 since they significantly influence the stability of oxides (and sulfides). Hence, the total fraction  
791 of crystals relevant for bubble nucleation processes influences strongly the degassing mechanism  
792 and, thus, controls whether degassing occurs at greater depth (higher pressures) via  
793 heterogeneous nucleation (low  $\Delta P$  required) or near surface (lower pressures) via homogeneous  
794 nucleation (high  $\Delta P$  required). The latter process results most likely in explosive and potentially  
795 hazardous eruptions.

796 Moreover, the evaluated experimental dataset shows that the effects of melt compositions on  
797 bubble number density are significant and have to be investigated more systematically. A main  
798 focus of future experimental studies could be the influence of water activity on bubble formation  
799 and growth, which seems to be significant and is of high importance to improve our  
800 understanding of degassing mechanisms at depth and during magma ascent, considering that  
801 magmatic systems are often not water-saturated prior to eruption (e.g., Hervig et al. 1989;  
802 Gardner et al. 1995). Finally, we have to investigate the differences between equilibrium and  
803 non-equilibrium volatile exsolution in regimes of closed- or open-system degassing, allowing us  
804 to predict the kinetics of volcanic eruptions from effusive to explosive activity (e.g., Pichavant et  
805 al., 2013; Cashman, 2014) and from slow to fast magma ascent.

806

807

## 6. Conclusion

808 In this manuscript we have mainly reviewed existing experimental and analytical methods  
809 associated with the vesiculation of silicate melts during decompression. We are highlighting gaps  
810 in the available experimental dataset that should be filled in the near future and describe  
811 advantages and disadvantages of the different experimental and analytical approaches that could  
812 be applied to perform such studies. There are four main observations and outcomes of this study:

813 1. Close attention has to be paid to capsule design and decompression techniques when  
814 comparing different experimental datasets. For instance, the simulation of natural magma  
815 ascent is probably best reproduced by experiments using foremost continuous pressure  
816 release techniques.

- 817 2. Variations in melt composition can significantly influence volatile exsolution and bubble  
818 forming processes. Even variations in the abundance of minor volatile species, e.g., Cl  
819 and/or S, show notable effects on the evolution of bubble number densities.
- 820 3. Based on literature data and results obtained from additional decompression experiments  
821 presented in this study, we propose a new decompression-rate-meter for initially water-  
822 undersaturated melts that links the melt viscosity in a simple approach to the  
823 decompression rate and the bubble number density.
- 824 4. Efforts have to be made to widen the range of experimental data on decompression-  
825 induced (equilibrium and disequilibrium) vesiculation, especially to intermediate and  
826 mafic melt compositions, as the available dataset is still limited. These data will allow  
827 one to improve the calibration of the suggested decompression-rate-meter as well as of  
828 previously published models.

829

830

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1212

### Figure captions

1213 **Figure 1.** Schematic plot of the 3 major decompression methods: single-step (blue dashed line),  
1214 multi-step (red solid line) and continuous (black dashed line). The decompression rate for single-  
1215 and multi-step experiments are averaged and given as a “constant” time-integrated value ( $= r_{int}$ ).  
1216 In case of the instantaneous, once-only pressure release of the single-step method, the following  
1217 annealing step is considered equal to the entire decompression run duration ( $\Delta t$ ).

1218

1219 **Figure 2.** Screenshots of 3D-visualization of bubbles from  $\mu$ -tomographical scan data for Nowak  
1220 et al. (2011) experimental end products for **a)** single-step, **b)** multi-step and **c)** continuous  
1221 decompression of water-saturated rhyodacitic melts, using YaDiV software (Friese et al., 2013).

1222

1223 **Figure 3.** Heterogeneous bubble nucleation: Relationship between wetting angle ( $\Psi$ ) and  
1224 supersaturation pressure ( $\Delta P_N$ ), where wetting angle  $\Psi = 180^\circ - \theta$  ( $\theta$  = contact angle; Gualda and  
1225 Ghiorso, 2007). It has been proven that Fe-(Ti)-oxides trigger heterogeneous nucleation (e.g.,  
1226 Hurwitz and Navon, 1994) but other minerals (especially oxides and possibly sulfides) may have  
1227 a similar effect. v.: vapor (fluid);  $\sigma$ : melt-vapor surface tension;  $\Delta F$ : Helmholtz free energy for  
1228 creating a curved surface;  $\Phi$ : wetting factor. The figure was modified after Hurwitz and Navon  
1229 (1994), Mangan et al. (2004b) and Gualda and Ghiorso (2007). *Please note:* Mangan et al.  
1230 (2004b) used the term *contact angle* in their Fig. 1 for the “outer angle”, which is typically  
1231 defined as wetting angle (e.g., this study; Zisman, 1964; Gualda and Ghiorso; 2007).

1232

1233 **Figure 4a-b.** Experimental results for homogeneous bubble nucleation based on experimental  
1234 approaches using (almost) continuous and constant decompression rates ( $r$ ). Figure **4a)** shows all

1235 available results for homogeneous bubble nucleation based on (almost) continuous  
1236 decompression experiments. A trend predicted by the model of Toramaru (2006) for rhyolitic  
1237 melts at 800 °C is plotted for comparison (see Section 5.1 for a detailed description of the  
1238 model). The haplogranitic melt composition of Martel and Bureau (2001; MB01) is similar to the  
1239 rhyolitic compositions used by the other studies. Pichavant et al. (2013) performed additional  
1240 basaltic experiments, which are not shown because they are not directly comparable to the  
1241 plotted datasets owing to a change (decrease) in decompression rate during decompression.  
1242 Linear regressions are plotted for selected experimental datasets (Fiege et al., 2014; Mangan and  
1243 Sisson, 2000; Marxer et al., 2015; Mourtada-Bonnefoi and Laporte, 2004), illustrating that the  
1244 results of the different studies follow trends with similar slopes. Figure 4b) is an enlarged view  
1245 of Fig. 4a and shows only selected data for rhyolitic systems at 800 °C. The selected rhyolitic  
1246 systems were volatile-saturated prior to decompression and contain initially 0 to 800 ppm bulk  
1247 CO<sub>2</sub>.

1248 \*The run products of Pichavant et al. (2013) contain very small amounts of Fe-Ti-oxides;  
1249 however, the bubbles in the center of the capsules are interpreted by the authors to be produced  
1250 homogeneous bubble nucleation.

1251 *References in Fig. 4:* Pi13: Pichavant et al. (2013); Fi14: Fiege et al. (2014a); Go11: Gondé et al.  
1252 (2011); MS00: Mangan and Sisson (2000); MB01; Martel and Bureau (2001); Ha10: Hamada et  
1253 al. (2010); MBL04: Mourtada-Bonnefoi and Laporte (2004); MBL02: Mourtada-Bonnefoi and  
1254 Laporte (2002); MBL99: Mourtada-Bonnefoi and Laporte (1999); To06: Toramaru (2006).

1255

1256 **Figure 5a-b.** Experimental results for heterogeneous bubble nucleation based on **a)** single- and  
1257 multi-step experiments or **b)** on experimental approaches using (almost) continuous and constant

1258 decompression rates ( $r$ ). The dashed and dotted lines are just to guide the eyes. Two dotted lines  
1259 are shown for the dataset of Mangan et al. (2004b) since these results scatter significantly.

1260 \*According to unpublished image analysis results of S.B. Cichy, the Fe-(Ti-) oxide content was  
1261 less than 0.1 vol% in the experiments of Cichy et al. (2011), while the total crystal fraction is  
1262 rather high (1 to 9 vol%; see Cichy et al, 2011).

1263

1264 **Figure 6a-b.** Influence of annealing time on BND. The experiments were performed by Fiege et  
1265 al. (2014; Fi14) using a hydrous (~6.5 wt% H<sub>2</sub>O) andesitic melt as starting material (temperature:  
1266 1030 °C; pressure was released continuously from 400 to 70 MPa). **a)**  $\log(\text{BND} \cdot \text{mm}^3)$  vs.  
1267 annealing time after fast decompression at a constant rate of 0.1 MPa/s (Fig. 6a was modified  
1268 after Fiege et al., 2014a). **b)**  $\log(\text{BND} \cdot \text{mm}^3)$  vs. integrated decompression rate [ $r_{\text{int}} = (P_i - P_f) /$   
1269  $\Delta t$ ; see Fig. 1]. The intergrated decompression rate was calculated for the experiments shown in  
1270 Fig. 6a and the results are compared to experiments, which were directly quenched after  
1271 decompression at different rates (0.0005 to 0.1 MPa/s).

1272 *Initial S and Cl contents of the andesitic melt:*

1273 a) Experiments GYCIA: ~1000 ppm S, ~1000 ppm Cl

1274 b) Exp. GYMClA: ~1000 ppm S; ~500 ppm Cl

1275 c) Exp. QFMA: ~140 ppm S, Cl-free; and QFMClA: ~240 ppm S, 1000 ppm Cl

1276 d) Exp.: GYCIA and GYMClA, see a) and b) for contents

1277

1278 **Figure 7a-b.** Correlation between bubble number density BND, decompression rate  $r$  and melt  
1279 viscosity  $\eta$  for water-undersaturated melts prior to decompression. Only experiments with short  
1280 run durations of Gondé et al. (2011) were considered to minimize the possible influence of water

1281 loss during their experiments (see Section 5.1 for details). The presented melt viscosities [Pa·s]  
1282 are average values (error: 2 sigma of mean) calculated based on the two values predicted by the  
1283 viscosity model of Hui and Zhang (2007) and of Giordano et al. (2008), respectively. **a)**  
1284  $\log(\text{BND} \cdot \text{mm}^3)$  vs. decompression rate [MPa/s]. The trends were predicted using equation 6  
1285 and 7 (Section 5.1). **b)** Y-axis intercept vs. melt viscosity. Only average values for each melt  
1286 composition and temperature are shown. The equations for the two regressions are given in the  
1287 text. The black trend is based on all results shown in Fig. 7b), while the experiments of Pichavant  
1288 et al. (2013) and Fiege et al. (2014a) are excluded for the calculation of the dashed blue trend  
1289 (see Section 5.1 for details).

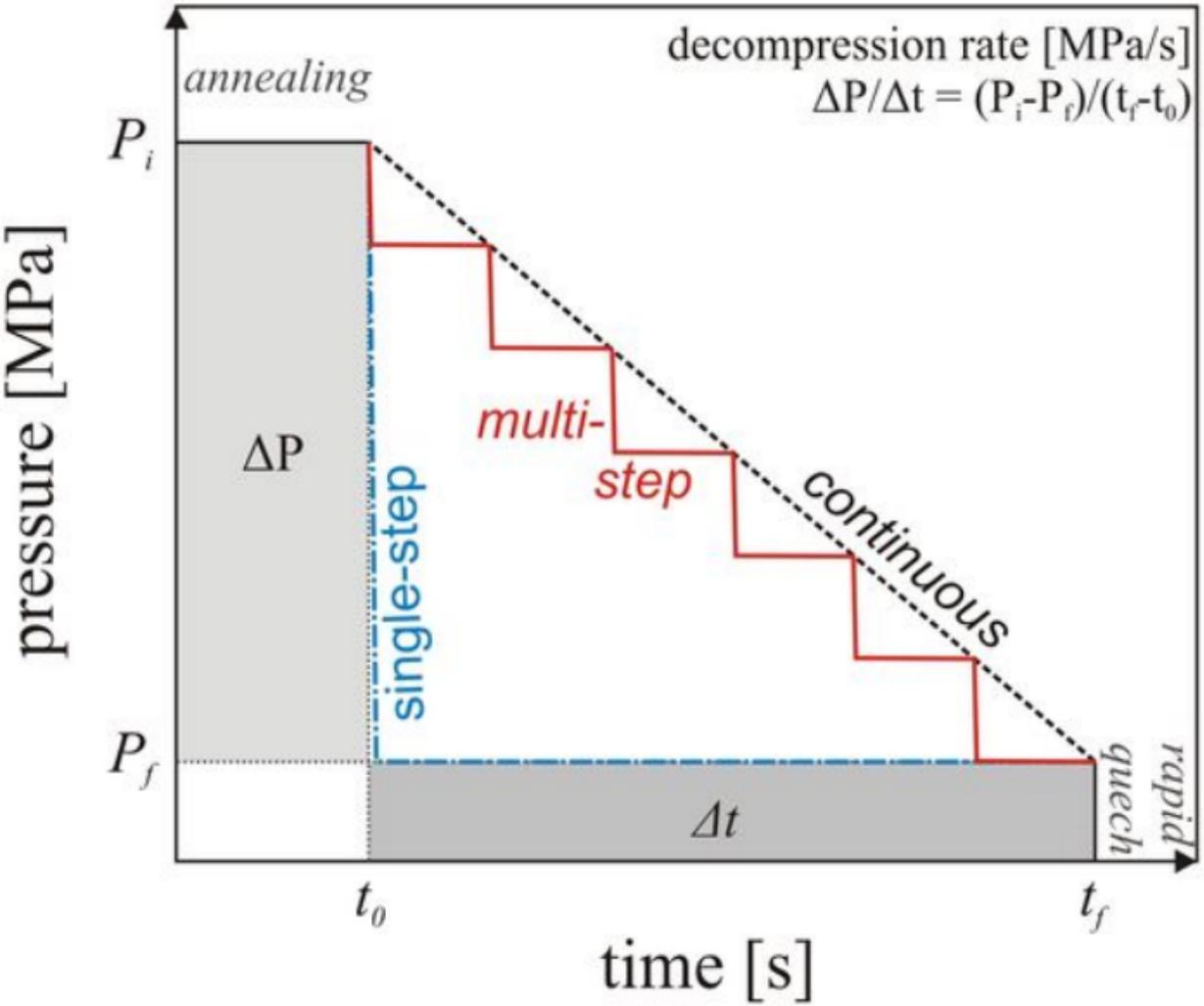
1290 *References in Fig. 7:* Pi13: Pichavant et al. (2013); Fi14: Fiege et al. (2014a); Go11: Gondé et al.  
1291 (2011); MB01; Martel and Bureau (2001).

1292 \*Y-axis intercept of the trends in Fig. 7a on a  $\log(\text{BND} \cdot \text{mm}^3)$  vs.  $\log(r \cdot \text{s/MPa})$  plot, assuming  
1293 a slop of 1.5 (see Section 5.1 for details).

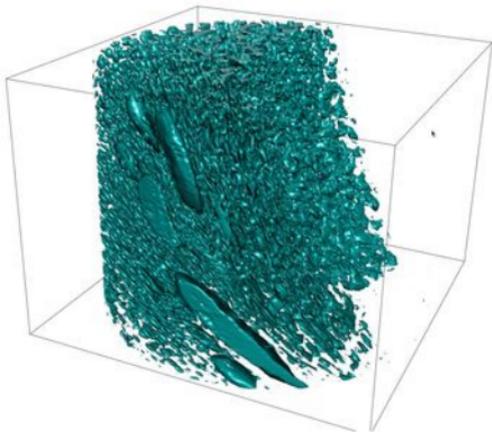
**Table 1:** Compilation of experimental studies and relevant conditions on decompression-induced bubble formation in silicate melts using (almost) continuous decompression rates and selected studies using single-step technique. Only conditions of experiments which produced bubbles and for which BND was determined are listed.

<i>Melt composition</i>	<i>P<sub>initial</sub> [MPa]</i>	<i>P<sub>final</sub> [MPa]</i>	<i>T [°C]</i>	<i>Annealing time t<sub>A</sub> [h or s]</i>	<i>Decompression rates [MPa/s]</i>	<i>Volatiles</i>	<i>H<sub>2</sub>O-saturated or -undersaturated</i>	<i>Continuous, multi-, or single-step</i>	<i>Experimental device</i>	<i>Reference</i>
<i>homogenous bubble nucleation</i>										
rhyolite	285	172	800	120 s	0.77	H <sub>2</sub> O	saturated	(quasi) continuous	CSPV	Mourtada-Bonnefoi and Laport (1999)
rhyolite	200	25 to 50	900	--	0.025 to 8.5	H <sub>2</sub> O (traces of CO <sub>2</sub> )	saturated	continuous	CSPV	Mangan and Sisson (2000)
haplogranite (rhyolite)	960 to 1220	~580 to 1245 #	~740 to 850 #	--	2.3 to 49.0	H <sub>2</sub> O	saturated	continuous #	DA	Martel and Bureau (2001)
rhyolite	200 to 295	29 to 246	800	1 to 122 s (one at 1.5 h)	0.30 to 6.32	H <sub>2</sub> O±CO <sub>2</sub>	saturated	(quasi) continuous	CSPV	Mourtada-Bonnefoi and Laport (2002)
rhyolite	260	58.9 to 88.6	800	--	0.0278 to 1.24	H <sub>2</sub> O	saturated	multi-step (almost continuous)*	CSPV	Mourtada-Bonnefoi and Laport (2004)
rhyolite	250	30 to 75	700 to 800	--	0.7 to 90	H <sub>2</sub> O	saturated	continuous	IHPV	Hamada et al. (2010)
haplogranite (rhyolite)	288 to 363	4 to 205	900 to 1000	--	0.06 to 0.75	H <sub>2</sub> O	undersaturated	continuous	TIHPV	Gondé et al. (2011)
phonolite	200	75 to 150	1050	--	0.0028 to 1.7	H <sub>2</sub> O	mainly saturated	continuous, multi- and single-step	IHPV	Marxer et al. (2015)
basalt	195 to 200	45 to 48	1150	--	0.017 to 0.027	H <sub>2</sub> O+CO <sub>2</sub>	undersaturated	continuous	IHPV	Pichavant et al. (2013) ¶
(dac.) andesite	400	70	1030	0 to 72 h	0.0005 to 0.1	H <sub>2</sub> O+S±Cl	undersaturated	continuous	IHPV	Fiege et al. (2014)
(dac.) andesite	400	70 to 150	1030	--	0.1	H <sub>2</sub> O (+S)	undersaturated	continuous	IHPV	<i>this study</i>
<i>heterogeneous bubble nucleation</i>										
rhyolite	200	50 to 175	900	--	0.003 to 8.5	H <sub>2</sub> O (traces of CO <sub>2</sub> )	saturated	continuous	CSPV	Mangan and Sisson (2000)
rhyolite	200	100 to 175	850	--	0.003 to 4.2	H <sub>2</sub> O+CO <sub>2</sub>	saturated	continuous	CSPV	Mangan et al. (2004a)
dacite	200	50 to 170	950	--	0.60 to 1.64	H <sub>2</sub> O	saturated	continuous	CSPV	Mangan et al. (2004b)
rhyolite	200	20.5 to 67.7	800	--	0.0278 to 1.01	H <sub>2</sub> O+CO <sub>2</sub>	saturated	continuous	CSPV	Cluzel et al. (2008)
rhyodacite	300	50	850	--	0.0002 to 20	H <sub>2</sub> O±CO <sub>2</sub>	saturated	continuous, multi- and single-step	CSPV	Cichy et al. (2011)
rhyolite	50 to 175	30 to 145	740 to 800	15 s to 6 h	0.0012 to 7.0	H <sub>2</sub> O	saturated	single-step	CSPV	Gardner and Denis (2004)
rhyolite	50 to 125	17.5 to 90	550 to 700	30 to 180 s	0.11 to 2.42	H <sub>2</sub> O	saturated	single-step	CSPV	Gardner (2007)

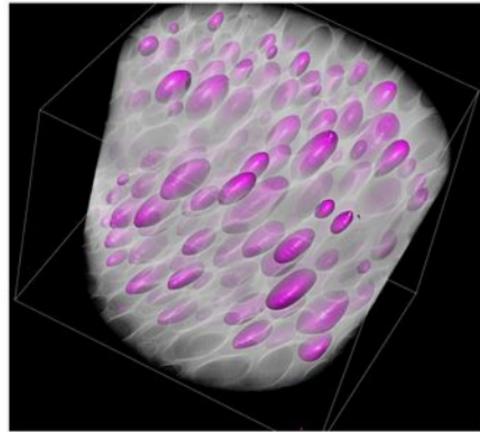
\*Step size was <1 MPa leading to an almost continuous decompression. CSPV: Cold sealed pressure vessel or externally heated pressure vessel; IHPV: Internally heated pressure vessel; TIHPV: Transparent internally heated pressure vessel using sapphire windows; DA: Bassett-type hydrothermal diamond-anvil cell. # Decompression is induced by cooling. ¶ The run products contain very small amounts of Fe-Ti-oxides; however, the bubbles in the center of the capsules are interpreted to be produced homogeneous bubble nucleation.



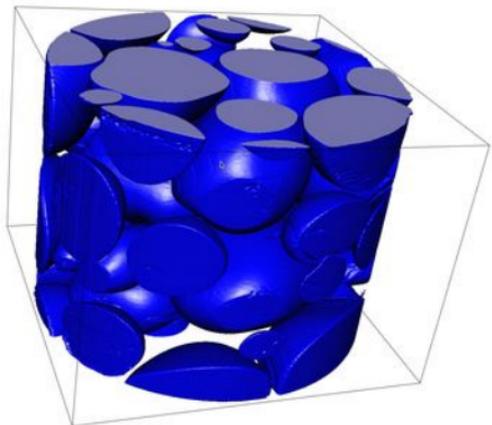
a) single-step



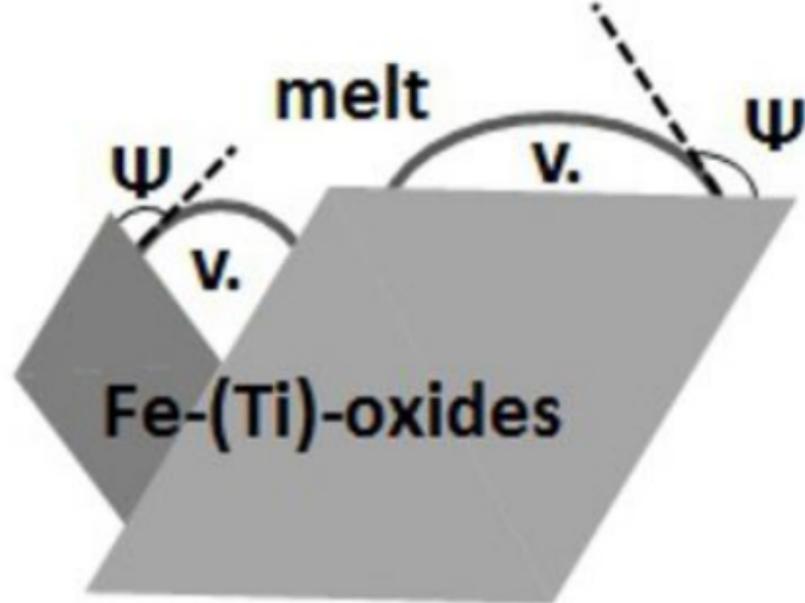
b) multi-step



c) continuous

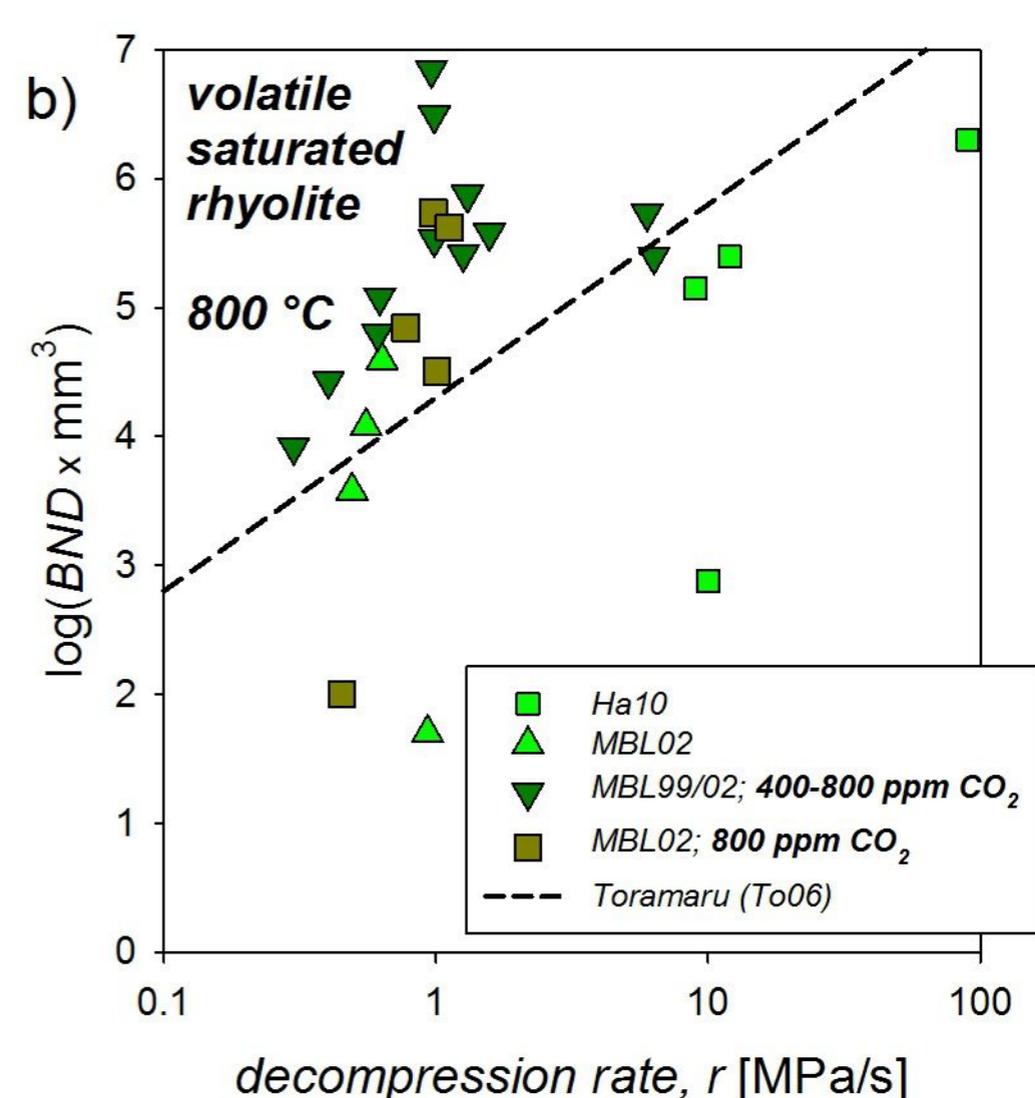
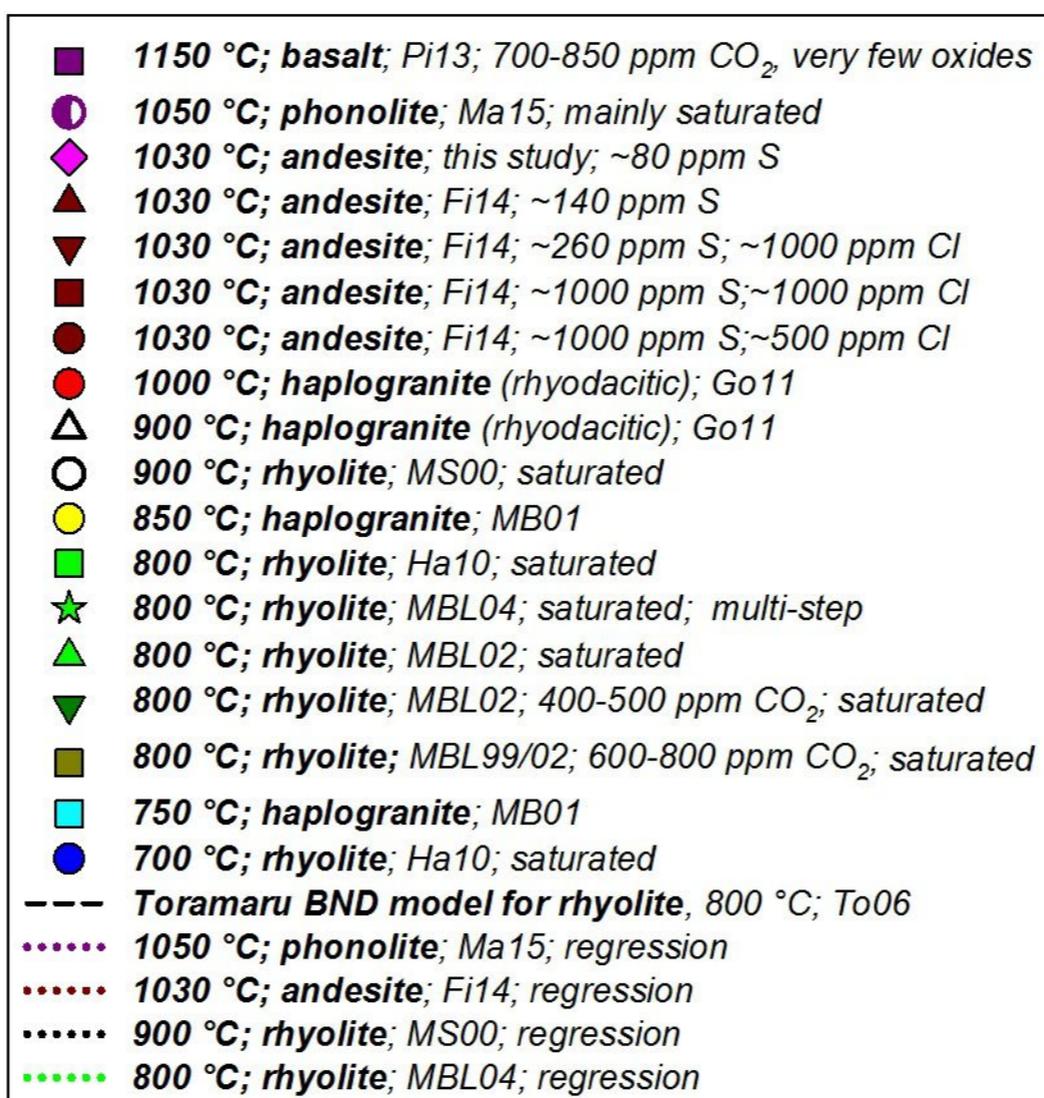
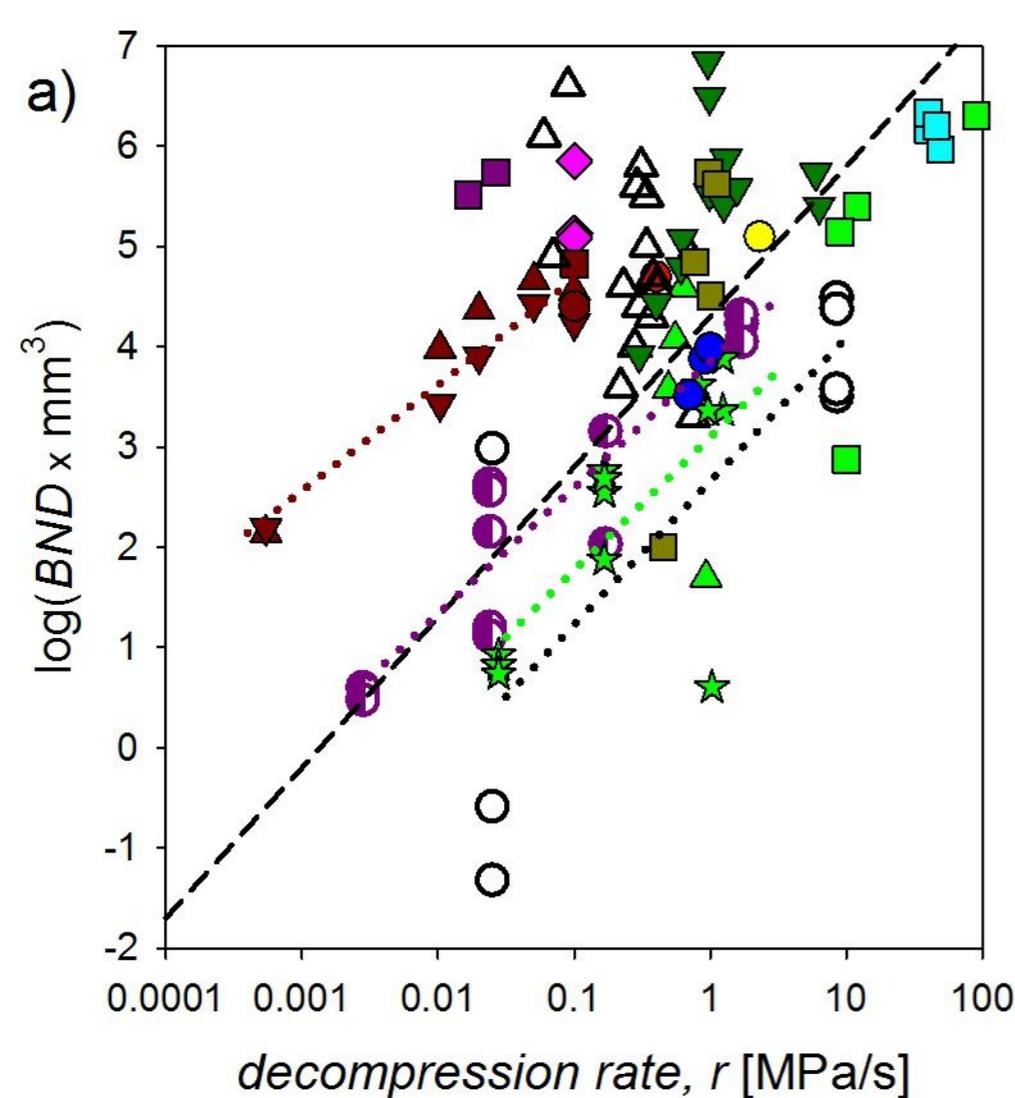


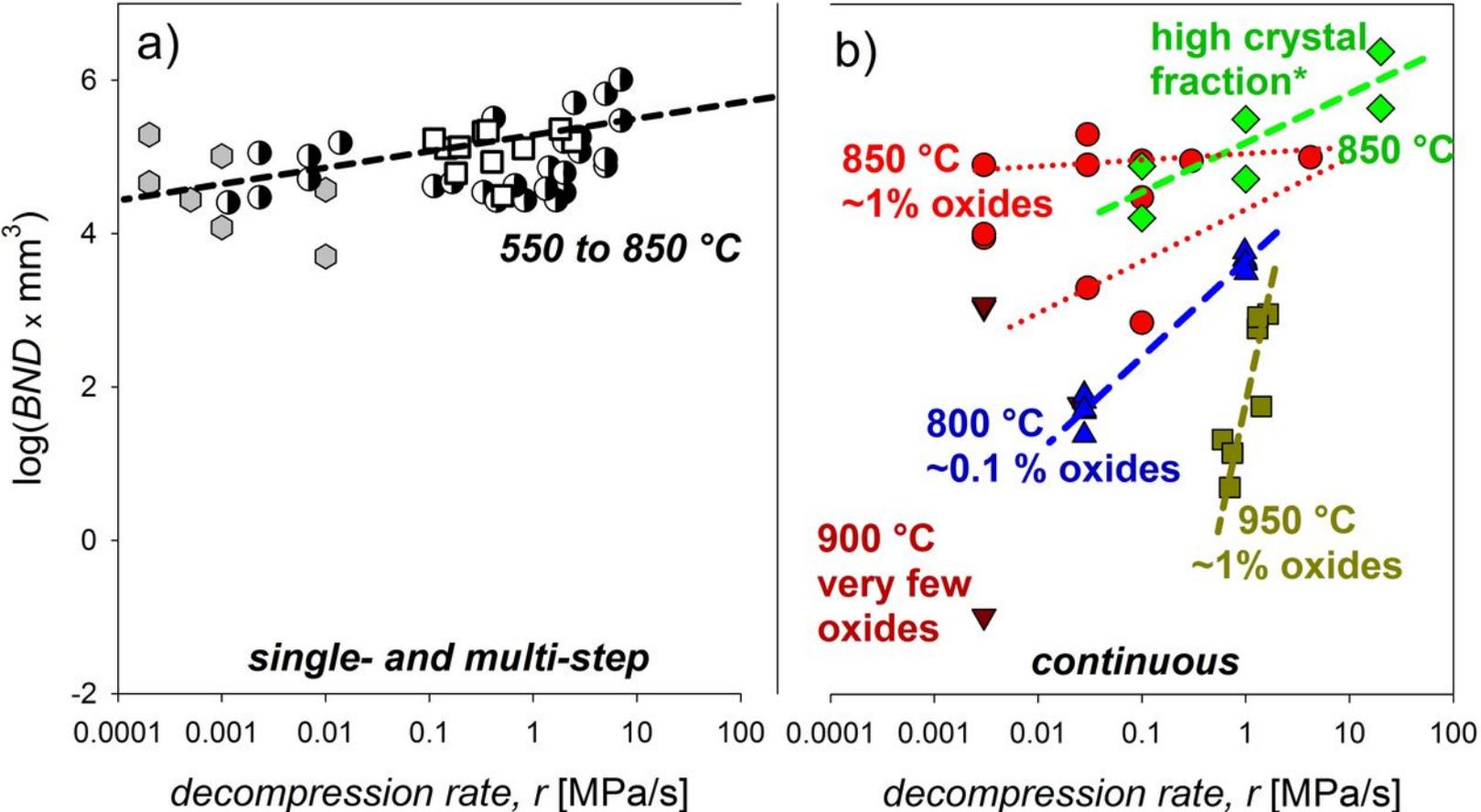
**box sizes (x, y, z):**  
0.76mm, 0.76mm, 0.76mm  
**rock sample volumes:**  
0.35mm<sup>3</sup> (cylindrical)



$$\Delta P_N = \sqrt{\frac{16 \cdot \pi \cdot \sigma^3 \cdot \Phi}{3 \cdot \Delta F}}$$

$$\Phi = (2 - \cos(\Psi)) \cdot (1 + \cos(\Psi))^2 / 4$$





- ◻ 850 °C; **rhyodacite**; Cichy et al. (2011); multi-
- 740-800 °C; Gardner and Denis (2004); single-s
- ◻ 550-700 °C; Gardner et al. (2007); single-step

- ▼ 900 °C; Mangan and Sisson (2000)
- 850 °C; Mangan et al. (2004b)
- ▲ 800 °C; Cluzel et al. (2008)
- 950 °C; **dacite**; Mangan et al. (2004a)
- ◆ 850 °C; **rhyodacite**; Cichy et al. (2011)

